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# Recommended Standards for Wastewater Facilities

## 2004 Edition

### **Policies for the Design, Review, and Approval of Plans and Specifications for Wastewater Collection and Treatment Facilities**

A Report of the Wastewater Committee of the  
Great Lakes--Upper Mississippi River Board  
of State and Provincial Public Health and Environmental Managers

MEMBER STATES AND PROVINCE  
Illinois Indiana Iowa Michigan Minnesota Missouri  
New York Ohio Ontario Pennsylvania Wisconsin

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## FOREWORD

In 1947, a "Committee on Development of Uniform Standards for Sewage Works" was created by the group now known as the Great Lakes -- Upper Mississippi River Board of State and Provincial Public Health and Environmental Managers.

This Committee, composed of a representative from each state, was assigned the responsibility to review existing standards for sewage works, to investigate the possibility of preparing joint standards to be adopted by the states represented, and to report its findings to the Board.

Based on this initial report, the Board authorized the Committee to prepare sewage works design standards, which were first published in 1951. They subsequently were revised and published again in 1960, 1968, 1971, 1973, 1978, 1990 and 1997. In 1977, the Province of Ontario was invited, as a Great Lakes participant, to serve on the Committee.

These standards have again been revised and are published herein as the 2004 edition. They are intended for use as a guide in the design and preparation of plans and specifications for wastewater facilities insofar as these standards are applicable to normal situations for an individual project.

The design criteria in these standards are intended for the more conventional municipal wastewater collection and treatment systems. Innovative approaches to collection and treatment, particularly for the very small municipal systems, are not included. The individual reviewing authority should be contacted for design guidance and criteria where such systems are being considered.

Lack of description or criteria for a unit process or equipment does not suggest it should not be used, but only that consideration by the reviewing authority will be on the basis of information submitted with the design. Engineering data that may be required for new process and application evaluation is included in Paragraph 53.2 of these standards.

These standards are intended to suggest limiting values for items upon which an evaluation of the plans and specifications will be made by the reviewing authority; and to establish, as far as practicable, uniformity of practice among the several states and province. Statutory requirements, regulations, and guidelines among the states and province are not uniform and use of the standards must adjust itself to these variations. Users also should be cognizant of locally adopted standards and applicable federal requirements.

The term "shall" is used where practice is sufficiently standardized to permit specific delineation of requirements or where safeguarding of the public health or protection of water quality justifies such definite action. Other terms, such as "should," "recommended," and "preferred," indicate desirable procedures or methods, with deviations subject to individual consideration.

Definition of terms and their use in these standards is intended to be in accordance with GLOSSARY -- WATER AND WASTEWATER CONTROL ENGINEERING, jointly prepared by APHA, ASCE, AWWA, and WPCF. The customary units of expression used are in accordance with those recommended in WPCF Manual of Practice No. 6, UNITS OF EXPRESSION FOR WASTEWATER MANAGEMENT. The International Standard Units are in accordance with those recommended in National Institute of Standards and Technology (NIST) Guide for the Use of the International System of Units (SI).

## **CHAPTER 10 ENGINEERING REPORTS AND FACILITY PLANS**

### **10. GENERAL**

#### **10.1 Engineering Services**

Engineering services are performed in three steps:

- a. Engineering Report or Facility Plan;
- b. Preparation of construction plans, specifications, and contractual documents; and
- c. Construction compliance, inspection, administration, and acceptance.

Chapter 10, Engineering Reports and Facility Plans, covers only item a. above.

#### **10.2 Preliminary Project Submittal**

A preliminary project submittal may be necessary prior to preparation of an Engineering Report or Facility Plan. This submittal needs to include:

- a. A description of problems or developments which have resulted in consideration of a wastewater facilities project;
- b. Identification of governmental and consultant representatives authorized to provide information and seek regulatory agency approvals and decisions regarding the project; and
- c. Identification of potential treated wastewater discharge locations for the purpose of regulatory agency determinations of suitable effluent quality requirements.

No approval for construction can be issued until final, detailed plans and specifications have been submitted and approved by the appropriate reviewing authority. Refer to Chapter 20.

### **11. ENGINEERING REPORT OR FACILITY PLAN**

For federal, provincial, or state financed grant or loan projects, additional requirements may apply.

The Engineering Report or Facility Plan: identifies and evaluates wastewater related problems; assembles basic information; presents criteria and assumptions; examines alternate projects, with preliminary layouts and cost estimates; describes financing methods, sets forth anticipated charges for users; reviews organizational and staffing requirements; offers a conclusion with a proposed project for client consideration; and outlines official actions and procedures to implement the project. The planning document must include sufficient detail to demonstrate that the proposed project meets applicable criteria.

The concept (including process description and sizing), factual data, and controlling assumptions and considerations for the functional planning of wastewater facilities are presented for each process unit and for the whole system. These data form the continuing technical basis for the detailed design and preparation of construction plans and specifications.

Architectural, structural, mechanical, and electrical designs are usually excluded. Sketches may be desirable to aid in presentation of a project. Outline specifications of process units, special

equipment, etc., are occasionally included.

Engineering Reports must be completed for minor collection system, pump station, and interceptor projects. Comprehensive Facility Plans must be completed or have been completed for projects involving new, expanded, upgraded, or rehabilitated wastewater treatment facilities and major collection, interceptor sewer, and pump station projects. The determination of classification as major or minor collection interceptor sewer and pump station projects will be made by the reviewing authority based on review of recommended classification by the owner.

## **11.1 Engineering Reports**

Engineering reports shall contain the following and other pertinent information as required by the reviewing authority:

### **11.11 Problem Defined**

Description of the existing system should include an evaluation of the conditions and problems needing correction.

### **11.12 Flow and Organic Load**

The anticipated design average and design peak flows and waste load for the existing and ultimate conditions must be established. The basis of the projection of initial and future flows and waste load must be included and must reflect the existing, or initial service area, and the anticipated future service area. Flow and organic load information and data needed for new facilities are included in Paragraphs 11.24 and 11.25.

### **11.13 Impact on Existing Wastewater Facilities**

The impact of the proposed project on all existing wastewater facilities, including gravity sewers, lift stations, and treatment facilities must be evaluated.

### **11.14 Project Description**

A written description of the project is required.

### **11.15 Drawings**

Drawings identifying the site of the project and anticipated location and alignment of proposed facilities are required.

### **11.16 Engineering Criteria**

Engineering criteria to be used in design of the project shall be included.

### **11.17 Site Information**

Project site information should include topography, soils, geologic conditions, depth to bedrock, groundwater level, floodway or floodplain considerations, and other pertinent site information.

### **11.18 Alternative Selection**

The reasons for selection of the proposed alternative, including any lift station sites, feasibility, and how the project fits into a long term plan, should be

discussed.

### **11.19 Environmental Review**

Consideration should be given to minimizing any potential adverse environmental effects of the proposed project. If appropriate, compliance with planning requirements of federal, provincial, state, and local regulatory agencies shall be documented.

## **11.2 Facility Plans**

Facility Plans shall contain the following and other pertinent information as required by the reviewing authority.

### **11.21 Problem Evaluation and Existing Facility Review**

- a. Descriptions of existing system including condition and evaluation of problems needing correction.
- b. Summary of existing and previous local and regional wastewater facility and related planning documents.

### **11.22 Planning and Service Area**

Planning area and existing and potential future service area.

### **11.23 Population Projection and Planning Period**

Present and predicted population shall be based on a 20 year planning period. Phased construction of wastewater facilities should be considered in rapid growth areas. Sewers and other facilities with a design life in excess of 20 years should be designed for the extended period.

### **11.24 Hydraulic Capacity**

#### **11.241 Flow Definitions and Identification**

The following flows for the design year shall be identified and used as a basis for design for sewers, lift stations, wastewater treatment plants, treatment units, and other wastewater handling facilities. Where any of the terms defined in this Section are used in these design standards, the definition contained in this Section applies.

- a. Design Average Flow

The design average flow is the average of the daily volumes to be received for a continuous 12 month period expressed as a volume per unit time. However, the design average flow for facilities having critical seasonal high hydraulic loading periods (e.g., recreational areas, campuses, industrial facilities) shall be based on the daily average flow during the seasonal period.

- b. Design Maximum Day Flow

The design maximum day flow is the largest volume of flow to be received during a continuous 24 hour period expressed as a volume

per unit time.

c. Design Peak Hourly Flow

The design peak hourly flow is the largest volume of flow to be received during a one hour period expressed as a volume per unit time.

d. Design Peak Instantaneous Flow

The design peak instantaneous flow is the instantaneous maximum flow rate to be received.

**11.242 Hydraulic Capacity for Wastewater Facilities to serve Existing Collection Systems**

- a. Projections shall be made from actual flow data to the extent possible.
- b. The probable degree of accuracy of data and projections shall be evaluated. This reliability estimation should include an evaluation of the accuracy of existing data, as well as an evaluation of the reliability of estimates of flow reduction anticipated due to infiltration/inflow (I/I) reduction or flow increases due to elimination of sewer bypasses and backups.
- c. Critical data and methodology used shall be included. It is recommended that graphical displays of critical peak wet weather flow data (refer to Paragraphs 11.241(b) (c) and (d)) be included for a sustained wet weather flow period of significance to the project.

**11.243 Hydraulic Capacity for Wastewater Facilities to serve New Collection Systems**

- a. The sizing of wastewater facilities receiving flows from new wastewater collection systems shall be based on an average daily flow of 100 gallons (380 L) per capita plus wastewater flow from industrial plants and major institutional and commercial facilities unless water use data or other justification upon which to better estimate flow is provided.
- b. The 100 gal/cap/d [380 L/(capita·d)] figure shall be used which, in conjunction with a peaking factor from Figure 1, is intended to cover normal infiltration for systems built with modern construction techniques. Refer to Section 31. However, an additional allowance should be made where conditions are unfavorable.
- c. If the new collection system is to serve existing development the likelihood of I/I contributions from existing service lines and non-wastewater connections to those service lines shall be evaluated and wastewater facilities designed accordingly.

**11.244 Combined Sewer Interceptors**

In addition to the above requirements, interceptors for combined sewers shall have capacity to receive sufficient quantity of combined wastewater for transport to treatment facilities to ensure attainment of the appropriate water quality standards.

## 11.25 Organic Capacity

### 11.251 Organic Load Definitions and Identification

The following organic loads for the design year shall be identified and used as a basis for design of wastewater treatment facilities. Where any of the terms defined in this Section are used in these design standards, the definition contained in this Section applies.

#### a. Biochemical Oxygen Demand Defined

The 5-day Biochemical Oxygen Demand (BOD<sub>5</sub>) is defined as the amount of oxygen required to stabilize biodegradable organic matter under aerobic conditions within a five day period in accordance with Standard Methods for the Examination of Water and Wastewater. Total 5-day Biochemical Oxygen Demand (TBOD<sub>5</sub>) is equivalent to BOD<sub>5</sub> and is sometimes used in order to differentiate carbonaceous plus nitrogenous oxygen demand from strictly carbonaceous oxygen demand.

The carbonaceous 5-day Biochemical Oxygen Demand (CBOD<sub>5</sub>) is defined as BOD<sub>5</sub> less the nitrogenous oxygen demand of the wastewater. See Standard Methods for the Examination of Water and Wastewater.

#### b. Design Average BOD<sub>5</sub>

The design average BOD<sub>5</sub> is generally the average of the organic load received for a continuous 12 month period for the design year expressed as weight per day. However, the design average BOD<sub>5</sub> for facilities having critical seasonal high loading periods (e.g., recreational areas, campuses, industrial facilities) shall be based on the daily average BOD<sub>5</sub> during the seasonal period.

#### c. Design Maximum Day BOD<sub>5</sub>

The design maximum day BOD<sub>5</sub> is the largest amount of organic load to be received during a continuous 24 hour period expressed as weight per day.

#### d. Design Peak Hourly BOD<sub>5</sub>

The design peak hourly BOD<sub>5</sub> is the largest amount of organic load to be received during a one hour period expressed as weight per day.

### 11.252 Design of Organic Capacity of Wastewater Treatment Facilities to Serve Existing Collection Systems

#### a. Projections shall be made from actual wasteload data to the extent possible.

- b. Projections shall be compared to Paragraph 11.253 and an accounting made for significant variations from those values.
- c. Impact of industrial sources shall be documented. For projects with significant industrial contributions, evidence of adequate pretreatment strategies must be included along with documentation that industries are aware of the pretreatment limitations and user costs associated with the project. Documentation of the individual industrial participation in the project plan including user charges shall be provided.
- d. Septage and leachate may contribute significant organic load and other materials which can cause operational problems and non-compliance with NPDES permit limitations. If septage or leachate are to be discharged to the wastewater treatment facility, consult the state regulatory agency and the Appendix, Handling and Treatment of Septage at a Wastewater Treatment Plant.

### **11.253 Organic Capacity of Wastewater Treatment Facilities to Serve New Collection Systems**

- a. Domestic waste treatment design shall be on the basis of at least 0.17 pounds (0.08 kg) of BOD<sub>5</sub> per capita per day and 0.20 pounds (0.09 kg) of suspended solids per capita per day, unless information is submitted to justify alternate designs.
- b. Where garbage grinders are commonly used in areas tributary to a domestic treatment plant, the design basis should be increased to 0.22 pounds (0.10 kg) of BOD<sub>5</sub> per capita per day and 0.25 pounds (0.11 kg) of suspended solids per capita per day.
- c. Industrial contributions. Refer to Paragraph 11.252(c).
- d. Septage and Leachate. Refer to Paragraph 11.252(d).
- e. Data from similar municipalities may be utilized in the case of new systems. However, thorough investigation that is adequately documented shall be provided to the reviewing authority to establish the reliability and applicability of such data.

### **11.26 Wastewater Treatment Facility Design Capacity**

The wastewater treatment facility design capacity is the design average flow at the design average BOD<sub>5</sub>. Refer to Paragraphs 11.24 and 11.25 for peaking factors that will be required.

### **11.27 Initial Alternative Development**

The process of selection of wastewater treatment alternatives for detailed evaluation should be discussed. All wastewater management alternatives considered, including no action, and the basis for the engineering judgement for selection of the alternatives chosen for detailed evaluation, should be included.

### **11.28 Detailed Alternative Evaluation**

The following shall be included for the alternatives to be evaluated in detail.

a. Sewer System Revisions

Proposed revisions to the existing sewer system including adequacy of portions not being changed by the project.

b. Wet Weather Flows

Facilities to transport and treat wet weather flows in a manner that complies with state and local regulations must be provided.

c. Site Evaluation

When a site must be used which is critical with respect to these items, appropriate measures shall be taken to minimize adverse impacts.

1. Compatibility of the treatment process with the present and planned future land use, including noise, potential odors, air quality, and anticipated sludge processing and disposal techniques, shall be considered.

Non-aerated lagoons should not be used if excessive sulfate is present in the wastewater.

Wastewater treatment facilities should be separate from habitation or any area likely to be built up within a reasonable future period and shall be separated in accordance with state and local requirements.

2. Zoning and other land use restrictions shall be identified.
3. An evaluation of the accessibility and topography of the site shall be submitted.
4. Area for future plant expansion shall be identified.
5. Direction of prevailing wind shall be identified.
6. Flood considerations, including the 25 and 100 year flood levels, impact on floodplain and floodway, and compliance with applicable regulations regarding construction in flood-prone areas, shall be evaluated. Paragraph 51.2 contains requirements for protection from flooding.
7. Geologic information, depth to bedrock, karst features, or other geologic considerations of significance to the project shall be included. Lagoons shall not be located in karst areas unless the specific geologic and construction details are acceptable.
8. Protection of groundwater including public and private wells is of utmost importance. Demonstration that protection will be provided must be included. The regulatory agency shall be contacted for required separation.
9. Soil type and suitability for construction and depth to normal and seasonal high groundwater shall be determined.

10. The location, depth, and discharge point of any field tile in the immediate area of the proposed site shall be identified.
  11. Present and known future effluent quality requirements determined by the regulatory agency shall be included.
  12. Access to receiving stream for the outfall line shall be discussed and displayed.
  13. A preliminary assessment of site availability shall be included.
- d. Unit Sizing
- Unit operation and unit process sizing and basis shall be provided.
- e. Flow Diagram
- Flow diagram of treatment facilities including all recycle flows.
- f. Emergency Operation
- Emergency operation requirements as outlined in Section 46 and Paragraph 56.1 shall be provided. State or local regulatory agencies may have more stringent requirements.
- g. Technology Not Included In These Standards
- Paragraph 53.2 outlines procedures for introducing and obtaining approval to use technology not included in these standards. Proposals to use technology not included in these standards must address the requirements of Paragraph 53.2.
- h. Sludge
- The solids disposal options considered and method selected must be included. This is critical to completion of a successful project. Compliance with requirements of Chapter 80, Sludge Processing, Storage, and Disposal must be assured.
- i. Treatment During Construction
- A plan for the method and level of treatment to be achieved during construction shall be developed and included in the facility plan that must be submitted to the regulatory agency for review and approval. This approved treatment plan must be implemented by inclusion in the plans and specifications to be bid for the project. Refer to Paragraph 20.15 and Section 21.
- j. Operation and Maintenance
- Portions of the project which involve complex operation or maintenance requirements shall be identified including laboratory requirements for operation, industrial sampling, and self monitoring.
- k. Cost Estimates

Cost estimates for capital and operation and maintenance (including basis), must be included.

1. Environmental Review

Consideration must be given to minimizing any potential adverse environmental effects of the proposed project. Compliance with planning requirements of federal, provincial, state, and local regulatory agencies must be documented.

### **11.29 Final Project Selection**

The project selected from the alternatives considered under Paragraph 11.28 shall be set forth in the final facility plan document to be forwarded to the reviewing authority for review and approval, including the financing considerations and recommendations for implementation of the plan.

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## **CHAPTER 20**

### **ENGINEERING PLANS AND SPECIFICATIONS**

#### **20. PLANS AND SUPPORT DOCUMENTS**

Submissions to the reviewing authority shall include sealed plans, design criteria, the appropriate construction permit applications, review forms, and permit fee if required.

##### **20.1 General**

###### **20.11 Plan Title**

All plans for wastewater facilities shall bear a suitable title showing the name of the municipality, sewer district, or institution. They shall show the scale in feet or metric measure, a graphical scale, the north point, date, and the name and signature of the engineer, with the certificate number and imprint of the professional engineering seal. A space should be provided for signature and/or approval stamp of the appropriate reviewing authority.

###### **20.12 Plan Format**

The plans shall be clear and legible (suitable for microfilming). They shall be drawn to a scale which will permit all necessary information to be plainly shown. Generally, the size of the plans should not be larger than 30 inches x 42 inches (760 mm x 1070 mm). Datum used should be indicated. Locations and logs of test borings, when required, shall be shown on the plans. Blueprints shall not be submitted.

###### **20.13 Plan Contents**

Detail plans shall consist of: plan views, elevations, sections, and supplementary views which, together with the specifications and general layouts, provide the working information for the contract and construction of the facilities. They shall also include: dimensions and relative elevations of structures, the location and outline form of equipment, location and size of piping, water levels, and ground elevations.

###### **20.14 Design Criteria**

Design criteria shall be included with all plans and specifications and a hydraulic profile shall be included for all wastewater treatment facilities. For sewer and lift station projects, information shall be submitted to verify adequate downstream sewer, pump station and treatment plant capacity.

###### **20.15 Operation During Construction**

Project construction documents shall specify the procedure for operation during construction that complies with the plan required by Paragraph 11.28(i), Treatment During Construction.

##### **20.2 Plans of Sewers**

###### **20.21 General Plan**

A plan of proposed and existing sewers shall be submitted for projects involving new sewer systems and substantial additions to existing systems. This plan shall

show the following:

### **20.211 Geographical Features**

- a. Topography and elevations - Existing or proposed streets and all streams or water surfaces shall be clearly shown. Contour lines at suitable intervals should be included.
- b. Streams - The direction of flow in all streams, and high and low water elevations of all water surfaces at sewer outlets and overflows shall be shown.
- c. Boundaries - The boundary lines of the municipality or the sewer district, and the area to be sewered, shall be shown.

### **20.212 Sewers**

The plan shall show the location, size, and direction of flow of relevant existing and proposed sanitary and combined sewers draining to the treatment facility concerned.

### **20.22 Detail Plans**

Detail plans shall be submitted. Profiles should have a horizontal scale of not more than 100 feet to the inch (1200:1) and a vertical scale of not more than 10 feet to the inch (120:1). Plan views should be drawn to a corresponding horizontal scale and must be shown on the same sheet. Plans and profiles shall show:

- a. Location of streets and sewers;
- b. Line of ground surface; size, material, and type of pipe; length between manholes; invert and surface elevation at each manhole; and grade of sewer between each two adjacent manholes (all manholes shall be numbered on the profile);

Where there is any question of the sewer being sufficiently deep to serve any residence, the elevation and location of the basement floor shall be plotted on the profile of the sewer which is to serve the house in question. The engineer shall state that all sewers are sufficiently deep to serve adjacent basements except where otherwise noted on the plans;

- c. Locations of all special features such as inverted siphons, concrete encasements, elevated sewers, etc.;
- d. All known existing structures and utilities, both above and below ground, which might interfere with the proposed construction or require isolation setback, particularly water mains and water supply structures (i.e., wells, clear wells, basins, etc.), gas mains, storm drains, and telephone and power conduits; and
- e. Special detail drawings, made to a scale to clearly show the nature of the design, shall be furnished to show the following particulars:

All stream crossings and sewer outlets, with elevations of the stream bed and high, normal and low water levels;

Details of all special sewer joints and cross-sections; and details of all sewer appurtenances such as manholes, lampholes, inspection chambers, inverted siphons, regulators, tide gates, and elevated sewers.

## **20.3 Plans of Wastewater Pumping Stations**

### **20.31 Location Plan**

A plan shall be submitted for projects involving construction or revision of pumping stations. This plan shall show the following:

- a. The location and extent of the tributary area;
- b. Any municipal boundaries within the tributary area; and
- c. The location of the pumping station and force main, and pertinent elevations.

### **20.32 Detail Plans**

Detail plans shall be submitted showing the following, where applicable:

- a. Topography of the site;
- b. Existing pumping station;
- c. Proposed pumping station, including provisions for installation of future pumps;
- d. Elevation of high water at the site, and maximum elevation of wastewater in the collection system upon occasion of power failure;
- e. Maximum hydraulic gradient in downstream gravity sewers when all installed pumps are in operation; and
- f. Test borings and groundwater elevations.

## **20.4 Plans of Wastewater Treatment Plants**

### **20.41 Location Plan**

A plan shall be submitted showing the wastewater treatment plant in relation to the remainder of the system.

Sufficient topographic features shall be included to indicate its location with relation to streams and the point of discharge of treated effluent.

### **20.42 General Layout**

Layouts of the proposed wastewater treatment plant shall be submitted, showing:

- a. Topography of the site;
- b. Size and location of plant structures;

- c. Schematic flow diagram(s) showing the flow through various plant units, and showing utility systems serving the plant processes;
- d. Piping, including any arrangements for bypassing individual units (materials handled and direction of flow through pipes shall be shown);
- e. Hydraulic profiles showing the flow of wastewater, supernatant liquor, and sludge; and
- f. Test borings and groundwater elevations.

### **20.43 Detail Plans**

Detail plans shall show the following, where applicable:

- a. Location, dimensions, and elevations of all existing and proposed plant facilities;
- b. Elevations of high and low water level of the body of water to which the plant effluent is to be discharged;
- c. Type, size, pertinent features, and operating capacity of all pumps, blowers, motors, and other mechanical devices;
- d. Minimum, design average, and peak hourly hydraulic flow in profile; and
- e. Adequate description of any features not otherwise covered by specifications or engineer's report.

## **21. SPECIFICATIONS**

Complete signed and sealed technical specifications (see Paragraph 20.11) shall be submitted for the construction of sewers, wastewater pumping stations, wastewater treatment plants, and all other appurtenances, and shall accompany the plans.

The specifications accompanying construction drawings shall include, but not be limited to, specifications for the approved procedures for operation during construction in accordance with Paragraphs 11.28(i) and 20.15, all construction information not shown on the drawings which is necessary to inform the builder in detail of the design requirements for the quality of materials, workmanship, and fabrication of the project.

The specifications shall also include: the type, size, strength, operating characteristics, and rating of equipment; allowable infiltration; the complete requirements for all mechanical and electrical equipment, including machinery, valves, piping, and jointing of pipe; electrical apparatus, wiring, instrumentation, and meters; laboratory fixtures and equipment; operating tools, construction materials; special filter materials, such as, stone, sand, gravel, or slag; miscellaneous appurtenances; chemicals when used; instructions for testing materials and equipment as necessary to meet design standards; and performance tests for the completed facilities and component units. It is suggested that these performance tests be conducted at design load conditions wherever practical.

## **22. REVISIONS TO APPROVED PLANS**

Any deviations from approved plans or specifications affecting capacity, flow, operation of units, or point of discharge shall be approved, in writing, before such changes are made. Plans or specifications so revised should, therefore, be submitted well in advance of any construction work which will be

affected by such changes to permit sufficient time for review and approval. Structural revisions or other minor changes not affecting capacities, flows, or operation will be permitted during construction without approval. "As built" plans clearly showing such alterations shall be submitted to the reviewing authority at the completion of the work.

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## CHAPTER 30 DESIGN OF SEWERS

### 31. APPROVAL OF SEWERS

In general, the appropriate reviewing authority will approve plans for new systems, extensions to new areas, or replacement sanitary sewers only when designed upon the separate basis, in which rain water from roofs, streets, and other areas, and groundwater from foundation drains, are excluded.

### 32. DESIGN CAPACITY AND DESIGN FLOW

In general, sewer capacities should be designed for the estimated ultimate tributary population, except in considering parts of the systems that can be readily increased in capacity. Similarly, consideration should be given to the maximum anticipated capacity of institutions, industrial parks, etc. Where future relief sewers are planned, economic analysis of alternatives should accompany initial permit applications. See Paragraph 11.24.

### 33. DETAILS OF DESIGN AND CONSTRUCTION

#### 33.1 Minimum Size

No public gravity sewer conveying raw wastewater shall be less than 8 inches (200 mm) in diameter.

#### 33.2 Depth

In general, sewers should be sufficiently deep to receive wastewater from basements and to prevent freezing. Insulation shall be provided for sewers that cannot be placed at a depth sufficient to prevent freezing.

#### 33.3 Buoyancy

Buoyancy of sewers shall be considered and flotation of the pipe shall be prevented with appropriate construction where high groundwater conditions are anticipated.

#### 33.4 Slope

##### 33.41 Recommended Minimum Slopes

All sewers shall be designed and constructed to give mean velocities, when flowing full, of not less than 2.0 feet per second (0.6 m/s), based on Manning's formula using an "n" value of 0.013. The following are the recommended minimum slopes which should be provided for sewers 42 inches (1050 mm) or less; however, slopes greater than these may be desirable for construction, to control sewer gases or to maintain self-cleansing velocities at all rates of flow within the design limits.

Nominal Sewer Size	Minimum Slope in Feet Per 100 Feet (m/100 m)
8 inch (200 mm)	0.40
10 inch (250 mm)	0.28
12 inch (300 mm)	0.22
14 inch (350 mm)	0.17

15 inch (375 mm)	0.15
16 inch (400 mm)	0.14
18 inch (450 mm)	0.12
21 inch (525 mm)	0.10
24 inch (600 mm)	0.08
27 inch (675 mm)	0.067
30 inch (750 mm)	0.058
33 inch (825 mm)	0.052
36 inch (900 mm)	0.046
39 inch (975 mm)	0.041
42 inch (1050 mm)	0.037

Sewers 48 inches (1200 mm) or larger should be designed and constructed to give mean velocities, when flowing full, of not less than 3.0 feet per second (0.9 m/s), based on Manning's formula using an "n" value of 0.013.

#### **33.42 Minimum Flow Depths**

Slopes which are slightly less than the recommended minimum slopes may be permitted. Such decreased slopes may be considered where the depth of flow will be 0.3 of the diameter or greater for design average flow. The operating authority of the sewer system will give written assurance to the appropriate reviewing authority that any additional sewer maintenance required by reduced slopes will be provided.

#### **33.43 Minimize Solids Deposition**

The pipe diameter and slope shall be selected to obtain the greatest practical velocities to minimize settling problems. Oversize sewers will not be approved to justify using flatter slopes. If the proposed slope is less than the minimum slope of the smallest pipe which can accommodate the design peak hourly flow, the actual depths and velocities at minimum, average, and design maximum day and peak hourly flow for each design section of the sewer shall be calculated by the design engineer and be included with the plans.

#### **33.44 Slope Between Manholes**

Sewers shall be laid with uniform slope between manholes.

#### **33.45 High Velocity Protection**

Where velocities greater than 15 feet per second (4.6 m/s) are attained, special provision shall be made to protect against displacement by erosion and impact.

#### **33.46 Steep Slope Protection**

Sewers on 20 percent slopes or greater shall be anchored securely with concrete, or equal, anchors spaced as follows:

- a. Not over 36 feet (11 m) center to center on grades 20 percent and up to 35 percent;

- b. Not over 24 feet (7.3 m) center to center on grades 35 percent and up to 50 percent; and
- c. Not over 16 feet (4.9 m) center to center on grades 50 percent and over.

### **33.5 Alignment**

In general, sewers 24 inches (600 mm) or less shall be laid with straight alignment between manholes. Straight alignment shall be checked by either using a laser beam or lamping.

Curvilinear alignment of sewers larger than 24 inches (600 mm) may be considered on a case by case basis provided compression joints are specified and ASTM or specific pipe manufacturers' maximum allowable pipe joint deflection limits are not exceeded. Curvilinear sewers shall be limited to simple curves which start and end at manholes. When curvilinear sewers are proposed, the recommended minimum slopes indicated in Paragraph 33.41 must be increased accordingly to provide a minimum velocity of 2.0 feet per second (0.6 m/s) when flowing full.

### **33.6 Changes in Pipe Size**

When a smaller sewer joins a large one, the invert of the larger sewer should be lowered sufficiently to maintain the same energy gradient. An approximate method for securing these results is to place the 0.8 depth point of both sewers at the same elevation.

Sewer extensions should be designed for projected flows even when the diameter of the receiving sewer is less than the diameter of the proposed extension at a manhole constructed in accordance with Section 34 with special consideration of an appropriate flow channel to minimize turbulence when there is a change in sewer size. The appropriate reviewing authority may require a schedule for construction of future downstream sewer relief.

### **33.7 Materials**

Any generally accepted material for sewers will be given consideration, but the material selected should be adapted to local conditions, such as: character of industrial wastes, possibility of septicity, soil characteristics, exceptionally heavy external loadings, abrasion, corrosion, and similar problems.

Suitable couplings complying with ASTM specifications shall be used for joining dissimilar materials. The leakage limitations on these joints shall be in accordance with Paragraphs 33.94 or 33.95.

All sewers shall be designed to prevent damage from superimposed live, dead, and frost induced loads. Proper allowance for loads on the sewer shall be made because of soil and potential groundwater conditions, as well as the width and depth of trench. Where necessary, special bedding, haunching and initial backfill, concrete cradle, or other special construction shall be used to withstand anticipated potential superimposed loading or loss of trench wall stability. See ASTM D 2321 or ASTM C 12 when appropriate.

For new pipe materials for which ASTM standards have not been established, the design engineer shall provide complete pipe specifications and installation specifications developed on the basis of criteria adequately documented and certified in writing by the pipe manufacturer to be satisfactory for the specific detailed plans.

## **33.8 Installation**

### **33.81 Standards**

Installation specifications shall contain appropriate requirements based on the criteria, standards, and requirements established by industry in its technical publications. Requirements shall be set forth in the specifications for the pipe and methods of bedding and backfilling thereof so as not to damage the pipe or its joints, impede cleaning operations and future tapping, nor create excessive side fill pressures and ovalation of the pipe, nor seriously impair flow capacity.

### **33.82 Trenching**

- a. The width of the trench shall be ample to allow the pipe to be laid and jointed properly and to allow the bedding and haunching to be placed and compacted to adequately support the pipe. The trench sides shall be kept as nearly vertical as possible. When wider trenches are specified, appropriate bedding class and pipe strength shall be used.

In unsupported, unstable soil the size and stiffness of the pipe, stiffness of the embedment and insitu soil and depth of cover shall be considered in determining the minimum trench width necessary to adequately support the pipe.

- b. Ledge rock, boulders, and large stones shall be removed to provide a minimum clearance of 4 inches (100 mm) below and on each side of all pipe(s).

### **33.83 Bedding, Haunching, and Initial Backfill**

- a. Bedding Classes A, B, C, or crushed stone as described in ASTM C 12 shall be used and carefully compacted for all rigid pipe provided the proper strength pipe is used with the specified bedding to support the anticipated load, based on the type soil encountered and potential ground water conditions.
- b. Embedment materials for bedding, haunching and initial backfill, Classes I, II, or III, as described in ASTM D 2321, shall be used and carefully compacted for all flexible pipe provided the proper strength pipe is used with the specified bedding to support the anticipated load, based on the type soil encountered and potential groundwater conditions.
- c. All water entering the excavations or other parts of the work shall be removed until all the work has been completed. No sanitary sewer shall be used for the disposal of trench water, unless specifically approved by the engineer, and then only if the trench water does not ultimately arrive at existing pumping or wastewater treatment facilities.

### **33.84 Final Backfill**

- a. Final backfill shall be of a suitable material removed from excavation except where other material is specified. Debris, frozen material, large clods or stones, organic matter, or other unstable materials shall not be used for final backfill within 2 feet (0.6 m) of the top of the pipe.

- b. Final backfill shall be placed in such a manner as not to disturb the alignment of the pipe.

### **33.85 Deflection Test**

- a. Deflection tests shall be performed on all flexible pipe. The test shall be conducted after the final backfill has been in place at least 30 days to permit stabilization of the soil-pipe system.
- b. No pipe shall exceed a deflection of 5 percent. If deflection exceeds 5 percent, the pipe shall be excavated. Replacement or correction shall be accomplished in accordance with requirements in the approved specifications.
- c. The rigid ball or mandrel used for the deflection test shall have a diameter not less than 95 percent of the base inside diameter or average inside diameter of the pipe depending on which is specified in the ASTM Specification, including the appendix, to which the pipe is manufactured. The test shall be performed without mechanical pulling devices.

## **33.9 Joints and Infiltration**

### **33.91 Joints**

The installation of joints and the materials used shall be included in the specifications. Sewer joints shall be designed to minimize infiltration and to prevent the entrance of roots throughout the life of the system.

### **33.92 Service Connections**

Service connections to the sewer main shall be water tight and not protrude into the sewer. If a saddle type connection is used, it shall be a device designed to join with the types of pipe which are to be connected. All materials used to make service connections shall be compatible with each other and with the pipe materials to be joined and shall be corrosion proof.

### **33.93 Leakage Tests**

Leakage tests shall be specified. This may include appropriate water or low pressure air testing. The testing methods selected should take into consideration the range in groundwater elevations during the test and anticipated during the design life of the sewer.

### **33.94 Water (Hydrostatic) Test**

The leakage exfiltration or infiltration shall not exceed 100 gallons per inch of pipe diameter per mile per day [9 L/(mm of pipe diameter·km·d)] for any section of the system. An exfiltration or infiltration test shall be performed with a minimum positive head of 2 feet (0.6 m).

### **33.95 Air test**

The air test shall, as a minimum, conform to the test procedure described in ASTM C 828 for clay pipe, ASTM C 924 for concrete pipe, ASTM F 1417 for plastic pipe, and for other materials test procedures approved by the regulatory

agency.

## **34. MANHOLES**

### **34.1 Location**

Manholes shall be installed: at the end of each line; at all changes in grade, size, or alignment; at all intersections; and at distances not greater than 400 feet (120 m) for sewers 15 inches (375 mm) or less, and 500 feet (150 m) for sewers 18 inches (450 mm) to 30 inches (750 mm), except that distances up to 600 feet (185 m) may be approved in cases where adequate modern cleaning equipment for such spacing is provided. Greater spacing may be permitted in larger sewers. Cleanouts may be used only for special conditions and shall not be substituted for manholes nor installed at the end of laterals greater than 150 feet (45 m) in length.

### **34.2 Drop Type**

A drop pipe shall be provided for a sewer entering a manhole at an elevation of 24 inches (610 mm) or more above the manhole invert. Where the difference in elevation between the incoming sewer and the manhole invert is less than 24 inches (610 mm), the invert shall be filleted to prevent solids deposition.

Drop manholes should be constructed with an outside drop connection. Inside drop connections (when necessary) shall be secured to the interior wall of the manhole and provide access for cleaning.

Due to the unequal earth pressures that would result from the backfilling operation in the vicinity of the manhole, the entire outside drop connection shall be encased in concrete.

### **34.3 Diameter**

The minimum diameter of manholes shall be 48 inches (1200 mm); larger diameters are preferable for large diameter sewers. A minimum access diameter of 24 inches (610 mm) shall be provided.

### **34.4 Flow Channel**

The flow channel straight through a manhole should be made to conform as closely as possible in shape, and slope to that of the connecting sewers. The channel walls should be formed or shaped to the full height of the crown of the outlet sewer in such a manner to not obstruct maintenance, inspection or flow in the sewers.

When curved flow channels are specified in manholes, including branch inlets, minimum slopes indicated in Paragraph 33.41 should be increased to maintain acceptable velocities.

### **34.5 Bench**

A bench shall be provided on each side of any manhole channel when the pipe diameter (s) are less than the manhole diameter. The bench should be sloped no less than ½ inch per foot (40 mm/m) (4 percent). No lateral sewer, service connection, or drop manhole pipe shall discharge onto the surface of the bench.

### **34.6 Watertightness**

Manholes shall be of the pre-cast concrete or poured-in-place concrete type. Manhole lift holes and grade adjustment rings shall be sealed with non-shrinking mortar or other

material approved by the regulatory agency.

Inlet and outlet pipes shall be joined to the manhole with a gasketed flexible watertight connection or any watertight connection arrangement that allows differential settlement of the pipe and manhole wall to take place.

Watertight manhole covers are to be used wherever the manhole tops may be flooded by street runoff or high water. Locked manhole covers may be desirable in isolated easement locations or where vandalism may be a problem.

### **34.7 Inspection and Testing**

The specifications shall include a requirement for inspection and testing for watertightness or damage prior to placing into service. Air testing, if specified for concrete sewer manholes, shall conform to the test procedures described in ASTM C 1244.

### **34.8 Corrosion Protection For Manholes**

Where corrosive conditions due to septicity or other causes are anticipated, corrosion protection on the interior of the manholes shall be provided.

### **34.9 Electrical**

Electrical equipment installed or used in manholes shall conform to Paragraph 42.35.

## **35. INVERTED SIPHONS**

Inverted siphons shall have not less than two barrels, with a minimum pipe size of 6 inches (150 mm). They shall be provided with necessary appurtenances for maintenance, convenient flushing, and cleaning equipment. The inlet and discharge structures shall have adequate clearances for cleaning equipment, inspection, and flushing. Design shall provide sufficient head and appropriate pipe sizes to secure velocities of at least 3.0 feet per second (0.9 m/s) for design average flows. The inlet and outlet details shall be so arranged that the design average flow is diverted to one barrel, and so that either barrel may be cut out of service for cleaning. The vertical alignment should permit cleaning and maintenance.

## **36. SEWERS IN RELATION TO STREAMS**

### **36.1 Location of Sewers in Streams**

#### **36.11 Cover Depth**

The top of all sewers entering or crossing streams shall be at a sufficient depth below the natural bottom of the stream bed to protect the sewer line. In general, the following cover requirements must be met:

- a. One foot (0.3 m) of cover where the sewer is located in rock;
- b. Three feet (0.9 m) of cover in other material. In major streams, more than 3 feet (0.9 m) of cover may be required; and
- c. In paved stream channels, the top of the sewer line should be placed below the bottom of the channel pavement.

Less cover may be approved only if the proposed sewer crossing will not interfere

with future modifications to the stream channel. Justification for requesting less cover shall be provided to the reviewing authority.

### **36.12 Horizontal Location**

Sewers located along streams shall be located outside of the stream bed and sufficiently removed therefrom to provide for future possible stream widening and to prevent pollution by siltation during construction.

### **36.13 Structures**

The sewer outfalls, headwalls, manholes, gate boxes, or other structures shall be located so they do not interfere with the free discharge of flood flows of the stream.

### **36.14 Alignment**

Sewers crossing streams should be designed to cross the stream as nearly perpendicular to the stream flow as possible and shall be free from change in grade. Sewer systems shall be designed to minimize the number of stream crossings.

## **36.2 Construction**

### **36.21 Materials**

Sewers entering or crossing streams shall be constructed of ductile iron pipe with mechanical joints; otherwise they shall be constructed so they will remain watertight and free from changes in alignment or grade. Material used to backfill the trench shall be stone, coarse aggregate, washed gravel, or other materials which will not readily erode, cause siltation, damage pipe during placement, or corrode the pipe.

### **36.22 Siltation and Erosion**

Construction methods that will minimize siltation and erosion shall be employed. The design engineer shall include in the project specifications the method(s) to be employed in the construction of sewers in or near streams. Such methods shall provide adequate control of siltation and erosion by limiting unnecessary excavation, disturbing or uprooting trees and vegetation, dumping of soil or debris, or pumping silt-laden water into the stream. Specifications shall require that cleanup, grading, seeding, and planting or restoration of all work areas shall begin immediately. Exposed areas shall not remain unprotected for more than seven days.

## **37. AERIAL CROSSINGS**

Support shall be provided for all joints in pipes utilized for aerial crossings. The supports shall be designed to prevent frost heave, overturning, and settlement.

Precautions against freezing, such as insulation and increased slope, shall be provided. Expansion jointing shall be provided between above ground and below ground sewers. Where buried sewers change to aerial sewers, special construction techniques shall be used to minimize frost heaving.

For aerial stream crossings, the impact of flood waters and debris shall be considered. The

bottom of the pipe should be placed no lower than the elevation of the 50 year flood. Ductile iron pipe with mechanical joints is recommended.

## **38. PROTECTION OF WATER SUPPLIES**

When wastewater sewers are proposed in the vicinity of any water supply facilities, requirements of the GLUMRB "Recommended Standards for Water Works" should be used to confirm acceptable isolation distances in addition to the following requirements.

### **38.1 Cross Connections Prohibited**

There shall be no physical connections between a public or private potable water supply system and a sewer, or appurtenance thereto which would permit the passage of any wastewater or polluted water into the potable supply. No water pipe shall pass through or come into contact with any part of a sewer manhole.

### **38.2 Relation to Water Works Structures**

While no general statement can be made to cover all conditions, it is generally recognized that sewers shall meet the requirements of the appropriate reviewing agency with respect to minimum distances from public water supply wells or other water supply sources and structures.

All existing waterworks units, such as basins, wells, or other treatment units, within 200 feet (60 m) of the proposed sewer shall be shown on the engineering plans.

Soil conditions in the vicinity of the proposed sewer within 200 feet (60 m) of waterworks units shall be determined and shown on the engineering plans.

### **38.3 Relation to Water Mains**

#### **38.31 Horizontal and Vertical Separation**

Sewers shall be laid at least 10 feet (3 m) horizontally from any existing or proposed water main. The distance shall be measured edge to edge. For gravity sewers where it is not practical to maintain a 10 foot (3 m) separation, the appropriate reviewing agency may allow deviation on a case-by-case basis, if supported by data from the design engineer. Such deviation may allow installation of the gravity sewer closer to a water main, provided that the water main is in a separate trench or on an undisturbed earth shelf located on one side of the gravity sewer and at an elevation so the bottom of the water main is at least 18 inches (460 mm) above the top of the sewer.

If it is impossible to obtain proper horizontal and vertical separation as described above for gravity sewers, both the water main and gravity sewer must be constructed of slip-on or mechanical joint pipe complying with public water supply design standards of the agency and be pressure tested to 150 psi (1034 kPa) to assure watertightness.

#### **38.32 Crossings**

Sewers crossing water mains shall be laid to provide a minimum vertical distance of 18 inches (460 mm) between the outside of the water main and the outside of the sewer. This shall be the case where the water main is either above or below the sewer. The crossing shall be arranged so that the sewer joints will be equidistant and as far as possible from the water main joints. Where a water main

crosses under a sewer, adequate structural support shall be provided for the sewer to maintain line and grade.

When it is impossible to obtain proper horizontal and vertical separation as stipulated above, one of the following methods must be specified:

- a. The sewer shall be designed and constructed equal to water pipe, and shall be pressure tested at 150 psi (1034 kPa) to assure watertightness.
- b. Either the water main or the sewer line may be encased in a watertight carrier pipe which extends 10 feet (3 m) on both sides of the crossing, measured perpendicular to the water main. The carrier pipe shall be of materials approved by the regulatory agency for use in water main construction.

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## **CHAPTER 40 WASTEWATER PUMPING STATIONS**

### **41 GENERAL**

#### **41.1 Flooding**

Wastewater pumping station structures and electrical and mechanical equipment shall be protected from physical damage by the 100 year flood. Wastewater pumping stations should remain fully operational and accessible during the 25 year flood. Regulations of state, provincial and federal agencies regarding flood plain obstructions shall be considered.

#### **41.2 Accessibility and Security**

The pumping station shall be readily accessible by maintenance vehicles during all weather conditions. The facility should be located off the traffic way of streets and alleys. It is recommended that security fencing and access hatches with locks be provided.

#### **41.3 Grit**

Where it is necessary to pump wastewater prior to grit removal, the design of the wet well and pump station piping shall receive special consideration to avoid operational problems from the accumulation of grit.

#### **41.4 Safety**

Adequate provision shall be made to effectively protect maintenance personnel from hazards. Equipment for confined space entry in accordance with OSHA and regulatory agency requirements shall be provided for all wastewater pumping stations. Also refer to Section 57.

### **42 DESIGN**

The following items should be given consideration in the design of wastewater pumping stations:

#### **42.1 Type**

Wastewater pumping stations in general use fall into four types: wet well/dry well, submersible, suction lift, and screw pump.

#### **42.2 Structures**

##### **42.21 Separation**

Dry wells, including their superstructure, shall be completely separated from the wet well. Common walls must be gas tight.

##### **42.22 Equipment Removal**

Provision shall be made to facilitate removing pumps, motors, and other mechanical and electrical equipment. Individual pump and motor removal must not interfere with the continued operation of remaining pumps.

##### **42.23 Access and Safety Landings**

**42.231 Access**

Suitable and safe means of access for persons wearing self-contained breathing apparatus shall be provided to dry wells, and to wet wells. Access to wet wells containing either bar screens or mechanical equipment requiring inspection or maintenance shall conform to Paragraph 61.13. Also refer to Section 57.

**42.232 Safety Landings**

For built-in-place pump stations, a stairway to the dry well shall be provided with rest landings at vertical intervals not to exceed 12 feet (3.7 m). For factory-built pump stations over 15 feet (4.6 m) deep, a rigidly fixed landing shall be provided at vertical intervals not to exceed 10 feet (3 m). Where a landing is used, a suitable and rigidly fixed barrier shall be provided to prevent an individual from falling past the intermediate landing to a lower level. A manlift or elevator may be used in lieu of landings in a factory-built station, provided emergency access is included in the design.

**42.24 Buoyancy**

Where high groundwater conditions are anticipated, buoyancy of the wastewater pumping station structures shall be considered and, if necessary, adequate provisions shall be made for protection.

**42.25 Construction Materials**

Materials shall be selected that are appropriate under conditions of exposure to hydrogen sulfide and other corrosive gases, greases, oils, and other constituents frequently present in wastewater. This is particularly important in the selection of metals and paints. Contact between dissimilar metals should be avoided or other provisions made to minimize galvanic action.

**42.3 Pumps****42.31 Multiple Units**

Multiple pumps shall be provided. Where only two units are provided, they shall be of the same size. Units shall have capacity such that, with any unit out of service, the remaining units will have capacity to handle the design peak hourly flow. All pumps should be tested by the manufacturer. These tests should include a hydrostatic test and an operating test.

**42.32 Protection Against Clogging****42.321 Combined Wastewater**

Pumps handling combined wastewater shall be preceded by readily accessible bar racks to protect the pumps from clogging or damage. Bar racks should have clear openings as provided in Paragraph 61.121. Where a bar rack is provided, a mechanical hoist shall also be provided. Where the size of the installation warrants, mechanically cleaned and/or duplicate bar racks shall be provided. Refer to Paragraphs 42.23 and 61.13.

### **42.322 Separate Sanitary Wastewater**

Pumps handling separate sanitary wastewater from 30 inch (750 mm) or larger diameter sewers shall be protected by bar racks meeting the above requirements. Appropriate protection from clogging shall also be considered for small pumping stations. Refer to Paragraphs 42.23 and 61.13.

### **42.33 Pump Openings**

Pumps handling raw wastewater shall be capable of passing spheres of at least 3 inches (80 mm) in diameter. Pump suction and discharge openings shall be at least 4 inches (100 mm) in diameter.

### **42.34 Priming**

The pump shall be so placed that under normal operating conditions it will operate under a positive suction head, except as specified in Section 43.

### **42.35 Electrical Equipment**

Electrical systems and components (e.g., motors, lights, cables, conduits, switch boxes, control circuits, etc.) in raw wastewater wet wells, or in enclosed or partially enclosed spaces where hazardous concentrations of flammable gases or vapors may be present, shall comply with the National Electrical Code requirements for Class I, Division 1, Group D locations. In addition, equipment located in the wet well shall be suitable for use under corrosive conditions. Each flexible cable shall be provided with a watertight seal and separate strain relief. A fused disconnect switch located above ground shall be provided for the main power feed for all pumping stations. When such equipment is exposed to weather, it shall meet the requirements of weatherproof equipment NEMA 3R or 4. Lightning and surge protection systems should be considered. A 110 volt power receptacle to facilitate maintenance shall be provided inside the control panel for lift stations that have control panels outdoors. Ground Fault Circuit Interruption (GFCI) protection shall be provided for all outdoor outlets.

### **42.36 Intake**

Each pump shall have an individual intake. Wet well and intake design should be such as to avoid turbulence near the intake and to prevent vortex formation.

### **42.37 Dry Well Dewatering**

A sump pump equipped with dual check valves shall be provided in the dry well to remove leakage or drainage with discharge above the maximum high water level of the wet well. Water ejectors connected to a potable water supply will not be approved. All floor and walkway surfaces should have an adequate slope to a point of drainage. Pump seal leakage shall be piped or channeled directly to the sump. The sump pump shall be sized to remove the maximum pump seal water discharge which would occur in the event of a pump seal failure. Refer to Section 46.

### **42.38 Pumping Rates**

The pumps and controls of main pumping stations, and especially pumping

stations operated as part of treatment facilities, should be selected to operate at varying delivery rates. Insofar as is practicable, such stations should be designed to deliver as uniform a flow as practicable in order to minimize hydraulic surges. The station design capacity shall be based on peak hourly flow as determined in accordance with Paragraph 11.24 and should be adequate to maintain a minimum velocity of 2 feet per second (0.6 m/s) in the force main. Refer to Paragraph 49.1.

#### **42.4 Controls**

Water level control sensing devices should be so located as not to be unduly affected by turbulent flows entering the well or by the turbulent suction of the pumps. Bubbler type level monitoring systems shall include dual air compressors. Provision shall be made to automatically alternate the pumps in use. Suction lift stations should be designed to alternate pumps daily instead of each pumping cycle to extend the life of the priming equipment.

#### **42.5 Valves**

##### **42.51 Suction Line**

Suitable shutoff valves shall be placed on the suction line of dry pit pumps.

##### **42.52 Discharge Line**

Suitable shutoff and check valves shall be placed on the discharge line of each pump (except on screw pumps). The check valve shall be located between the shutoff valve and the pump. Check valves shall be suitable for the material being handled and shall be placed on the horizontal portion of discharge piping except for ball checks, which may be placed in the vertical run. Valves shall be capable of withstanding normal pressure and water hammer.

All shutoff and check valves shall be operable from the floor level and accessible for maintenance. Outside levers are recommended on swing check valves.

#### **42.6 Wet Wells**

##### **42.61 Divided Wells**

Where continuity of pumping station operation is critical, consideration should be given to dividing the wet well into two sections, properly interconnected, to facilitate repairs and cleaning.

##### **42.62 Size**

The design fill time and minimum pump cycle time shall be considered in sizing the wet well. The effective volume of the wet well shall be based on design average flow and a filling time not to exceed 30 minutes unless the facility is designed to provide flow equalization. The pump manufacturer's duty cycle recommendations shall be utilized in selecting the minimum cycle time. When the anticipated initial flow tributary to the pumping station is less than the design average flow, provisions should be made so that the fill time indicated is not exceeded for initial flows. When the wet well is designed for flow equalization as part of a treatment plant, provisions should be made to prevent septicity.

##### **42.63 Floor Slope**

The wet well floor shall have a minimum slope of 1 to 1 to the hopper bottom.

The horizontal area of the hopper bottom shall be no greater than necessary for proper installation and function of the inlet.

#### **42.64 Air Displacement**

Covered wet wells shall have provisions for air displacement to the atmosphere, such as an inverted "j" tube or other means.

### **42.7 Safety Ventilation**

#### **42.71 General**

Adequate ventilation shall be provided for all pump stations. Where the dry well is below the ground surface, mechanical ventilation is required. If screens or mechanical equipment requiring maintenance or inspection are located in the wet well, permanently installed ventilation is required. There shall be no interconnection between the wet well and dry well ventilation systems.

#### **42.72 Air Inlets and Outlets**

In dry wells over 15 feet (4.6 m) deep, multiple inlets and outlets are desirable. Dampers should not be used on exhaust or fresh air ducts. Fine screens or other obstructions in air ducts should be avoided to prevent clogging.

#### **42.73 Electrical Controls**

Switches for operation of ventilation equipment should be marked and located conveniently. All intermittently operated ventilation equipment shall be interconnected with the respective pit lighting system. Consideration should be given also to automatic controls where intermittent operation is used. The manual lighting/ventilation switch shall override the automatic controls. For a two speed ventilation system with automatic switch over where gas detection equipment is installed, consideration should be given to increasing the ventilation rate automatically in response to the detection of hazardous concentrations of gases or vapors.

#### **42.74 Fans, Heating, and Dehumidification**

The fan wheel shall be fabricated from non-sparking material. Automatic heating and dehumidification equipment shall be provided in all dry wells. The electrical equipment and components shall meet the requirements in Paragraph 42.35.

#### **42.75 Wet Wells**

Wet well ventilation may be either continuous or intermittent. Ventilation, if continuous, shall provide at least 12 complete air changes per hour; if intermittent, at least 30 complete air changes per hour. Air shall be forced into the wet well by mechanical means rather than solely exhausted from the wet well. The air change requirements shall be based on 100 percent fresh air. Portable ventilation equipment shall be provided for use at submersible pump stations and wet wells with no permanently installed ventilation equipment.

#### **42.76 Dry Wells**

Dry well ventilation may be either continuous or intermittent. Ventilation, if continuous, shall provide at least 6 complete air changes per hour; if intermittent, at least 30 complete air changes per hour. A system of two speed ventilation with

an initial ventilation rate of 30 changes per hour for 10 minutes and automatic switch over to 6 changes per hour may be used to conserve heat. The air change requirements shall be based on 100 percent fresh air.

#### **42.8 Flow Measurement**

Suitable devices for measuring wastewater flow shall be provided at all pumping stations. Indicating, totalizing, and recording flow measurement shall be provided at pumping stations with a 1200 gpm (75 L/s) or greater design peak flow. Elapsed time meters used in conjunction with annual pumping rate tests may be acceptable for pump stations with a design peak hourly flow up to 1200 gpm (75 L/s) provided sufficient metering is configured to measure the duration of individual and simultaneous pump operation.

#### **42.9 Water Supply**

There shall be no physical connection between any potable water supply and a wastewater pumping station which under any conditions might cause contamination of the potable water supply. If a potable water supply is brought to the station, it shall comply with conditions stipulated under Paragraph 56.23.

### **43 SUCTION-LIFT PUMP STATIONS**

Suction-lift pumps shall meet the applicable requirements of Section 42.

#### **43.1 Pump Priming and Lift Requirements**

Suction-lift pumps shall be of the self-priming or vacuum-priming type. Suction-lift pump stations using dynamic suction lifts exceeding the limits outlined in the following sections may be approved upon submission of factory certification of pump performance and detailed calculations indicating satisfactory performance under the proposed operating conditions. Such detailed calculations must include static suction-lift as measured from "lead pump off" elevation to center line of pump suction, friction, and other hydraulic losses of the suction piping, vapor pressure of the liquid, altitude correction, required net positive suction head, and a safety factor of at least 6 feet (1.8 m).

##### **43.11 Self-Priming Pumps**

Self-priming pumps shall be capable of rapid priming and repriming at the "lead pump on" elevation. Such self-priming and repriming shall be accomplished automatically under design operating conditions. Suction piping should not exceed the size of the pump suction and shall not exceed 25 feet (7.6 m) in total length. Priming lift at the "lead pump on" elevation shall include a safety factor of at least 4 feet (1.2 m) from the maximum allowable priming lift for the specific equipment at design operating conditions. The combined total of dynamic suction-lift at the "pump off" elevation and required net positive suction head at design operating conditions shall not exceed 22 feet (6.7 m).

##### **43.12 Vacuum-Priming Pumps**

Vacuum-priming pump stations shall be equipped with dual vacuum pumps capable of automatically and completely removing air from the suction-lift pump. The vacuum pumps shall be adequately protected from damage due to wastewater. The combined total of dynamic suction-lift at the "pump off" elevation and required net positive suction head at design operating conditions shall not exceed 22 feet (6.7 m).

### **43.2 Equipment, Wet Well Access, and Valving Location**

The pump equipment compartment shall be above grade or offset and shall be effectively isolated from the wet well to prevent a hazardous and corrosive sewer atmosphere from entering the equipment compartment. Wet well access shall not be through the equipment compartment and shall be at least 24 inches (610 mm) in diameter. Gasketed replacement plates shall be provided to cover the opening to the wet well for pump units removed for servicing. Valving shall not be located in the wet well.

## **44 SUBMERSIBLE PUMP STATIONS - SPECIAL CONSIDERATIONS**

Submersible pump stations shall meet the applicable requirements under Section 42, except as modified in this Section.

### **44.1 Construction**

Submersible pumps and motors shall be designed specifically for raw wastewater use, including totally submerged operation during a portion of each pumping cycle and shall meet the requirements of the National Electrical Code for such units. An effective method to detect shaft seal failure or potential seal failure shall be provided.

### **44.2 Pump Removal**

Submersible pumps shall be readily removable and replaceable without personnel entering or dewatering the wet well, or disconnecting any piping in the wet well.

### **44.3 Electrical Equipment**

#### **44.31 Power Supply and Control Circuitry**

Electrical supply, control, and alarm circuits shall be designed to provide strain relief and to allow disconnection from outside the wet well. Terminals and connectors shall be protected from corrosion by location outside the wet well or through use of watertight seals.

#### **44.32 Controls**

The motor control center shall be located outside the wet well, be readily accessible, and be protected by a conduit seal or other appropriate measures meeting the requirements of the National Electrical Code, to prevent the atmosphere of the wet well from gaining access to the control center. The seal shall be so located that the motor may be removed and electrically disconnected without disturbing the seal. When such equipment is exposed to weather, it shall meet the requirements of weatherproof equipment NEMA 3R or 4.

#### **44.33 Power Cord**

Pump motor power cords shall be designed for flexibility and serviceability under conditions of extra hard usage and shall meet the requirements of the National Electrical Code standards for flexible cords in wastewater pump stations. Ground fault interruption protection shall be used to de-energize the circuit in the event of any failure in the electrical integrity of the cable. Power cord terminal fittings shall be corrosion-resistant and constructed in a manner to prevent the entry of moisture into the cable, shall be provided with strain relief appurtenances, and shall be designed to facilitate field connecting.

#### **44.4 Valves**

Valves required under Paragraph 42.5 shall be located in a separate valve chamber. Provisions shall be made to remove or drain accumulated water from the valve chamber. The valve chamber may be dewatered to the wet well through a drain line with a gas and water tight valve. Check valves that are integral to the pump need not be located in a separate valve chamber provided that the valve can be removed from the wet well in accordance with Paragraph 44.2. Access shall be provided in accordance with Paragraph 42.231.

### **45 SCREW PUMP STATIONS - SPECIAL CONSIDERATIONS**

Screw pumps shall meet the applicable requirements of Section 42.

#### **45.1 Covers**

Covers or other means of excluding direct sunlight shall be provided as necessary to eliminate adverse effects from temperature changes.

#### **45.2 Pump Wells**

A positive means of isolating individual screw pump wells shall be provided.

#### **45.3 Bearings**

Submerged bearings shall be lubricated by an automated system without pump well dewatering.

### **46 ALARM SYSTEMS**

Alarm systems with a backup power source shall be provided for pumping stations. The alarm shall be activated in cases of power failure, dry well sump and wet well high water levels, pump failure, unauthorized entry, or any other cause of pump station malfunction. Pumping station alarms including identification of the alarm condition shall be transmitted to a municipal facility that is staffed 24 hours a day. If such a facility is not available and a 24-hour holding capacity is not provided, the alarm shall be transmitted to municipal offices during normal working hours and to the home of the responsible person(s) in charge of the lift station during off-duty hours. Audio-visual alarm systems may be acceptable in some cases in lieu of a transmitting system depending upon location, station holding capacity and inspection frequency.

### **47 EMERGENCY OPERATION**

#### **47.1 Objective**

The objective of emergency operation is to prevent the discharge of raw or partially treated wastewater to any waters and to protect public health by preventing back-up of wastewater and subsequent discharge to basements, streets, and other public and private property.

#### **47.2 Emergency Pumping Capability**

Emergency pumping capability is required unless on-system overflow prevention is provided by adequate storage capacity. Emergency pumping capability shall be accomplished by connection of the station to at least two independent utility substations, or by provision of portable or in-place internal combustion engine equipment which will

generate electrical or mechanical energy, or by the provision of portable pumping equipment. Such emergency standby systems shall have sufficient capacity to start up and maintain the total rated running capacity of the station. Regardless of the type of emergency standby system provided, a portable pump connection to the force main with rapid connection capabilities and appropriate valving shall be provided outside the dry well and wet well.

### **47.3 Emergency High Level Overflows**

For use during possible periods of extensive power outages, mandatory power reductions, or uncontrollable emergency conditions, consideration should be given to providing a controlled, high-level wet well overflow to supplement alarm systems and emergency power generation in order to prevent backup of wastewater into basements, or other discharges which may cause severe adverse impacts on public interests, including public health and property damage. Where a high level overflow is utilized, consideration shall also be given to the installation of storage/detention tanks, or basins, which shall be made to drain to the station wet well. Where such overflows affect public water supplies or other critical water uses, the regulatory agency shall be contacted for the necessary treatment or storage requirements.

### **47.4 Equipment Requirements**

#### **47.41 General**

The following general requirements shall apply to all internal combustion engines used to drive auxiliary pumps, service pumps through special drives, or electrical generating equipment:

##### **47.411 Engine Protection**

The engine must be protected from operating conditions that would result in damage to equipment. Unless continuous manual supervision is planned, protective equipment shall be capable of shutting down the engine and activating an alarm on site and as provided in Section 46. Protective equipment shall monitor for conditions of low oil pressure and overheating, except that oil pressure monitoring will not be required for engines with splash lubrication.

##### **47.412 Size**

The engine shall have adequate rated power to start and continuously operate under all connected loads.

##### **47.413 Fuel Type**

Reliability and ease of starting, especially during cold weather conditions, should be considered in the selection of the type of fuel.

##### **47.414 Underground Fuel Storage**

Underground fuel storage and piping facilities shall be constructed in accordance with applicable state, provincial, and federal regulations.

##### **47.415 Engine Ventilation**

The engine shall be located above grade with adequate ventilation of

fuel vapors and exhaust gases.

#### **47.416 Routine Start-up**

All emergency equipment shall be provided with instructions indicating the need for regular starting and running of such units at full loads.

#### **47.417 Protection of Equipment**

Emergency equipment shall be protected from damage at the restoration of regular electrical power.

### **47.42 Engine-Driven Pumping Equipment**

Where permanently-installed or portable engine-driven pumps are used, the following requirements in addition to general requirements shall apply:

#### **47.421 Pumping Capacity**

Engine-driven pumps shall meet the design pumping requirements unless storage capacity is available for flows in excess of pump capacity. Pumps shall be designed for anticipated operating conditions, including suction lift if applicable.

#### **47.422 Operation**

The engine and pump shall be equipped to provide automatic start-up and operation of pumping equipment unless manual start-up and operation is justified. Provisions shall also be made for manual start-up. Where manual start-up and operation is justified, storage capacity and alarm system must meet the requirements of Paragraph 47.423.

#### **47.423 Portable Pumping Equipment**

Where part or all of the engine-driven pumping equipment is portable, sufficient storage capacity with alarm system shall be provided to allow time for detection of pump station failure and transportation and hookup of the portable equipment.

### **47.43 Engine-Driven Generating Equipment**

Where permanently-installed or portable engine-driven generating equipment is used, the following requirements shall apply in addition to general requirements of Paragraph 47.41:

#### **47.431 Generating Capacity**

- a. Generating unit size shall be adequate to provide power for pump motor starting current and for lighting, ventilation, and other auxiliary equipment necessary for safety and proper operation of the lift station.
- b. The operation of only one pump during periods of auxiliary power supply must be justified. Such justification may be made on the basis of the design peak hourly flows relative to single-pump capacity, anticipated length of power outage, and storage capacity.

- c. Special sequencing controls shall be provided to start pump motors unless the generating equipment has capacity to start all pumps simultaneously with auxiliary equipment operating.

#### **47.432 Operation**

Provisions shall be made for automatic and manual start-up and load transfer unless only manual start-up and operation is justified. The generator must be protected from operating conditions that would result in damage to equipment. Provisions should be considered to allow the engine to start and stabilize at operating speed before assuming the load. Where manual start-up and transfer is justified, storage capacity and alarm system must meet the requirements of Paragraph 47.433.

#### **47.433 Portable Generating Equipment**

Where portable generating equipment or manual transfer is provided, sufficient storage capacity with alarm system shall be provided to allow time for detection of pump station failure and transportation and connection of generating equipment. The use of special electrical connections and double throw switches are recommended for connecting portable generating equipment.

#### **47.44 Independent Utility Substations**

Where independent substations are used for emergency power, each separate substation and its associated transmission lines shall be capable of starting and operating the pump station at its rated capacity.

### **48 INSTRUCTIONS AND EQUIPMENT**

Wastewater pumping stations and portable equipment shall be supplied with a complete set of operational instructions, including emergency procedures, maintenance schedules, tools and such spare parts as may be necessary.

### **49 FORCE MAINS**

#### **49.1 Velocity and Diameter**

At design pumping rates, a cleansing velocity of at least 2 feet per second (0.6 m/s) should be maintained. The minimum force main diameter for raw wastewater shall not be less than 4 inches (100 mm).

#### **49.2 Air and Vacuum Relief Valve**

An air relief valve shall be placed at high points in the force main to prevent air locking. Vacuum relief valves may be necessary to relieve negative pressures on force mains. The force main configuration and head conditions should be evaluated as to the need for and placement of vacuum relief valves.

#### **49.3 Termination**

The force main shall enter the receiving manhole with a smooth flow transition to the gravity sewer system at a point not more than 1 foot (0.3 m) above the flow line. Corrosion protection for the receiving manhole shall be provided in accordance with

Paragraph 34.8.

#### **49.4 Pipe and Design Pressure**

Pipe and joints shall be equal to water main strength materials suitable for design conditions. The force main, reaction blocking, and station piping shall be designed to withstand water hammer pressures and associated cyclic reversal of stresses that are expected with the cycling of wastewater lift stations. The use of surge valves, surge tanks or other suitable means to protect the force main against severe pressure changes shall be evaluated.

#### **49.5 Special Construction**

Force main construction near streams or water works structures and at water main crossings shall meet applicable provisions of Sections 36, 37, and 38. There shall be at least a 10 foot (3 m) horizontal separation between water mains and sewer force mains.

#### **49.6 Design Friction Losses**

##### **49.61 Friction Coefficient**

Friction losses through force mains shall be based on the Hazen and Williams formula or other acceptable methods. When the Hazen and Williams formula is used, the value for "C" shall be 100 for unlined iron or steel pipe for design. For other smooth pipe materials such as PVC, polyethylene, lined ductile iron, etc., a higher "C" value not to exceed 120 may be allowed for design.

##### **49.62 Maximum Power Requirements**

When initially installed, force mains will have a significantly higher "C" factor. The effect of the higher "C" factor should be considered in calculating maximum power requirements and duty cycle time to prevent damage to the motor. The effects of higher discharge rates on selected pumps and downstream facilities should also be considered.

#### **49.7 Identification**

Where force mains are constructed of material which might cause the force main to be confused with potable water mains, the force main shall be appropriately identified.

#### **49.8 Leakage Testing**

Leakage tests shall be specified including testing methods and leakage limits.

#### **49.9 Maintenance Considerations**

Isolation valves should be considered where force mains connect into a common force main. Cleanouts at low points and chambers for pig launching and catching should be considered for any force main to facilitate maintenance.

#### **49.10 Cover**

Force mains shall be covered with sufficient earth or other insulation to prevent freezing.

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## **CHAPTER 50 WASTEWATER TREATMENT FACILITIES**

### **51. PLANT LOCATION**

#### **51.1 General**

Items to be considered when selecting a plant site are listed in Chapter 10.

#### **51.2 Flood Protection**

The treatment plant structures, electrical, and mechanical equipment shall be protected from physical damage by the one hundred (100) year flood. Treatment plants should remain fully operational and accessible during the twenty-five (25) year flood. This requirement applies to new construction and to existing facilities undergoing major modification. Flood plain regulations of state, province, and federal agencies shall be considered.

### **52. QUALITY OF EFFLUENT**

The required degree of wastewater treatment shall be based on the effluent requirements and water quality standards established by the responsible province, state agency and/or appropriate federal regulations including discharge permit requirements.

### **53. DESIGN**

#### **53.1 Type of Treatment**

Items to be considered in selection of the appropriate type of treatment are presented in Chapter 10.

The plant design shall provide the necessary flexibility to perform satisfactorily within the expected range of waste characteristics and volumes.

#### **53.2 Required Engineering Data for New Process and Application Evaluation**

The policy of the reviewing authority is to encourage rather than obstruct the development of any methods or equipment for treatment of wastewater. The lack of inclusion in these standards of some types of wastewater treatment processes or equipment should not be construed as precluding their use. The reviewing authority may approve other types of wastewater treatment processes and equipment under the condition that the operational reliability and effectiveness of the process or device shall have been demonstrated with a suitably-sized prototype unit operating at its design load conditions, to the extent required.

To determine that such new processes and equipment or applications have a reasonable and substantial chance of success, the reviewing authority may require the following:

- a. Monitoring observations, including test results and engineering evaluations, demonstrating the efficiency of such processes.
- b. Detailed description of the test methods.
- c. Testing, including appropriately-composited samples, under various ranges of strength and flow rates (including diurnal variations) and waste temperatures over a sufficient length of time to demonstrate performance under climatic and other

conditions which may be encountered in the area of the proposed installations.

d. Other appropriate information.

The reviewing authority may require that appropriate testing be conducted and evaluations be made under the supervision of a competent process engineer other than those employed by the manufacturer or developer.

### **53.3 Design Period**

The design period shall be clearly identified in the engineering report or facilities plan as required in Chapter 10.

### **53.4 Design Loads**

#### **53.41 Hydraulic Design**

##### **53.411 Critical Flow Conditions**

Flow conditions critical to the design of the treatment plant are described in Chapter 10.

Initial low flow conditions must be evaluated in the design to minimize operational problems with freezing, septicity, flow measurements and solids dropout. The design peak hourly flows must be considered in evaluating unit processes, pumping, piping, etc.

##### **53.412 Treatment Plant Design Capacity**

The treatment plant design capacity shall be as described in Chapter 10. The plant design flow selected shall meet the appropriate effluent and water quality standards that are set forth in the discharge permit. The design of treatment units that are not subject to peak hourly flow requirements shall be based on the design average flow. For plants subject to high wet weather flows or overflow detention pumpback flows, the design maximum day flows that the plant is to treat on a sustained basis should be specified.

##### **53.413 Flow Equalization**

Facilities for the equalization of flows and organic shock load shall be considered at all plants which are critically affected by surge loadings. The sizing of the flow equalization facilities should be based on data obtained herein and from Chapter 10.

#### **53.42 Organic Design**

Organic loadings for wastewater treatment plant design shall be based on the information given in Chapter 10. The effects of septage flow which may be accepted at the plant shall be given consideration and appropriate facilities shall be included in the design. Refer to the Appendix.

#### **53.43 Shock Effects**

The shock effects of high concentrations and diurnal peaks for short periods of time on the treatment process, particularly for small treatment plants, shall be

considered.

### **53.5 Conduits**

All piping and channels shall be designed to carry the maximum expected flows. The incoming sewer should be designed for unrestricted flow. Bottom corners of the channels must be filleted. Conduits shall be designed to avoid creation of pockets and corners where solids can accumulate.

Suitable gates or valves should be placed in channels to seal off unused sections which might accumulate solids. The use of shear gates, stop plates or stop planks is permitted where they can be used in place of gate valves or sluice gates. Non-corrodible materials shall be used for these control gates.

### **53.6 Arrangement of Units**

Component parts of the plant should be arranged for greatest operating and maintenance convenience, flexibility, economy, continuity of maximum effluent quality, and ease of installation of future units.

### **53.7 Flow Division Control**

Flow division control facilities shall be provided as necessary to ensure organic and hydraulic loading control to plant process units and shall be designed for easy operator access, change, observation, and maintenance. The use of upflow division boxes equipped with adjustable sharp-crested weirs or similar devices is recommended. The use of valves for flow splitting is not acceptable. Appropriate flow measurement facilities shall be incorporated in the flow division control design.

## **54. PLANT DETAILS**

### **54.1 Installation of Mechanical Equipment**

The specifications should be so written that the installation and initial operation of major items of mechanical equipment will be inspected and approved by a representative of the manufacturer.

### **54.2 Unit Bypasses**

#### **54.21 Removal from Service**

Properly located and arranged bypass structures and piping shall be provided so that each unit of the plant can be removed from service independently. The bypass design shall facilitate plant operation during unit maintenance and emergency repair so as to minimize deterioration of effluent quality and ensure rapid process recovery upon return to normal operational mode.

Bypassing may be accomplished through the use of duplicate or multiple treatment units in any stage if the design peak instantaneous flow can be handled hydraulically with the largest unit out of service.

The actuation of all bypasses shall require manual action by operating personnel. All power-actuated bypasses shall be designed to permit manual operation in the event of power failure and shall be designed so that the valve will fail as is, upon failure of the power operator.

A fixed high water level bypass overflow should be provided in addition to a manually or power actuated bypass.

#### **54.22 Unit Bypass During Construction**

Unit bypassing during construction shall be in accordance with the requirements in Paragraphs 11.28(i), 20.15 and Section 21.

#### **54.3 Unit Dewatering, Flotation Protection, and Plugging**

Means such as drains or sumps shall be provided to completely dewater each unit to an appropriate point in the process. Due consideration shall be given to the possible need for hydrostatic pressure relief devices to prevent flotation of structures. Pipes subject to plugging shall be provided with means for mechanical cleaning or flushing.

#### **54.4 Construction Materials**

Materials shall be selected that are appropriate under conditions of exposure to hydrogen sulfide and other corrosive gases, greases, oils, and other constituents frequently present in wastewater. This is particularly important in the selection of metals and paints. Contact between dissimilar materials should be avoided or other provisions made to minimize galvanic action.

#### **54.5 Painting**

The use of paints containing lead or mercury should be avoided. In order to facilitate identification of piping, particularly in the large plants, it is suggested that the different lines be color-coded. The following color scheme is recommended for purposes of standardization.

- Raw sludge line - brown with black bands
- Sludge recirculation suction line - brown with yellow bands
- Sludge draw off line - brown with orange bands
- Sludge recirculation discharge line - brown
- Sludge gas line - orange (or red)
- Natural gas line - orange (or red) with black bands
- Nonpotable water line - blue with black bands
- Potable water line - blue
- Chlorine line - yellow
- Sulfur Dioxide - yellow with red bands
- Sewage (wastewater) line - gray
- Compressed air line - green
- Water lines for heating digesters or buildings - blue with a 6-inch (150 mm) red band spaced 30 inches (760 mm) apart
- Fuel oil/diesel - red
- Plumbing drains and vents - black
- Polymer - purple

The contents and direction of flow shall be stenciled on the piping in a contrasting color.

#### **54.6 Operating Equipment**

A complete outfit of tools, accessories, and spare parts necessary for the plant operator's use shall be provided.

Readily accessible storage space and workbench facilities shall be provided, and

consideration shall be given to provision of a garage for large equipment storage, maintenance, and repair.

#### **54.7 Erosion Control During Construction**

Effective site erosion control shall be provided during construction.

#### **54.8 Grading and Landscaping**

Upon completion of the plant, the ground shall be graded and sodded or seeded. All-weather walkways should be provided for access to all units. Where possible, steep slopes should be avoided to prevent erosion. Surface water shall not be permitted to drain into any unit. Particular care shall be taken to protect trickling filter beds, sludge beds, and intermittent sand filters from stormwater runoff. Provision should be made for landscaping, particularly when a plant must be located near residential areas.

### **55. PLANT OUTFALLS**

#### **55.1 Discharge Impact Control**

The outfall sewer shall be designed to discharge to the receiving stream in a manner acceptable to the reviewing authority. Consideration should be given in each case to the following:

- a. Preference for free fall or submerged discharge at the site selected;
- b. Utilization of cascade aeration of effluent discharge to increase dissolved oxygen; and
- c. Limited or complete across-stream dispersion as needed to protect aquatic life movement and growth in the immediate reaches of the receiving stream.

#### **55.2 Protection and Maintenance**

The outfall sewer shall be so constructed and protected against the effects of floodwater, tide, ice, or other hazards as to reasonably ensure its structural stability and freedom from stoppage. A manhole should be provided at the shore end of all gravity sewers extended into the receiving waters. Hazards to navigation shall be considered in designing outfall sewers.

#### **55.3 Sampling Provisions**

All outfalls shall be designed so that a sample of the effluent can be obtained at a point after the final treatment process and before discharge to or mixing with the receiving waters.

### **56. ESSENTIAL FACILITIES**

#### **56.1 Emergency Power Facilities**

##### **56.11 General**

All plants shall be provided with an alternate source of electric power or pumping capability to allow continuity of operation during power failures, except as noted below. Refer to Paragraph 46.4 for design details. Methods of providing alternate sources include:

- a. The connection of at least two independent power sources such as substations. A power line from each substation is recommended, and will be required unless documentation is received and approved by the reviewing authority verifying that a duplicate line is not necessary;
- b. Portable or in-place internal combustion engine equipment which will generate electrical or mechanical energy; and
- c. Portable pumping equipment when only emergency pumping is required.

#### **56.12 Power for Aeration**

Standby generating capacity normally is not required for aeration equipment used in the activated sludge process. In cases where a history of long-term (4 hours or more) power outages have occurred, auxiliary power for minimum aeration of the activated sludge will be required. Full power generating capacity may be required by the reviewing authority for waste discharges to certain critical stream segments such as upstream of bathing beaches, public water supply intake or other similar situations.

#### **56.13 Power for Disinfection**

Continuous disinfection, where required, shall be provided during all power outages. Continuous dechlorination is required for those systems that dechlorinate.

### **56.2 Water Supply**

#### **56.21 General**

An adequate supply of potable water under pressure should be provided for use in the laboratory and for general cleanliness around the plant. No piping or other connections shall exist in any part of the treatment plant which, under any conditions, might cause the contamination of a potable water supply. The chemical quality should be checked for suitability for its intended uses such as in heat exchangers, chlorinators, etc.

#### **56.22 Direct Connections**

Potable water from a municipal or separate supply may be used directly at points above grade for the following hot and cold supplies:

- a. Lavatory;
- b. Water closet;
- c. Laboratory sink (with vacuum breaker);
- d. Shower;
- e. Drinking fountain;
- f. Eye wash fountain; and
- g. Safety shower.

Hot water for any of the above units shall not be taken directly from a boiler used for supplying hot water to a sludge heat exchanger or digester heating unit.

#### **56.23 Indirect Connections**

Where a potable water supply is to be used for any purpose in a plant other than those listed in Paragraph 56.22, a break tank, pressure pump, and pressure tank shall be provided. Water shall be discharged to the tank through an air gap at least 6 inches (150 mm) above the maximum flood line or the spill line of the tank, whichever is higher.

A sign shall be permanently posted at every hose bib, faucet, hydrant, or sill cock located on the water system beyond the break tank to indicate that the water is not safe for drinking.

#### **56.24 Separate Potable Water Supply**

Where it is not possible to provide potable water from a public water supply, a separate well may be provided. Location and construction of the well should comply with requirements of the governing state or province and local regulations. Requirements governing the use of the potable water supply are those contained in Paragraphs 56.22 and 56.23.

#### **56.25 Separate Non-Potable Water Supply**

Where a separate non-potable water supply is to be provided, a break tank will not be necessary, but all system outlets shall be posted with a permanent sign indicating the water is not safe for drinking.

### **56.3 Sanitary Facilities**

Toilet, shower, lavatory, and locker facilities should be provided in sufficient numbers and at convenient locations to serve the expected plant personnel.

### **56.4 Floor Slope**

Floor surfaces shall be sloped adequately to a point of drainage.

### **56.5 Stairways**

Stairways shall be installed in lieu of ladders for access to units requiring routine inspection and maintenance, such as digesters, trickling filters, aeration tanks, clarifiers, tertiary filters, etc. Spiral or winding stairs are permitted only for secondary access where dual means of egress are provided.

Stairways shall have slopes between 30 and 40 degrees from the horizontal to facilitate carrying samples, tools, etc. Each tread and riser shall be of uniform dimension in each flight. Minimum tread run shall not be less than 9 inches (230 mm). The sum of the tread run and riser shall not be less than 17 inches (430 mm) nor more than 18 inches (460 mm). A flight of stairs shall consist of not more than a 12-foot (3.7 m) continuous rise without a platform.

### **56.6 Flow Measurement**

#### **56.61 Location**

Flow measurement facilities shall be provided to measure the following flows:

- a. Plant influent or effluent flow;
- b. Plant influent flow: If influent flow is significantly different from

effluent flow, both shall be measured. This would apply for installations such as lagoons, sequencing batch reactors, and plants with excess flow storage or flow equalization;

- c. Excess flow treatment facility discharges;
- d. Other flows required to be monitored under the provisions of the discharge permit; and
- e. Other flows such as return activated sludge, waste activated sludge, recirculation, and recycle required for plant operational control.

### **56.62 Facilities**

Indicating, totalizing, and recording flow measurement devices shall be provided for all mechanical plants. Flow measurement facilities for lagoon systems shall not be less than elapsed time meters used in conjunction with pumping rate tests or shall be calibrated weirs. All flow measurement equipment must be sized to function effectively over the full range of flows expected and shall be protected against freezing.

### **56.63 Hydraulic Conditions**

Flow measurement equipment including approach and discharge conduit configuration and critical control elevations shall be designed to ensure that the required hydraulic conditions necessary for accurate measurement are provided. Conditions that must be avoided include turbulence, eddy currents, air entrainment, etc., that upset the normal hydraulic conditions that are necessary for accurate flow measurement.

### **56.7 Sampling Equipment**

Effluent composite sampling equipment shall be provided at all mechanical plants with a design average flow of 0.1 mgd (380 m<sup>3</sup>/d) or greater and at other facilities where necessary to meet discharge permit monitoring requirements. Composite sampling equipment shall also be provided as needed for influent sampling and for monitoring plant operations. The influent sampling point should be located prior to any process return flows.

## **57. SAFETY**

### **57.1 General**

Adequate provision shall be made to effectively protect plant personnel and visitors from hazards. The following shall be provided to fulfill the particular needs of each plant:

- a. Enclosure of the plant site with a fence and signs designed to discourage the entrance of unauthorized persons and animals;
- b. Hand rails and guards around tanks, trenches, pits, stairwells, and other hazardous structures with the tops of walls less than 42 inches (1070 mm) above the surrounding ground level;
- c. Gratings over appropriate areas of treatment units where access for maintenance is required;
- d. First aid equipment;

- e. "No Smoking" signs in hazardous areas;
- f. Protective clothing and equipment, such as self-contained breathing apparatus, gas detection equipment, goggles, gloves, hard hats, safety harnesses, etc.;
- g. Portable blower and sufficient hose;
- h. Portable lighting equipment complying with the National Electrical Code requirements;
- i. Gas detectors listed and labeled for use in Class I, Division 1, Group D locations;
- j. Appropriately-placed warning signs for slippery areas, non-potable water fixtures, low head clearance areas, open service manholes, hazardous chemical storage areas, flammable fuel storage areas, etc.;
- k. Adequate ventilation in pump station areas in accordance with Paragraph 42.7;
- l. Provisions for local lockout on stop motor controls;
- m. Provisions for confined space entry and laboratory safety in accordance with OSHA and regulatory agency requirements; and
- n. Adequate vector control.

## **57.2 Hazardous Chemical Handling**

### **57.21 Containment Materials**

The materials utilized for storage, piping, valves, pumping, metering, splash guards, etc., shall be specially selected considering the physical and chemical characteristics of each hazardous or corrosive chemical.

### **57.22 Secondary Containment**

Chemical storage areas shall be enclosed in dikes or curbs which will contain the stored volume until it can be safely transferred to alternate storage or released to the wastewater at controlled rates which will not damage facilities, inhibit the treatment processes, or contribute to stream pollution. Liquid polymer should be similarly contained to reduce areas with slippery floors, especially to protect travelways. Non-slip floor surfaces are desirable in polymer-handling areas.

### **57.23 Liquefied Gas Chemicals**

Properly designed isolated areas shall be provided for storage and handling of chlorine and sulfur dioxide and other hazardous gases. Gas detection kits, alarms, controls, safety devices, and emergency repair kits shall also be provided.

### **57.24 Splash Guards**

All pumps or feeders for hazardous or corrosive chemicals shall have guards which will effectively prevent spray of chemicals into space occupied by personnel. The splash guards are in addition to guards to prevent injury from moving or rotating machinery parts.

**57.25 Piping, Labeling, Coupling Guards, Location**

All piping containing or transporting corrosive or hazardous chemicals shall be identified with labels every 10 feet (3 m) and with at least two labels in each room, closet, or pipe chase. Color-coding may also be used, but is not an adequate substitute for labeling.

All connections (flanged or other type), except those adjacent to storage or feeder areas, shall have guards which will direct any leakage away from space occupied by personnel. Pipes containing hazardous or corrosive chemicals should not be located above shoulder level except where continuous drip collection trays and coupling guards will eliminate chemical spray or dripping onto personnel.

**57.26 Protective Clothing and Equipment**

The following items of protective clothing or equipment shall be available and utilized for all operations or procedures where their use will minimize injury hazard to personnel:

- a. Self-contained breathing apparatus recommended for protection against chlorine;
- b. Chemical worker's goggles or other suitable goggles (safety glasses are insufficient);
- c. Face masks or shields for use over goggles;
- d. Dust mask to protect the lungs in dry chemical areas;
- e. Rubber gloves;
- f. Rubber aprons with leg straps;
- g. Rubber boots (leather and wool clothing should be avoided near caustics); and
- h. Safety harness and line.

**57.27 Warning System and Signs**

Facilities shall be provided for automatic shutdown of pumps and sounding of alarms when failure occurs in a pressurized chemical discharge line.

Warning signs requiring use of goggles shall be located near chemical stations, pumps, and other points of frequent hazard.

**57.28 Dust Collection**

Dust collection equipment shall be provided to protect personnel from dusts injurious to the lungs or skin and to prevent polymer dust from settling on walkways which become slick when wet.

**57.29 Eyewash Fountains and Safety Showers**

Eyewash fountains and safety showers utilizing potable water shall be provided

on each floor level or work location involving hazardous or corrosive chemical storage, mixing (or slaking), pumping, metering, or transportation unloading. These facilities are to be as close as practical to points of chemical exposure. They are to be fully operable during all weather conditions.

The eyewash fountains shall be supplied with water of moderate temperature 50° to 90°F (10 °C to 32 °C) suitable to provide 15 to 30 minutes of continuous irrigation of the eyes. The emergency showers shall be capable of discharging 30 to 50 gpm (1.9 L/s to 3.2 L/s) of water at moderate temperature and at pressures of 20 to 50 psi (140 kPa to 345 kPa).

### **57.3 Hazardous Chemical Container Identification**

The identification and hazard warning data included on shipping containers, when received, shall appear on all containers (regardless of size or type) used to store, carry, or use a hazardous substance. Wastewater and sludge sample containers should be adequately labeled. Below is a suitable label to identify a wastewater sample as a hazardous substance:

RAW SEWAGE WASTEWATER

Sample point No. \_\_\_\_\_

Contains Harmful Bacteria.

May contain hazardous or toxic material.

Do not drink or swallow.

Avoid contact with openings or breaks in the skin.

## **58. LABORATORY**

### **58.1 General**

All treatment plants shall include a laboratory for making the necessary analytical determinations and operating control tests, except for those plants utilizing only processes not requiring laboratory testing for plant control and where satisfactory off-site laboratory provisions are made to meet the permit monitoring requirements. For plants where a fully equipped laboratory is not required, the requirements for utilities, fume hoods, etc., may be reduced. The laboratory shall have sufficient size, bench space, equipment, and supplies to perform all self-monitoring analytical work required by discharge permits, and to perform the process control tests necessary for good management of each treatment process included in the design.

The facilities and supplies necessary to perform analytical work to support industrial waste control programs will normally be included in the same laboratory. The laboratory arrangement should be sufficiently flexible to allow future expansion should more analytical work be needed. Laboratory instrumentation and size should reflect treatment plant size, staffing requirements, process complexity, and applicable certification requirements. Experience and training of plant operators should also be assessed in determining treatment plant laboratory needs.

Treatment plant laboratory needs may be divided into the following three general categories:

- I. Plants performing only basic operational testing; this typically includes pH, temperature, and dissolved oxygen;
- II. Plants performing more complex operational and permit laboratory tests including biochemical oxygen demand, suspended solids, and fecal coliform analysis, and;
- III. Plants performing more complex operational, permit, industrial pretreatment, and multiple plant laboratory testing.

Expected minimum laboratory needs for these three plant classifications are outlined in this Section. However, in specific cases laboratory needs may have to be modified or increased due to the industrial monitoring needs or special process control requirements.

## **58.2 Category I: Plants performing only basic operational testing.**

### **58.21 Location and Space**

A floor area up to 150 square feet (14 m<sup>2</sup>) should be adequate. It is recommended that this be at the treatment site. Another location in the community utilizing space in an existing structure owned by the involved wastewater authority may be acceptable.

### **58.22 Design and Materials**

The facility shall provide for electricity, water, heat, sufficient storage space, a sink, and a bench top. The lab components need not be of industrial grade materials. Laboratory equipment and glassware shall be of types recommended by Standard Methods for the Examination of Water and Wastewater and the reviewing authority.

## **58.3 Category II: Plants performing more complex operational and permit laboratory tests including biochemical oxygen demand, suspended solids, and fecal coliform analysis.**

### **58.31 Location and Space**

The laboratory size should be based on providing adequate room for the equipment to be used. In general, the laboratories for this category of plant should provide a minimum of approximately 300 square feet (28 m<sup>2</sup>) of floor space. Adequate bench space for each analyst shall be provided. The laboratory should be located at the treatment site on ground level. It shall be isolated from vibrating, noisy, or high-temperature machinery or equipment which might have adverse effects on the performance of laboratory staff or instruments.

### **58.32 Floors**

Floor surfaces should be fire resistant, and highly resistant to acids, alkalies, solvents, and salts.

### **58.33 Cabinets and Bench Tops**

Laboratories in this category usually perform both the NPDES permit testing and operational control monitoring utilizing "acids" and "bases" in small quantities, such that laboratory grade metal cabinets and shelves are not mandatory. The cabinets and shelves selected may be of wood or other durable materials. Bench

tops should be of acid resistant laboratory grade materials for protection of the underlying cabinets. Glass doors on wall-hung cabinets are recommended. One or more cupboard style base cabinets should be provided. Cabinets with drawers should have stops to prevent accidental removal. Cabinets for Category II laboratories are not required to have gas, air, vacuum, and electrical service fixtures. Built-in shelves should be adjustable.

### **58.34 Fume Hoods, Sinks, and Ventilation**

#### **58.341 Fume Hoods**

Fume hoods shall be provided for laboratories in which required analytical work results in the production of noxious fumes. Air intake should be balanced against all exhaust ventilation to maintain an overall positive pressure relative to atmospheric in the laboratory.

#### **58.342 Sinks**

A laboratory grade sink and drain trap shall be provided.

#### **58.343 Ventilation**

Laboratories should be air conditioned. In addition, separate exhaust ventilation should be provided.

### **58.35 Balance and Table**

An analytical balance of the automated digital readout, single pan 0.1 milligram sensitivity type shall be provided. A heavy special-design balance table which will minimize vibration of the balance is recommended. It shall be located as far as possible from windows, doors, or other sources of drafts or air movements, so as to minimize undesirable impacts from these sources upon the balance.

### **58.36 Equipment, Supplies, and Reagents**

The laboratory shall be provided with all of the equipment, supplies, and reagents that are needed to carry out all of the facility's analytical testing requirements. If any required analytical testing produces malodorous or noxious fumes, the engineer should verify that the in-house analysis is more cost-effective than use of an independent off-site laboratory. Composite samplers may be required to satisfy permit sampling requirements. Discharge permit, process control, and industrial waste monitoring requirements should be considered when specifying equipment needs. References such as Standard Methods for the Examination of Water and Wastewater and the U.S.E.P.A. Analytical Procedures Manual should be consulted prior to specifying equipment items.

### **58.37 Utilities**

#### **58.371 Power Supply**

Consideration should be given to providing line voltage regulation for power supplied to laboratories using delicate instruments.

#### **58.372 Laboratory Water**

Reagent water of a purity suitable for analytical requirements shall be

supplied to the laboratory. In general, reagent water prepared using an all glass distillation system is adequate. However, some analyses require deionization of the distilled water. Consideration should be given to softening the feed water to the still.

## **58.38 Safety**

### **58.381 Equipment**

Laboratories shall provide as a minimum the following: first aid equipment; protective clothing including goggles, gloves, lab aprons, etc.; and a fire extinguisher.

### **58.382 Eyewash Fountains and Safety Showers**

Eyewash fountains and safety showers utilizing potable water shall be provided in the laboratory and should be as close as practical and shall be no more than 25 feet (7.6 m) from points of hazardous chemical exposure.

The eyewash fountains shall be supplied with water of moderate temperature 50° to 90°F (10 °C to 32 °C) suitable to provide 15 to 30 minutes of continuous irrigation of the eyes. The emergency showers shall be capable of discharging 30 to 50 gpm (1.9 L/s to 3.2 L/s) of water at a moderate temperature and at pressures of 20 to 50 psi (140 kPa to 345 kPa).

## **58.4 Category III: Plants performing more complex operational, permit, industrial pretreatment and multiple plant laboratory testing.**

### **58.41. Location and Space**

The laboratory should be located at the treatment site on ground level, with environmental control as an important consideration. It shall be isolated from vibrating, noisy, high temperature machinery or equipment which might have adverse effects on the performance of laboratory staff or instruments.

The laboratory facility needs for Category III plants should be described in the engineering report or facilities plan. The laboratory floor space and facility layout should be based on an evaluation of the complexity, volume, and variety of sample analyses expected during the design life of the plant including testing for process control, industrial pretreatment control, user charge monitoring, and discharge permit monitoring requirements.

Consideration shall be given to the necessity to provide separate (and possibly isolated) areas for some special laboratory equipment, glassware, and chemical storage. The analytical and sample storage areas should be isolated from all potential sources of contamination. It is recommended that the organic chemical facilities be isolated from other facilities. Adequate security shall be provided for sample storage areas. Provisions for the proper storage and disposal of chemical wastes shall be provided. At large plants, office and administrative space needs should be considered.

For less complicated laboratory needs bench-top working surface should occupy at least 35 percent of the total laboratory floor space. Additional floor and bench space should be provided to facilitate performance of analysis of industrial

wastes, as required by the discharge permit and the utility's industrial waste pretreatment program. Ceiling height should be adequate to provide for the installation of wall mounted water stills, deionizers, distillation racks, hoods, and other equipment with extended height requirements.

## **58.42 Floors and Doors**

### **58.421 Floors**

Floor surfaces should be fire resistant, and highly resistant to acids, alkalies, solvents, and salts.

### **58.422 Doors**

Two exit doors should be located to permit a straight egress from the laboratory, preferably at least one to outside the building. Panic hardware should be used. They should have large glass windows for easy visibility of approaching or departing personnel. Automatic door closers should be installed; swinging doors should not be used.

Flush hardware should be provided on doors if cart traffic is anticipated. Kick plates are also recommended.

## **58.43 Cabinets and Bench Tops**

### **58.431 Cabinets**

Wall-hung cabinets are useful for dust-free storage of instruments and glassware. Units with sliding glass doors are recommended. A reasonable proportion of cupboard style base cabinets and drawer units should be provided.

Drawers should slide out so that entire contents are easily visible. They should be provided with rubber bumpers and with stops which prevent accidental removal. Drawers should be supported on ball bearings or nylon rollers which pull easily in adjustable steel channels. All metal drawer fronts should be double-wall construction.

All cabinet shelving should be acid resistant and adjustable. The laboratory furniture shall be supplied with adequate water, gas, air, and vacuum service fixtures; traps, strainers, plugs, and tailpieces, and all electrical service fixtures.

### **58.432 Bench Tops**

Bench tops should be constructed of materials resistant to attacks from normally used laboratory reagents. Generally, bench-top height should be 36 inches (915 mm). However, areas to be used exclusively for sit-down type operations should be 30 inches (760 mm) high and include knee-hole space. One-inch (25 mm) overhangs and drip grooves should be provided to keep liquid spills from running along the face of the cabinet. Tops should be furnished in large sections, 1¼ inches (32 mm) thick. They should be field joined into a continuous surface with acid, alkali, and solvent-resistant cements which are at least as strong as the material of which the top is made.

## **58.44 Hoods**

### **58.441 General**

Fume hoods to promote safety and canopy hoods over heat-releasing equipment shall be provided.

### **58.442 Fume Hoods**

#### **a. Location**

Fume hoods should be located where air disturbance at the face of the hood is minimal. Air disturbance may be created by persons walking past the hood; by heating, ventilating, or air-conditioning systems; by drafts from opening or closing a door; etc.

Safety factors should be considered in locating a hood. If a hood is situated near a doorway, a secondary means of egress must be provided. Bench surfaces should be available next to the hood so that chemicals need not be carried long distances.

#### **b. Design and Materials**

The selection, design, and materials of construction of fume hoods and their appropriate safety alarms must be made by considering the variety of analytical work to be performed. The characteristics of the fumes, chemicals, gases, or vapors that will or may be released by the activities therein should be considered. Special design and construction is necessary if perchloric acid use is anticipated. Consideration should be given to providing more than one fume hood to minimize potential hazardous conditions throughout the laboratory. Air intake should be balanced against all exhaust ventilation to maintain an overall positive pressure relative to atmospheric in the laboratory.

Fume hoods are not appropriate for operation of heat-releasing equipment that does not contribute to hazards, unless they are provided in addition to those needed to perform hazardous tasks.

#### **c. Fixtures**

One sink should be provided inside each fume hood. A cup sink is usually adequate.

All switches, electrical outlets, and utility and baffle adjustment handles should be located outside the hood. Light fixtures should be explosion-proof.

#### **d. Exhaust**

Twenty-four hour continuous exhaust capability should be provided. Exhaust fans should be explosion-proof. Exhaust velocities should be checked when fume hoods are installed.

### **58.443 Canopy Hoods**

Canopy hoods should be installed over the bench-top areas where hot plate, steam bath, or other heating equipment or heat-releasing instruments are used. The canopy should be constructed of heat and corrosion resistant material.

## **58.45 Sinks, Ventilation, and Lighting**

### **58.451 Sinks**

The laboratory should have a minimum of two sinks (not including cup sinks). At least one of them should be a double-well sink with drainboards. Additional sinks should be provided in separate work areas as needed, and identified for the use intended.

Sinks and traps should be made of epoxy resin or plastic materials highly resistant to acids, alkalies, solvents, and salts, and should be abrasion and heat resistant, non-absorbent, and light in weight. Traps should be made of glass, plastic, or lead when appropriate and easily accessible for cleaning. Waste openings should be located toward the back so that a standing overflow will not interfere.

All water fixtures on which hoses may be used should be provided with reduced zone pressure backflow preventers to prevent contamination of water lines.

### **58.452 Ventilation**

Laboratories should be separately air conditioned, with external air supply for one hundred percent make-up volume. In addition, separate exhaust ventilation should be provided. Ventilation outlet locations should be remote from ventilation inlets. Consideration should be given to providing dehumidifiers.

### **58.453 Lighting**

Good lighting, free from shadows, must be provided for reading dials, meniscuses, etc., throughout the laboratory.

## **58.46 Balance and Table**

An analytical balance of the automatic, digital readout, single pan, 0.1 milligram sensitivity type shall be provided. A heavy special-design balance table which will minimize vibration of the balance is needed. It shall be located as far as practical from windows, doors, or other sources of drafts or air movements, so as to minimize undesirable impacts from these sources upon the balance.

## **58.47 Equipment, Supplies, and Reagents**

The laboratory shall be provided with all of the equipment, supplies, and reagents that are needed to carry out all of the facility's analytical testing requirements. Composite samplers may be required to satisfy permit sampling requirements. Discharge permit, process control, and industrial waste monitoring requirements should be considered when specifying equipment needs. References such as Standard Methods for the Examination of Water and Wastewater and the U.S.E.P.A. Analytical Procedures Manual should be consulted prior to specifying

equipment items.

## **58.48 Utilities and Services**

### **58.481 Power Supply**

Consideration should be given to providing line voltage regulation for power supplied to laboratories using delicate instruments.

### **58.482 Laboratory Water**

Reagent water of a purity suitable for analytical requirements shall be supplied to the laboratory. In general, reagent water prepared using an all glass distillation system is adequate. However, some analyses require deionization of the distilled water. Consideration also should be given to softening and/or deionizing the feed water to the still.

### **58.483 Gas and Vacuum**

Natural or LP gas should be supplied to the laboratory. Digester gas should not be used.

An adequately-sized line source of vacuum should be provided with outlets available throughout the laboratory.

## **58.49 Safety**

### **58.491 Equipment**

Laboratories shall provide the following: first aid equipment; protective clothing and equipment such as goggles, safety glasses, full face shields, gloves, etc.; fire extinguishers; chemical spill kits; posting of "No Smoking" signs in hazardous areas; and appropriately placed warning signs for slippery areas, non-potable water fixtures, hazardous chemical storage areas, flammable fuel storage areas, etc.

### **58.492 Eyewash Fountains and Safety Showers**

Eyewash fountains and safety showers utilizing potable water shall be provided in the laboratory. These facilities are to be as close as practical and shall be no more than 25 feet (7.6 m) from points of hazardous chemical exposure.

The eyewash fountains shall be supplied with water of moderate temperature 50° to 90°F (10 °C to 32 ° C), suitable to provide 15 to 30 minutes of continuous irrigation of the eyes. The emergency showers shall be capable of discharging 30 to 50 gpm (1.9 L/s to 3.2 L/s) of water at moderate temperature and at pressures of 20 to 50 psi (140 kPa to 345 kPa).

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## **CHAPTER 60**

### **SCREENING, GRIT REMOVAL, AND FLOW EQUALIZATION**

#### **61. SCREENING DEVICES**

##### **61.1 Coarse Screens**

###### **61.11 Where Required**

Protection for pumps and other equipment shall be provided by trash racks, coarse bar racks, or coarse screens.

###### **61.12 Design and Installation**

###### **61.121 Bar Spacing**

Clear openings between bars should be no less than 1 inch (25 mm) for manually cleaned screens. Clear openings for mechanically cleaned screens may be smaller. Maximum clear openings should be 1¾ inches (45 mm).

###### **61.122 Slope and Velocity**

Manually cleaned screens should be placed on a slope of 30 to 45 degrees from the horizontal.

At design average flow conditions, approach velocities should be no less than 1.25 feet per second (0.4 m/s), to prevent settling; and no greater than 3.0 fps (0.9 m/s) to prevent forcing material through the openings.

###### **61.123 Channels**

Dual channels shall be provided and equipped with the necessary gates to isolate flow from any screening unit. Provisions shall also be made to facilitate dewatering each unit. The channel preceding and following the screen shall be shaped to eliminate stranding and settling of solids.

###### **61.124 Auxiliary Screens**

Where a single mechanically cleaned screen is used, an auxiliary manually cleaned screen shall be provided. Where two or more mechanically cleaned screens are used, the design shall provide for taking any unit out of service without sacrificing the capability to handle the design peak instantaneous flows.

###### **61.125 Invert**

The screen channel invert should be 3 to 6 inches (75 mm to 150 mm) below the invert of the incoming sewer.

###### **61.126 Flow Distribution**

Entrance channels should be designed to provide equal and uniform distribution of flow to the screens.

###### **61.127 Backwater Effect on Flow Metering**

Flow measurement devices should be selected for reliability and accuracy. The effect of changes in backwater elevation, due to intermittent cleaning of screens, should be considered in locations of flow measurement equipment.

#### **61.128 Freeze Protection**

Screening devices and screening storage areas shall be protected from freezing.

#### **61.129 Screenings Removal and Disposal**

A convenient and adequate means for removing screenings shall be provided. Hoisting or lifting equipment may be necessary depending on the depth of pit and amount of screenings or equipment to be lifted.

Facilities must be provided for handling, storage, and disposal of screenings in a manner acceptable to the regulatory agency. Separate grinding of screenings and return to the wastewater flow is unacceptable.

Manually cleaned screening facilities shall include an accessible platform from which the operator may rake screenings easily and safely. Suitable drainage facilities shall be provided for both the platform and the storage area.

### **61.13 Access and Ventilation**

Screens located in pits more than 4 feet (1.2 m) deep shall be provided with stairway access. Access ladders are acceptable for pits less than 4 feet (1.2 m) deep, in lieu of stairways.

Screening devices, installed in a building where other equipment or offices are located, shall be isolated from the rest of the building, be provided with separate outside entrances, and be provided with separate and independent fresh air supply.

Fresh air shall be forced into enclosed screening device areas or into open pits more than 4 feet (1.2 m) deep. Dampers should not be used on exhaust or fresh air ducts and fine screens or other obstructions should be avoided to prevent clogging. Where continuous ventilation is required at least 12 complete air changes per hour shall be provided. Where continuous ventilation would cause excessive heat loss, intermittent ventilation of at least 30 complete air changes per hour shall be provided when personnel enter the area. The air change requirements shall be based on 100 percent fresh air.

Switches for operation of ventilation equipment should be marked and located conveniently. All intermittently operated ventilation equipment shall be interconnected with the respective pit lighting system. The fan wheel shall be fabricated from non-sparking material. Explosion proof gas detectors shall be provided in accordance with Section 57.

### **61.14 Safety and Shields**

#### **61.141 Railings and Gratings**

Manually cleaned screen channels shall be protected by guard railings

and deck gratings, with adequate provisions for removal or opening to facilitate raking.

Mechanically cleaned screen channels shall be protected by guard railings and deck gratings. Consideration should also be given to temporary access arrangements to facilitate maintenance and repair.

#### **61.142 Mechanical Devices**

Mechanical screening equipment shall have adequate removable enclosures to protect personnel against accidental contact with moving parts and to prevent dripping in multi-level installations.

A positive means of locking out each mechanical device and temporary access for use during maintenance shall be provided.

#### **61.143 Drainage**

Floor design and drainage shall be provided to prevent slippery areas.

#### **61.144 Lighting**

Suitable lighting shall be provided in all work and access areas. Refer to Paragraph 61.152.

### **61.15 Electrical Equipment and Control Systems**

#### **61.151 Timing Devices**

All mechanical units which are operated by timing devices shall be provided with auxiliary controls which will set the cleaning mechanism in operation at a preset high water elevation. If the cleaning mechanism fails to lower the high water, a warning should be signaled.

#### **61.152 Electrical Equipment, Fixtures and Controls**

Electrical equipment, fixtures and controls in the screening area where hazardous gases may accumulate shall meet the requirements of the National Electrical Code for Class I, Division 1, Group D locations.

#### **61.153 Manual Override**

Automatic controls shall be supplemented by a manual override.

## **61.2 Fine Screens**

### **61.21 General**

Fine screens as discussed here have openings of approximately 1/16 inch (2 mm). The amount of material removed by fine screens is dependent on the waste stream being treated and screen opening size.

Fine screens should not be considered equivalent to primary sedimentation but may be used in lieu of primary sedimentation where subsequent treatment units are designed on the basis of anticipated screen performance. Selection of screen capacity should consider flow restriction due to retained solids, gummy materials,

frequency of cleaning, and extent of cleaning. Where fine screens are used, additional provision for removal of floatable oils and greases shall be considered.

### **61.22 Design**

Tests should be conducted to determine BOD<sub>5</sub> and suspended solids removal efficiencies at the design maximum day flow and design maximum day BOD<sub>5</sub> loadings. Pilot testing for an extended time is preferred.

A minimum of two fine screens shall be provided, each unit being capable of independent operation. Capacity shall be provided to treat design peak instantaneous flow with one unit out of service.

Fine screens shall be preceded by a coarse bar screening device. Fine screens shall be protected from freezing and located to facilitate maintenance.

### **61.23 Electrical Equipment, Fixtures and Control**

Electrical equipment, fixtures and controls in the screening area where hazardous gases may accumulate shall meet the requirements of the National Electrical Code for Class I, Division 1, Group D locations.

### **61.24 Servicing**

Hosing equipment shall be provided to facilitate cleaning. Provision shall be made for isolating and removing units from their location for servicing.

## **62. COMMINUTORS**

### **62.1 General**

Provisions for access, ventilation, shields, and safety shall be in accordance with Paragraphs 61.13, 61.14, and 61.15.

### **62.2 When Used**

Comminutors may be used in lieu of screening devices to protect equipment where stringy substance accumulation on downstream equipment will not be a substantial problem.

### **62.3 Design Considerations**

#### **62.31 Location**

Comminutors should be located downstream of grit removal equipment and be protected by a coarse screening device. Comminutors not preceded by grit removal equipment shall be protected by a 6.0 inch (150 mm) deep gravel trap.

#### **62.32 Size**

Comminutor capacity shall be adequate to handle design peak hourly flow.

#### **62.33 Installation**

A screened bypass channel shall be provided. The use of the bypass channel should be automatic for all comminutor failures.

Gates shall be provided in accordance with Paragraphs 61.123 and 61.124.

#### **62.34 Servicing**

Provision shall be made to facilitate servicing units in place and removing units from their location for servicing.

#### **62.35 Electrical Controls and Motors**

Electrical equipment in comminutor chambers where hazardous gases may accumulate shall meet the requirements of the National Electrical Code for Class I, Division 1, Group D locations. Motors shall be protected against accidental submergence.

### **63. GRIT REMOVAL FACILITIES**

#### **63.1 When Required**

Grit removal facilities should be provided for all wastewater treatment plants, and are required for plants receiving wastewater from combined sewers or from sewer systems receiving substantial amounts of grit. If a plant serving a separate sewer system is designed without grit removal facilities, the design shall include provision for future installation. Consideration shall be given to possible damaging effects on pumps, comminutors, and other preceding equipment, and the need for additional storage capacity in treatment units where grit is likely to accumulate.

#### **63.2 Location**

##### **63.21 General**

Grit removal facilities should be located ahead of pumps and comminuting devices. Coarse bar racks should be placed ahead of grit removal facilities.

##### **63.22 Housed Facilities**

###### **63.221 Ventilation**

Refer to Paragraph 61.13. Fresh air shall be introduced continuously at a rate of at least 12 air changes per hour, or intermittently at a rate of at least 30 air changes per hour. Odor control facilities may also be warranted.

###### **63.222 Access**

Adequate stairway access to above or below grade facilities shall be provided.

###### **63.223 Electrical**

All electrical work in enclosed grit removal areas where hazardous gases may accumulate shall meet the requirements of the National Electrical Code for Class I, Division 1, Group D locations. Explosion proof gas detectors shall be provided in accordance with Section 57.

##### **63.23 Outside Facilities**

Grit removal facilities located outside shall be protected from freezing.

### **63.3 Type and Number of Units**

Plants treating waste from combined sewers should have at least two mechanically cleaned grit removal units, with provisions for bypassing. A single manually cleaned or mechanically cleaned grit chamber with bypass is acceptable for small wastewater treatment plants serving separate sanitary sewer systems. Minimum facilities for larger plants serving separate sanitary sewers should be at least one mechanically cleaned unit with a bypass.

Facilities other than channel-type shall be provided with adequate and flexible controls for velocity and/or air supply devices and with grit collection and removal equipment. Aerated grit chambers should have air rates adjustable in the range of 3 to 8 cubic feet per minute per foot [4.7 L/(m·s) to 12.4 L/(m·s)] of tank length. Detention time in the tank should be in the range of 3 to 5 minutes at design peak hourly flows.

### **63.4 Design Factors**

#### **63.41 General**

The design effectiveness of a grit removal system shall be commensurate with the requirements of the subsequent process units.

#### **63.42 Inlet**

Inlet turbulence shall be minimized in channel type units.

#### **63.43 Velocity and Detention**

Channel-type chambers shall be designed to control velocities during normal variations in flow as close as possible to 1 foot per second (0.3 m/s). The detention period shall be based on the size of particle to be removed. All aerated grit removal facilities should be provided with adequate control devices to regulate air supply and agitation.

#### **63.44 Grit Washing**

The need for grit washing should be determined by the method of grit handling and final disposal.

#### **63.45 Dewatering**

Provision shall be made for isolating and dewatering each unit. The design shall provide for complete draining and cleaning by means of a sloped bottom equipped with a drain sump.

#### **63.46 Water**

An adequate supply of water under pressure shall be provided for cleanup.

#### **63.47 Grit Handling**

Grit removal facilities located in deep pits should be provided with mechanical equipment for hoisting or transporting grit to ground level. Impervious, non-slip,

working surfaces with adequate drainage shall be provided for grit handling areas. Grit transporting facilities shall be provided with protection against freezing and loss of material.

#### **64. PREAERATION**

Preaeration of wastewater to reduce septicity may be required in special cases.

#### **65. FLOW EQUALIZATION**

##### **65.1 General**

Use of flow equalization should be considered where significant variations in organic and hydraulic loadings can be expected.

##### **65.2 Location**

Equalization basins should be located downstream of pretreatment facilities such as bar screens, comminutors, and grit chambers.

##### **65.3 Type**

Flow equalization can be provided by using separate basins or on-line treatment units, such as aeration tanks. Equalization basins may be designed as either in-line or side-line units. Unused treatment units, such as sedimentation or aeration tanks, may be utilized as equalization basins during the early period of design life.

##### **65.4 Size**

Equalization basin capacity should be sufficient to effectively reduce expected flow and load variations to the extent deemed to be economically advantageous. With a diurnal flow pattern, the volume required to achieve the desired degree of equalization can be determined from a cumulative flow plot over a representative 24-hour period.

##### **65.5 Operation**

###### **65.51 Mixing**

Aeration or mechanical equipment shall be provided to maintain adequate mixing. Corner fillets and hopper bottoms with draw-offs should be provided to alleviate the accumulation of sludge and grit.

###### **65.52 Aeration**

Aeration equipment shall be sufficient to maintain a minimum of 1.0 mg/L of dissolved oxygen in the mixed basin contents at all times. Air supply rates should be a minimum of 1.25 cfm/1000 gal [0.16 L/(m<sup>3</sup>:s)] of storage capacity. The air supply should be isolated from other treatment plant aeration requirements to facilitate process aeration control, although process air supply equipment may be utilized as a source of standby aeration.

###### **65.53 Controls**

Inlets and outlets for all basin compartments shall be suitably equipped with accessible external valves, stop plates, weirs, or other devices to permit flow control and the removal of an individual unit from service. Facilities shall also be

provided to measure and indicate liquid levels and flow rates.

#### **65.6 Electrical**

All electrical work in housed equalization basins, where hazardous concentrations of flammable gases or vapors may accumulate, shall meet the requirements of the National Electrical Code for Class I, Division 1, Group D locations.

#### **65.7 Access**

Suitable access shall be provided to facilitate cleaning and the maintenance of equipment.

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## CHAPTER 70 SETTLING

### 71. GENERAL

#### 71.1 Number of Units

Multiple units capable of independent operation are desirable and shall be provided in all plants where design average flows exceed 100,000 gallons/day (380 m<sup>3</sup>/d). Plants not having multiple units shall include other provisions to assure continuity of treatment.

#### 71.2 Flow Distribution

Effective flow splitting devices and control appurtenances (i.e., gates, splitter boxes, etc.) shall be provided to permit proper proportioning of flow and solids loading to each unit, throughout the expected range of flows. Refer to Paragraph 53.7.

### 72. DESIGN CONSIDERATIONS

#### 72.1 Dimensions

The minimum length of flow from inlet to outlet shall be 10 feet (3 m) unless special provisions are made to prevent short circuiting. The vertical side water depths shall be designed to provide an adequate separation zone between the sludge blanket and the overflow weirs. The side water depths shall not be less than the following values:

Type of Settling Tank	Minimum Side Water Depth ft (m)
Primary	10 (3.0)
Secondary tank following activated sludge process*	12 (3.7)
Secondary tank following attached growth biological reactor*	10 (3.0)

\* Greater side water depths are recommended for secondary clarifiers in excess of 4,000 square feet (372 m<sup>2</sup>) surface area [equivalent to 70 feet (21 m) diameter] and for nitrification plants. Less than 12 feet (3.7 m) side water depths may be permitted for package plants with a design average flow less than 25,000 gallons per day (95 m<sup>3</sup>/d), if justified based on successful operating experience.

#### 72.2 Surface Overflow Rates

##### 72.21 Primary Settling Tanks

Primary settling tank sizing should reflect the degree of solids removal needed and the need to avoid septic conditions during low flow periods. Sizing shall be calculated for both design average and design peak hourly flow conditions, and the larger surface area determined shall be used. The following surface overflow rates should not be exceeded in the design:

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Type of Primary Settling Tank	Surface Overflow Rates at: *	
	Design Average Flow gpd/ft <sup>2</sup> [m <sup>3</sup> /(m <sup>2</sup> ·d)]	Design Peak Hourly Flow gpd/ft <sup>2</sup> [m <sup>3</sup> /(m <sup>2</sup> ·d)]
Tanks not receiving waste activated sludge **	1,000 (41)	1,500 - 2,000 (61-81)
Tanks receiving waste activated sludge		1200 (49)

\* Surface overflow rates shall be calculated with all flows received at the settling tanks. Primary settling of normal domestic wastewater can be expected to remove approximately 1/3 of the influent BOD when operating at an overflow rate of 1000 gallons per day/square foot [41 m<sup>3</sup>/(m<sup>2</sup>·d)].

\*\* Anticipated BOD removal should be determined by laboratory tests and consideration of the character of the wastes. Significant reduction in BOD removal efficiency will result when the peak hourly overflow rate exceeds 1500 gallons per day/square foot [61 m<sup>3</sup>/(m<sup>2</sup>·d)].

### 72.22 Intermediate Settling Tanks

Surface overflow rates for intermediate settling tanks following series units of fixed film reactor processes shall not exceed 1,500 gallons per day per square foot [61 m<sup>3</sup>/(m<sup>2</sup>·d)] based on design peak hourly flow.

### 72.23 Final Settling Tanks

Settling tests shall be conducted wherever a pilot study of biological treatment is warranted by unusual waste characteristics, treatment requirements, or where proposed loadings go beyond the limits set forth in this Section.

#### 72.231 Final Settling Tanks - Attached Growth Biological Reactors

Surface overflow rates for settling tanks following trickling filters or rotating biological contactors shall not exceed 1,200 gallons per day per square foot [49 m<sup>3</sup>/(m<sup>2</sup>·d)] based on design peak hourly flow.

#### 72.232 Final Settling Tanks - Activated Sludge

To perform properly while producing a concentrated return flow, activated sludge settling tanks must be designed to meet thickening as well as solids separation requirements. Since the rate of recirculation of return sludge from the final settling tanks to the aeration or reaeration tanks is quite high in activated sludge processes, surface overflow rate and weir overflow rate should be adjusted for the various processes to minimize the problems with sludge loadings, density currents, inlet hydraulic turbulence, and occasional poor sludge settleability. The size of the settling tank must be based on the larger surface area determined for surface overflow rate and solids loading rate. The following design criteria shall not be exceeded:

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Treatment Process	Surface Overflow Rate at Design Peak Hourly Flow*	Peak Solids Loading Rate***
gpd/ft <sup>2</sup> [m <sup>3</sup> /(m <sup>2</sup> ·d)]	lb/day/ft <sup>2</sup> [kg/(m <sup>2</sup> ·d)]	
Conventional, Step Aeration, Complete Mix, Contact Stabilization, Carbonaceous Stage of Separate Stage Nitrification	1,200** (49)	50 (244)
Extended Aeration Single Stage Nitrification	1,000 (41)	35 (171)
2 Stage Nitrification	800 (33)	35 (171)
Activated Sludge with Chemical addition to Mixed Liquor for Phosphorus Removal	900**** (37)	As Above

\* Based on influent flow only.

\*\* Plants needing to meet 20 mg/L suspended solids should reduce surface overflow rate to 1,000 gallons per day per square foot [41 m<sup>3</sup>/(m<sup>2</sup>·d)].

\*\*\* Clarifier peak solids loading rate shall be computed based on the design maximum day flow rate plus the design maximum return sludge rate requirement and the design MLSS under aeration.

\*\*\*\* When phosphorus removal to a concentration of less than 1.0 mg/L is required.

### 72.3 Inlet Structures

Inlets and baffling shall be designed to dissipate the inlet velocity, to distribute the flow equally both horizontally and vertically and to prevent short circuiting. Channels shall be designed to maintain a velocity of at least 1 foot per second (0.3 m/s) at one-half of the design average flow. Corner pockets and dead ends shall be eliminated and corner fillets or channeling shall be used where necessary. Provisions shall be made for elimination or removal of floating materials which may accumulate in inlet structures.

### 72.4 Weirs

#### 72.41 General

Overflow weirs shall be readily adjustable over the life of the structure to correct for differential settlement of the tank.

#### 72.42 Location

Overflow weirs shall be located to optimize actual hydraulic detention time, and minimize short circuiting. Peripheral weirs shall be placed at least 1 foot (0.3 m) from the wall.

#### 72.43 Design Rates

Weir loadings shall not exceed:

Average Plant Capacity	Loading Rate at Design Peak Hourly Flow gpd/lin ft [m <sup>3</sup> /(m·d)]
equal to or less than 1 mgd (3785 m <sup>3</sup> /d)	20,000 (250)
greater than 1 mgd (3785 m <sup>3</sup> /d)	30,000 (375)

If pumping is required, the pumps shall be operated as nearly continuous as possible. Also, weir loadings should be related to pump delivery rates to avoid short circuiting.

#### 72.44 Weir Troughs

Weir troughs shall be designed to prevent submergence at design peak hourly flow, and to maintain a velocity of at least 1 foot per second (0.3 m/s) at one-half design average flow.

#### 72.5 Submerged Surface

The tops of troughs, beams, and similar submerged construction elements shall have a minimum slope of 1.4 vertical to 1 horizontal; the underside of such elements shall have a slope of 1 to 1 to prevent the accumulation of scum and solids.

#### 72.6 Unit Dewatering

Unit dewatering features shall conform to the provisions outlined in Paragraph 54.3. The bypass design shall also provide for distribution of the plant flow to the remaining units.

#### 72.7 Freeboard

Walls of settling tanks shall extend at least 6 inches (150 mm) above the surrounding ground surface and shall provide not less than 12 inches (300 mm) freeboard. Additional freeboard or the use of wind screens is recommended where larger settling tanks are subject to high velocity wind currents that would cause tank surface waves and inhibit effective scum removal.

### 73. SLUDGE AND SCUM REMOVAL

#### 73.1 Scum Removal

Full surface mechanical scum collection and removal facilities, including baffling, shall be provided for all settling tanks. The unusual characteristics of scum which may adversely affect pumping, piping, sludge handling and disposal, shall be recognized in design. Provisions shall be made to remove scum from the wastewater treatment process and direct it to the sludge treatment process. Other special provisions for disposal may

be necessary.

## **73.2 Sludge Removal**

Mechanical sludge collection and withdrawal facilities shall be designed to assure rapid removal of the sludge. Suction withdrawal should be provided for activated sludge clarifiers over 60 feet (18 m) in diameter, especially for activated sludge plants that nitrify.

Each settling tank shall have its own sludge withdrawal lines to ensure adequate control of sludge wasting rate for each tank.

### **73.21 Sludge Hopper**

The minimum slope of the side walls shall be 1.7 vertical to 1 horizontal. Hopper wall surfaces should be made smooth with rounded corners to aid in sludge removal. Hopper bottoms shall have a maximum dimension of 2 feet (0.6 m). Extra depth sludge hoppers for sludge thickening are not acceptable.

### **73.22 Cross-Collectors**

Cross-collectors serving one or more settling tanks may be useful in place of multiple sludge hoppers.

### **73.23 Sludge Removal Pipeline**

Each hopper shall have an individually valved sludge withdrawal line at least 6 inches (150 mm) in diameter. The static head available for withdrawal of sludge shall be 30 inches (760 mm) or greater, as necessary to maintain a 3 foot per second (0.9 m/s) velocity in the withdrawal pipe. Clearance between the end of the withdrawal line and the hopper walls shall be sufficient to prevent "bridging" of the sludge. Adequate provisions shall be made for rodding or back-flushing individual pipe runs. Provisions shall be made to allow for visual confirmation of return sludge. Piping shall be provided to return sludge for further processing.

### **73.24 Sludge Removal Control**

Separate settling tank sludge lines may drain to a common sludge well.

Sludge wells equipped with telescoping valves or other appropriate equipment shall be provided for viewing, sampling, and controlling the rate of sludge withdrawal. A means of measuring the sludge removal rate shall be provided. Air-lift type of sludge removal will not be approved for removal of primary sludges.

## **74. PROTECTIVE AND SERVICE FACILITIES**

### **74.1 Operator Protection**

All settling tanks shall be equipped to enhance safety for operators. Such features shall appropriately include machinery covers, life lines, stairways, walkways, handrails, and slip resistant surfaces.

### **74.2 Mechanical Maintenance Access**

The design shall provide for convenient and safe access to routine maintenance items

such as gear boxes, scum removal mechanisms, baffles, weirs, inlet stilling baffle areas, and effluent channels.

### **74.3 Electrical Equipment, Fixtures and Controls**

Electrical equipment, fixtures and controls in enclosed settling basins and scum tanks, where hazardous concentrations of flammable gases or vapors may accumulate, shall meet the requirements of the National Electrical Code for Class 1, Division 1, Group D locations.

The fixtures and controls shall be located so as to provide convenient and safe access for operation and maintenance. Adequate area lighting shall be provided.

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## **CHAPTER 80 SLUDGE PROCESSING, STORAGE, AND DISPOSAL**

### **81. GENERAL**

Facilities for processing sludge shall be provided at all mechanical wastewater treatment plants. Handling equipment shall be capable of processing sludge to a form suitable for ultimate disposal unless provisions acceptable to the regulatory agency are made for processing the sludge at an alternate location.

The reviewing authority should be contacted if sludge unit processes not described in this Chapter are being considered or are necessary to meet state, provincial, or federal sludge disposal requirements.

### **82. PROCESS SELECTION**

The selection of sludge handling unit processes should be based upon at least the following considerations:

- a. Local land use;
- b. System energy requirements;
- c. Cost effectiveness of sludge thickening and dewatering;
- d. Equipment complexity and staffing requirements;
- e. Adverse effects of heavy metals and other sludge components upon the unit processes;
- f. Sludge digestion or stabilization requirements, including appropriate pathogen and vector attraction reduction;
- g. Side stream or return flow treatment requirements (e.g., digester or sludge storage facilities supernatant, dewatering unit filtrate, wet oxidation return flows);
- h. Sludge storage requirements;
- i. Methods of ultimate disposal; and
- j. Back-up techniques of sludge handling and disposal.

### **83. SLUDGE THICKENERS**

#### **83.1 Design Considerations**

Sludge thickeners to reduce the volume of sludge should be considered. The design of thickeners (gravity, dissolved-air flotation, centrifuge, and others) should consider the type and concentration of sludge, the sludge stabilization processes, storage requirements, the method of ultimate sludge disposal, chemical needs, and the cost of operation.

The use of gravity thickening tanks for unstabilized sludges is not recommended because of problems due to septicity unless provisions are made for adequate control of process operational problems and odors at the gravity thickener and any following unit processes.

Particular attention should be given to the pumping and piping of the concentrated sludge and possible onset of anaerobic conditions.

## **83.2 Prototype Studies**

Process selection and unit process design parameters should be based on prototype studies. The reviewing authority will require such studies where the sizing of other plant units is dependent on performance of the thickeners. Refer to Paragraph 53.2 for any new process determination.

## **84. ANAEROBIC SLUDGE DIGESTION**

### **84.1 General**

#### **84.11 Multiple Units**

Multiple units or alternate methods of sludge processing shall be provided. Facilities for sludge storage and supernatant separation in an additional unit may be required, depending on raw sludge concentration and disposal methods for sludge and supernatant.

#### **84.12 Depth**

If process design provides for supernatant withdrawal, the proportion of depth to diameter should be such as to allow for the formation of a reasonable depth of supernatant liquor. A minimum side water depth of 20 feet (6.1 m) is recommended.

#### **84.13 Design Maintenance Provisions**

To facilitate emptying, cleaning, and maintenance, the following features are desirable:

##### **84.131 Slope**

The tank bottom shall slope to drain toward the withdrawal pipe. For tanks equipped with a suction mechanism for sludge withdrawal, a bottom slope not less than 1 to 12 is recommended. Where the sludge is to be removed by gravity alone, 1 to 4 slope is recommended.

##### **84.132 Access Manholes**

At least 2 access manholes not less than 30 inches (760 mm) in diameter should be provided in the top of the tank in addition to the gas dome. There should be stairways to reach the access manholes.

A separate side wall manhole shall be provided that is large enough to permit the use of mechanical equipment to remove grit and sand. The side wall access manhole should be low enough to facilitate heavy equipment handling and may be buried in the earthen bank insulation.

##### **84.133 Safety**

Non-sparking tools, rubber-soled shoes, safety harness, gas detectors for flammable and toxic gases, and at least two self-contained breathing units shall be provided for emergency use. Refer to other safety items as appropriate in Section 57.

#### **84.14 Toxic Materials**

If the anaerobic digestion process is proposed, the basis of design shall be supported by wastewater analyses to determine the presence of undesirable materials, such as high concentrations of sulfates and inhibitory concentrations of heavy metals.

### **84.2 Sludge Inlets, Outlets, Recirculation, and High Level Overflow**

#### **84.21 Multiple Inlets and Draw-Offs**

Multiple sludge inlets and draw-offs and, where used, multiple recirculation suction and discharge points to facilitate flexible operation and effective mixing of the digester contents, shall be provided unless adequate mixing facilities are provided within the digester.

#### **84.22 Inlet Configurations**

One inlet should discharge above the liquid level and be located at approximately the center of the tank to assist in scum breakup. The second inlet should be opposite to the suction line at approximately the 2/3 diameter point across the digester.

#### **84.23 Inlet Discharge Location**

Raw sludge inlet discharge points should be so located as to minimize short circuiting to the digested sludge or supernatant draw-offs.

#### **84.24 Sludge Withdrawal**

Sludge withdrawal to disposal should be from the bottom of the tank. The bottom withdrawal pipe should be interconnected with the necessary valving to the recirculation piping, to increase operational flexibility in mixing the tank contents.

#### **84.25 Emergency Overflow**

An unvalved vented overflow shall be provided to prevent damage to the digestion tank and cover in case of accidental overfilling. This emergency overflow shall be piped to an appropriate point and at an appropriate rate in the treatment process or sidestream treatment facilities to minimize the impact on process units.

### **84.3 Tank Capacity**

#### **84.31 Rational Design**

The total digestion tank capacity shall be determined by rational calculations based upon such factors as: volume of sludge added, percent solids, and character; the temperature to be maintained in the digesters; the degree or extent of mixing to be obtained; the degree of volatile solids reduction required; the solids retention time at peak loadings; method of sludge disposal and the size of the installation with appropriate allowances for gas, scum, supernatant, and digested sludge storage. Secondary digesters of two-stage series digestion systems which are utilized for digested sludge storage and concentration shall not be credited in the calculations for volumes required for sludge digestion. Calculations should be

submitted to justify the basis of design.

### **84.32 Standard Design**

When such calculations are not submitted to justify the design based on the above factors, the minimum digestion tank capacity outlined below will be required. Such requirements assume that the raw sludge is derived from ordinary domestic wastewater, a digestion temperature is to be maintained in the range of 85° to 95° F (29 °C to 35 °C), 40 to 50 percent volatile matter in the digested sludge, and that the digested sludge will be removed frequently from the process. (See also Paragraphs 84.11 and 89.11.)

#### **84.321 Completely Mixed Systems**

For digestion systems providing for intimate and effective mixing of the digester contents, the system may be loaded up to 80 pounds of volatile solids per 1000 cubic feet of volume per day [ $1.3 \text{ kg}/(\text{m}^3 \cdot \text{d})$ ] in the active digestion units.

#### **84.322 Moderately Mixed Systems**

For digestion systems where mixing is accomplished only by circulating sludge through an external heat exchanger, the system may be loaded up to 40 pounds of volatile solids per 1000 cubic feet of volume per day [ $0.65 \text{ kg}/(\text{m}^3 \cdot \text{d})$ ] in the active digestion units. This loading may be modified upward or downward depending upon the degree of mixing provided.

#### **84.323 Multistage Systems**

For digestion systems utilizing two stages (primary and secondary units), the first stage (primary) may be either completely mixed or moderately mixed and loaded in accordance with Paragraphs 84.321 or 84.322. The second stage (secondary) is to be designed for sludge storage, concentration, and gas collection and shall not be credited in the calculations for volumes required for sludge digestion.

#### **84.324 Digester Mixing**

Facilities for mixing the digester contents shall be provided where required for proper digestion by reason of loading rates or other features of the system. Where sludge recirculation pumps are used for mixing they shall be provided in accordance with appropriate requirements of Paragraph 87.1.

### **84.4 Gas Collection, Piping, and Appurtenances**

#### **84.41 General**

All portions of the gas system including the space above the tank liquor, storage facilities, and piping shall be so designed that under all normal operating conditions, including sludge withdrawal, the gas will be maintained under pressure. All enclosed areas where any gas leakage might occur shall be adequately ventilated.

#### **84.42 Safety Equipment**

All necessary safety facilities shall be included where gas is produced. Pressure and vacuum relief valves and flame traps together with automatic safety shut off valves shall be provided and protected from freezing. Water seal equipment shall not be installed. Safety equipment and gas compressors should be housed in a separate room with an exterior door.

#### **84.43 Gas Piping and Condensate**

Gas piping shall have a minimum diameter of 4 inches (100 mm). A smaller diameter pipe at the gas production meter is acceptable. Gas piping shall slope to condensation traps at low points. The use of float-controlled condensate traps is not permitted. Condensation traps shall be protected from freezing.

Tightly fitted self-closing doors should be provided at connecting passageways and tunnels which connect digestion facilities to other facilities to minimize the spread of gas. Piping galleries shall be ventilated in accordance with Paragraph 84.47.

#### **84.44 Gas Utilization Equipment**

Gas burning boilers, engines, etc., shall be located in well-ventilated rooms. Such rooms would not ordinarily be classified as a hazardous location if isolated from the digestion gallery. Gas lines to these units shall be provided with suitable flame traps.

#### **84.45 Electrical Equipment, Fixtures, and Controls**

Electrical equipment, fixtures and controls, in places enclosing and adjacent to anaerobic digestion appurtenances, where hazardous gases may accumulate shall comply with the National Electric Code for Class 1, Division 1, Group D locations.

#### **84.46 Waste Gas**

##### **84.461 Location**

Waste gas burners shall be readily accessible and should be located at least 50 feet (15 m) away from any plant structure. Waste gas burners shall be of sufficient height and so located to prevent injury to personnel due to wind or downdraft conditions.

##### **84.462 Pilot Light**

All waste gas burners shall be equipped with automatic ignition such as a pilot light or a device using a photoelectric cell sensor. Consideration should be given to the use of natural or propane gas to ensure reliability of the pilot.

##### **84.463 Gas Piping Slope**

Gas piping shall be sloped at a minimum of 2 percent up to the waste gas burner with a condensate trap provided in a location not subject to freezing.

#### **84.47 Ventilation**

Any underground enclosures connecting with digestion tanks or containing sludge or gas piping or equipment shall be provided with forced ventilation for dry wells in accordance with Paragraphs 42.71 through 42.74 and 42.76. The ventilation rate for Class 1, Division 2, Group D locations including enclosed areas without a gas tight partition from the digestion tank or areas containing gas compressors, sediment traps, drip traps, gas scrubbers, or pressure regulating and control valves, if continuous, shall be at least 12 complete air changes per hour.

#### **84.48 Meter**

A gas meter with bypass shall be provided, to meter total gas production for each active digestion unit. Total gas production for two-stage digestion systems operated in series may be measured by a single gas meter with proper interconnected gas piping.

Where multiple primary digestion units are utilized with a single secondary digestion unit, a gas meter shall be provided for each primary digestion unit. The secondary digestion unit may be interconnected with the gas measurement unit of one of the primary units. Interconnected gas piping shall be properly valved with gas tight gate valves to allow measurement of gas production from either digestion unit or maintenance of either digestion unit.

Gas meters may be of the orifice plate, turbine or vortex type. Positive displacement meters should not be utilized. The meter must be specifically designed for contact with corrosive and dirty gases.

### **84.5 Digestion Tank Heating**

#### **84.51 Insulation**

Wherever possible digestion tanks should be constructed above ground-water level and shall be suitably insulated to minimize heat loss. Maximum utilization of earthen bank insulation should be used.

#### **84.52 Heating Facilities**

Sludge may be heated by circulating the sludge through external heaters or by units located inside the digestion tank. Refer to Paragraph 84.522.

##### **84.521 External Heating**

Piping shall be designed to provide for the preheating of feed sludge before introduction into the digesters. Provisions shall be made in the layout of the piping and valving to facilitate heat exchanger tube removal and cleaning of the lines. Heat exchanger sludge piping should be sized for peak heat transfer requirements. Heat exchangers should have a heating capacity of 130 percent of the calculated peak heating requirement to account for the occurrence of sludge tube fouling.

##### **84.522 Other Heating Methods**

- a. The use of hot water heating coils affixed to the walls of the digester, or other types of internal heating equipment that require emptying the digester contents for repair, are not acceptable.

- b. Other systems and devices have been developed recently to provide both mixing and heating of anaerobic digester contents. These systems will be reviewed on their own merits. Operating data detailing their reliability, operation, and maintenance characteristics will be required. Refer to Paragraph 53.2.

## **84.53 Heating Capacity**

### **84.531 Capacity**

Sufficient heating capacity shall be provided to consistently maintain the design sludge temperature considering insulation provisions and ambient cold weather conditions. Where digestion tank gas is used for other purposes, an auxiliary fuel may be required. The design operating temperature should be in the range of 85° to 100°F (29 °C to 38 °C) where optimum mesophilic digestion is required.

### **84.532 Standby Requirements**

The provision of standby heating capacity or the use of multiple units sized to provide the heating requirements shall be considered unless acceptable alternative means of handling raw sludge are provided for the extended period that digestion process outage is experienced due to heat loss.

## **84.54 Hot Water Internal Heating Controls**

### **84.541 Mixing Valves**

A suitable automatic mixing valve shall be provided to temper the boiler water with return water so that the inlet water to the removable heat jacket or coil in the digester can be held below a temperature at which caking will be accentuated. Manual control should also be provided by suitable bypass valves.

### **84.542 Boiler Controls**

The boiler should be provided with suitable automatic controls to maintain the boiler temperature at approximately 180°F (82 °C) to minimize corrosion and to shut off the main gas supply in the event of pilot burner or electrical failure, low boiler water level, low gas pressure, or excessive boiler water temperature or pressure.

### **84.543 Boiler Water Pumps**

Boiler water pumps shall be sealed and sized to meet the operating conditions of temperature, operating head, and flow rate. Duplicate units shall be provided.

### **84.544 Thermometers**

Thermometers shall be provided to show inlet and outlet temperatures of the sludge, hot water feed, hot water return, and boiler water.

### **84.545 Water Supply**

The chemical quality should be checked for suitability for this use. Refer to Paragraph 56.23 for required break tank for indirect water supply connections.

#### **84.55 External Heater Operating Controls**

All controls necessary to ensure effective and safe operation are required. Provision for duplicate units in critical elements should be considered.

### **84.6 Supernatant Withdrawal**

Where supernatant separation is to be used to concentrate sludge in the digester units and increase digester solids retention time, the design shall provide for ease of operation and positive control of supernatant quality.

#### **84.61 Piping Size**

Supernatant piping should not be less than 6 inches (150 mm) in diameter.

#### **84.62 Withdrawal Arrangements**

##### **84.621 Withdrawal Levels**

Piping should be arranged so that withdrawal can be made from three or more levels in the tank. An unvalved vented overflow shall be provided. The emergency overflow shall be piped to an appropriate point and at an appropriate rate in the treatment process or side stream treatment units to minimize the impact on process units.

##### **84.622 Withdrawal Selection**

On fixed cover tanks the supernatant withdrawal level should preferably be selected by means of interchangeable extensions at the discharge end of the piping.

##### **84.623 Supernatant Selector**

A fixed screen supernatant selector or similar type device shall be limited for use in an unmixed secondary digestion unit. If such supernatant selector is provided, provisions shall be made for at least one other draw-off level located in the supernatant zone of the tank, in addition to the unvalved emergency supernatant draw-off pipe. High pressure back-wash facilities shall be provided.

#### **84.63 Sampling**

Provision shall be made for sampling at each supernatant draw-off level. Sampling pipes should be at least 1½ inches (40 mm) in diameter and should terminate at a suitably sized sampling sink or basin.

#### **84.64 Supernatant Disposal**

Supernatant return and disposal facilities should be designed to alleviate adverse hydraulic and organic effects on plant operations. If nutrient removal (e.g., phosphorus, ammonia nitrogen) must be accomplished at a plant, then a separate supernatant side stream treatment system should be provided.

### 84.7 Anaerobic Digestion Sludge Production

For calculating design sludge handling and disposal needs, sludge production values from a two-stage anaerobic digestion process shall be based on a maximum solids concentration of 5 percent without additional thickening. The solids production values on a dry weight basis shall be based on the following for the listed processes:

Primary plus waste activated sludge - at least 0.12 lb/P.E./day [0.05 kg/(P.E.·d)].

Primary plus fixed film sludge - at least 0.09 lb/P.E./day [0.04 kg/(P.E.·d)].

## 85. AEROBIC SLUDGE DIGESTION

### 85.1 General

The aerobic sludge digestion system shall include provisions for digestion, supernatant separation, sludge concentration, and any necessary sludge storage. These provisions may be accomplished by separate tanks or processes, or in the digestion tanks.

### 85.2 Multiple Units

Multiple digestion units capable of independent operation are desirable and shall be provided in all plants where the design average flow exceeds 100,000 gallons per day (380 m<sup>3</sup>/d). All plants not having multiple units shall provide alternate sludge handling and disposal methods.

### 85.3 Tank Capacity

#### 85.31 Volume Required

The following digestion tank capacities are based on a solids concentration of 2 percent with supernatant separation performed in a separate tank. If supernatant separation is performed in the digestion tank, a minimum of 25 percent additional volume is required. These capacities shall be provided unless sludge thickening facilities (refer to Section 83) are utilized to thicken the feed solids concentration to greater than 2 percent. If such thickening is provided, the digestion volumes may be decreased proportionally.

Sludge Source	Volume/Population Equivalent
	ft <sup>3</sup> /P.E. (m <sup>3</sup> /P.E.)
Waste activated sludge -- no primary settling	4.5 (0.13)*
Primary plus waste activated sludge	4.0 (0.11)*
Waste activated sludge exclusive of primary sludge	2.0 (0.06)*
Extended aeration activated sludge	3.0 (0.09)
Primary plus attached growth biological reactor sludge	3.0 (0.09)

\* These volumes also apply to waste activated sludge from single stage

nitrification facilities with less than 24 hours detention time based on design average flow.

### **85.32 Effect of Temperature on Volume**

The volumes in Paragraph 85.31 are based on digester temperatures of 59°F (15 °C) and a solids retention time of 27 days. Aerobic digesters should be covered to minimize heat loss for colder temperature applications. Additional volume or supplemental heat may be required if the land application disposal method is used in order to meet applicable U.S. EPA requirements. Refer to Paragraph 85.9 for necessary sludge storage.

### **85.4 Mixing**

Aerobic digesters shall be provided with mixing equipment which can maintain solids in suspension and ensure complete mixing of the digester contents. Refer to Paragraph 85.5.

### **85.5 Air Requirements**

Sufficient air shall be provided to keep the solids in suspension and maintain dissolved oxygen between 1 mg/L and 2 mg/L. For minimum mixing and oxygen requirements, an air supply of 30 cfm/1000 ft<sup>3</sup> [0.5 L/(m<sup>3</sup>·s)] of tank volume shall be provided with the largest blower out of service. If diffusers are used, the nonclog type is recommended, and they should be designed to permit continuity of service. If mechanical turbine aerators are utilized, at least two turbine aerators per tank shall be provided to permit continuity of service. Mechanical aerators are not recommended for use in aerobic digesters where freezing conditions will cause ice build-up on the aerator and support structures.

### **85.6 Supernatant Separation and Scum and Grease Removal**

#### **85.61 Supernatant Separation**

Facilities shall be provided for effective separation or decanting of supernatant. Separate facilities are recommended; however, supernatant separation may be accomplished in the digestion tank provided additional volume is provided per Paragraph 85.3. The supernatant drawoff unit shall be designed to prevent recycle of scum and grease back to plant process units. Provision should be made to withdraw supernatant from multiple levels of the supernatant withdrawal zone.

#### **85.62 Scum and Grease Removal**

Facilities shall be provided for the effective collection of scum and grease from the aerobic digester for final disposal and to prevent its recycle back to the plant process and to prevent long term accumulation and potential discharge in the effluent.

### **85.7 High Level Emergency Overflow**

An unvalved high level overflow and any necessary piping shall be provided to return digester overflow back to the head of the plant or to the aeration process in case of accidental overfilling. Design considerations related to the digester overflow shall include waste sludge rate and duration during the period the plant is unattended, potential effects on plant process units, discharge location of the emergency overflow, and potential discharge of suspended solids in the plant effluent.

## 85.8 Aerobic Digestion Sludge Production

For calculating design sludge handling and disposal needs, sludge production values from aerobic digesters shall be based on a maximum solids concentration of 2 percent without additional thickening. The solids production values on a dry weight basis shall be based on the following for the listed processes:

Primary plus waste activated sludge - at least 0.16 lb/P.E./day [0.07 kg/(P.E.·d)].

Primary plus fixed film sludge - at least 0.12 lb/P.E./day [0.05 kg/(P.E.·d)].

## 85.9 Digested Sludge Storage Volume

### 85.91 Sludge Storage Volume

Sludge storage must be provided in accordance with Section 89 to accommodate daily sludge production volumes and as an operational buffer for unit outage and adverse weather conditions. Designs utilizing increased sludge age in the activated sludge system as a means of storage are not acceptable.

### 85.92 Liquid Sludge Storage

Liquid sludge storage facilities shall be based on the following values unless digested sludge thickening facilities are utilized (refer to Section 83) to provide solids concentrations of greater than 2 percent.

ft <sup>3</sup> /P.E./day [m <sup>3</sup> /(P.E.·d)]	
Sludge Source	Volume/Population Equivalent
Waste activated sludge -- no primary settling, primary plus waste activated sludge, and extended aeration activated sludge	0.13 (0.004)
Waste activated sludge exclusive of primary sludge	0.06 (0.002)
Primary plus attached growth biological reactor sludge	0.10 (0.003)

## 86. HIGH pH STABILIZATION

### 86.1 General

Alkaline material may be added to liquid primary or secondary sludges for sludge stabilization in lieu of digestion facilities; to supplement existing digestion facilities; or for interim sludge handling. There is no direct reduction of organic matter or sludge solids with the high pH stabilization process. There is an increase in the mass of dry sludge solids. Without supplemental dewatering, additional volumes of sludge will be generated. The design shall account for the increased sludge quantities for storage, handling, transportation, and disposal methods and associated costs.

### 86.2 Operational Criteria

Sufficient alkaline material shall be added to liquid sludge in order to produce a

homogeneous mixture with a minimum pH of 12 after 2 hours of vigorous mixing. Facilities for adding supplemental alkaline material shall be provided to maintain the pH of the sludge during interim sludge storage periods.

### **86.3 Odor Control and Ventilation**

Odor control facilities shall be provided for sludge mixing and treated sludge storage tanks when located within 1/2 mile (0.8 km) of residential or commercial areas. The reviewing authority should be contacted for design and air pollution control objectives to be met for various types of air scrubber units. Ventilation is required for indoor sludge mixing, storage or processing facilities in accordance with Paragraph 42.75.

### **86.4 Mixing Tanks and Equipment**

#### **86.41 Tanks**

Mixing tanks may be designed to operate as either a batch or continuous flow process. A minimum of two tanks shall be provided of adequate size to provide a minimum 2 hours contact time in each tank. The following items shall also be considered in determining the number and size of tanks:

- a. peak sludge flow rates;
- b. storage between batches;
- c. dewatering or thickening performed in tanks;
- d. repeating sludge treatment due to pH decay of stored sludge;
- e. sludge thickening prior to sludge treatment; and
- f. type of mixing device used and associated maintenance or repair requirements.

#### **86.42 Equipment**

Mixing equipment shall be designed to provide vigorous agitation within the mixing tank, maintain solids in suspension and provide for a homogeneous mixture of the sludge solids and alkaline material. Mixing may be accomplished either by diffused air or mechanical mixers. If diffused aeration is used, an air supply of 30 cfm/1000 ft<sup>3</sup> [0.5 L/(m<sup>3</sup>·s)] of mixing tank volume shall be provided with the largest blower out of service. When diffusers are used, the nonclog type is recommended, and they should be designed to permit continuity of service. If mechanical mixers are used, the impellers shall be designed to minimize fouling with debris in the sludge and consideration shall be made to provide continuity of service during freezing weather conditions.

### **86.5 Chemical Feed and Storage Equipment**

#### **86.51 General**

Alkaline material is caustic in nature and can cause eye and tissue injury. Equipment for handling or storing alkaline material shall be designed for adequate operator safety. Refer to Section 57 for proper safety precautions. Storage, slaking, and feed equipment should be sealed as airtight as practical to prevent contact of alkaline material with atmospheric carbon dioxide and water vapor and

to prevent the escape of dust material. All equipment and associated transfer lines or piping shall be accessible for cleaning.

### **86.52 Feed and Slaking Equipment**

The design of the feeding equipment shall be determined by the treatment plant size, type of alkaline material used, slaking required, and operator requirements. Equipment may be either of batch or automated type. Automated feeders may be of the volumetric or gravimetric type depending on accuracy, reliability, and maintenance requirements. Manually operated batch slaking of quicklime (CaO) should be avoided unless adequate protective clothing and equipment are provided. At small plants, use of hydrated lime [Ca(OH)<sub>2</sub>] is recommended over quicklime due to safety and labor-saving reasons. Feed and slaking equipment shall be sized to handle a minimum of 150% of the peak sludge flow rate including sludge that may need to be retreated due to pH decay. Duplicate units shall be provided.

### **86.53 Chemical Storage Facilities**

Alkaline materials may be delivered either in bag or bulk form depending upon the amount of material used. Material delivered in bags must be stored indoors and elevated above floor level. Bags should be of the multi-wall moisture-proof type. Dry bulk storage containers must be as airtight as practical and shall contain a mechanical agitation mechanism. Storage facilities shall be sized to provide a minimum of a 30-day supply.

## **86.6 Sludge Storage**

Refer to Section 89 for general design considerations for sludge storage facilities. The design shall incorporate the following considerations for the storage of high pH stabilized sludge:

### **86.61 Liquid Sludge**

Liquid high pH stabilized sludge shall not be stored in a lagoon. Said sludge shall be stored in a tank or vessel equipped with rapid sludge withdrawal mechanisms for sludge disposal or retreatment. Provisions shall be made for adding alkaline material in the storage tank. Mixing equipment in accordance with Paragraph 86.42 above shall also be provided in all storage tanks.

### **86.62 Dewatered Sludge**

On-site storage of dewatered high pH stabilized sludge should be limited to 30 days. Provisions for rapid retreatment or disposal of dewatered sludge stored on-site shall also be made in case of sludge pH decay.

### **86.63 Off-Site Storage**

There shall be no off-site storage of high pH stabilized sludge unless specifically permitted by the regulatory agency.

## **86.7 Disposal**

Immediate sludge disposal methods and options are recommended to be utilized in order to reduce the sludge inventory on the treatment plant site and amount of sludge that may need to be retreated to prevent odors if sludge pH decay occurs. If the land application

disposal option is utilized for high pH stabilized sludge, said sludge should be incorporated into the soil during the same day of delivery to the site.

## **87. SLUDGE PUMPS AND PIPING**

### **87.1 Sludge Pumps**

#### **87.11 Capacity**

Pump capacities shall be adequate but not excessive. Provision for varying pump capacity is desirable. A rational basis of design shall be provided with the plan documents.

#### **87.12 Duplicate Units**

Duplicate units shall be provided at all installations.

#### **87.13 Type**

Plunger pumps, screw feed pumps or other types of pumps with demonstrated solids handling capability shall be provided for handling raw sludge. Where centrifugal pumps are used, a parallel positive displacement pump shall be provided as an alternate to pump heavy sludge concentrations, such as primary or thickened sludge, that may exceed the pumping head of the centrifugal pump.

#### **87.14 Minimum Head**

A minimum positive head of 24 inches (610 mm) shall be provided at the suction side of centrifugal type pumps and is desirable for all types of sludge pumps. Maximum suction lifts should not exceed 10 feet (3 m) for plunger pumps.

#### **87.15 Sampling Facilities**

Unless sludge sampling facilities are otherwise provided, quick-closing sampling valves shall be installed at the sludge pumps. The size of valve and piping should be at least 1½ inches (40 mm) and terminate at a suitably sized sampling sink or floor drain.

### **87.2 Sludge Piping**

#### **87.21 Size and Head**

Digested sludge withdrawal piping should have a minimum diameter of 8 inches (200 mm) for gravity withdrawal and 6 inches (150 mm) for pump suction and discharge lines. Where withdrawal is by gravity, the available head on the discharge pipe should be at least 4 feet (1.2 m) and preferably more. Undigested sludge withdrawal piping shall be sized in accordance with Paragraph 73.23.

#### **87.22 Slope and Flushing Requirements**

Gravity piping should be laid on uniform grade and alignment. Slope on gravity discharge piping should not be less than 3 percent for primary sludges and all sludges thickened to greater than 2 percent solids. Slope on gravity discharge piping should not be less than 2 percent for aerobically digested sludge or waste activated sludge with less than 2 percent solids. Cleanouts shall be provided for all gravity sludge piping. Provisions shall be made for draining and flushing

discharge lines. All sludge piping shall be suitably located or otherwise adequately protected to prevent freezing.

### **87.23 Supports**

Special consideration shall be given to the corrosion resistance and permanence of supporting systems for piping located inside the digestion tank.

## **88. SLUDGE DEWATERING**

### **88.1 General**

On-site sludge dewatering facilities shall be provided for all plants, although the following requirements may be reduced with on-site liquid sludge storage facilities or approved off-site sludge disposal.

For calculating design sludge handling and disposal needs for sludge stabilization processes other than described in Paragraphs 84.7 for anaerobic digestion and 85.8 for aerobic digestion, a rational basis of design for sludge production values shall be developed and provided to the reviewing authority for approval on a case-by-case basis.

### **88.2 Sludge Drying Beds**

#### **88.21 Applicability**

Sludge drying beds may be used for dewatering well digested sludge from either the anaerobic or aerobic process. Due to the large volume of sludge produced by the aerobic digestion process, consideration should be given to using a combination of dewatering systems or other means of ultimate sludge disposal.

#### **88.22 Unit Sizing**

Sludge drying bed area shall be calculated on a rational basis with the following items considered:

- a. The volume of wet sludge produced by existing and proposed processes.
- b. Depth of wet sludge drawn to the drying beds. For design calculation purposes a maximum depth of 8 inches (200 mm) shall be utilized. For operational purposes, the depth of sludge placed on the drying bed may increase or decrease from the design depth based on the percent solids content and type of digestion utilized.
- c. Total digester volume and other wet sludge storage facilities.
- d. Degree of sludge thickening provided after digestion.
- e. The maximum drawing depth of sludge which can be removed from the digester or other sludge storage facilities without causing process or structural problems.
- f. The time required on the bed to produce a removable cake. Adequate provision shall be made for sludge dewatering and/or sludge disposal facilities for those periods of time during which outside drying of sludge on beds is hindered by weather.

- g. Capacities of auxiliary dewatering facilities.

## **88.23 Percolation Type Bed Components**

### **88.231 Gravel**

The lower course of gravel around the underdrains should be properly graded and should be at least 12 inches (300 mm) in depth, extending at least 6 inches (150 mm) above the top of the underdrains. It is desirable to place this in two or more layers. The top layer of at least 3 inches (80 mm) should consist of gravel 1/8 to 1/4 inch (3 mm to 6 mm) in size.

### **88.232 Sand**

The top course should consist of at least 9 to 12 inches (230 mm to 300 mm) of clean, hard, and washed coarse sand. The effective size of the sand should be in the range of 0.8 mm to 1.5 mm. The finished sand surface should be level.

### **88.233 Underdrains**

Underdrains should be at least 4 inches (100 mm) in diameter laid with open joints. Perforated pipe may also be used. Underdrains should be spaced not more than 20 feet (6.1 m) apart and sloped at a minimum of 1 percent. Lateral tiles should be spaced at 8 to 10 feet (2.4 m to 3.0 m). Various pipe materials may be selected provided the pipe is corrosion resistant and appropriately bedded to ensure that the underdrains are not damaged by sludge removal equipment.

### **88.234 Additional Dewatering Provisions**

Consideration shall be given for providing a means of decanting the supernatant of sludge placed on the sludge drying beds. More effective decanting of supernatant may be accomplished with polymer treatment of sludge.

### **88.235 Seal**

The bottom shall be sealed in a manner approved by the reviewing authority.

## **88.24 Walls**

Walls should extend 18 inches (460 mm) above and at least 9 inches (230 mm) below the surface of the bed. Outer walls shall be water tight down to the bottom of the bed and extend at least 4 inches (100 mm) above the outside grade elevation to prevent soil from washing into the beds.

## **88.25 Sludge Removal**

Each bed shall be constructed so as to be readily and completely accessible to mechanical equipment for cleaning and sand replacement. Concrete runways spaced to accommodate mechanical equipment shall be provided. Special attention should be given to assure adequate access to the areas adjacent to the sidewalls. Entrance ramps down to the level of the sand bed shall be provided. These ramps should be high enough to eliminate the need for an entrance end wall

for the sludge bed.

### **88.3 Mechanical Dewatering Facilities**

#### **88.31 General**

Provision shall be made to maintain sufficient continuity of service so that sludge may be dewatered without accumulation beyond storage capacity. The number of vacuum filters, centrifuges, filter presses, belt filters, other mechanical dewatering facilities, or combinations thereof should be sufficient to dewater the sludge produced with the largest unit out of service. Unless other standby wet sludge facilities are available, adequate storage facilities of at least 4 days production volume in addition to any other sludge storage needs shall be provided. Documentation must be submitted justifying the basis of design of mechanical dewatering facilities.

#### **88.32 Water Supply Protection**

Provisions for water supply to mechanical dewatering facilities shall be in accordance with Paragraph 56.23.

#### **88.33 Auxiliary Facilities for Vacuum Filters**

Back-up vacuum and filtrate pumps shall be provided. It is permissible to have uninstalled back-up vacuum and filtrate pumps for every three or less vacuum filters, provided that the installed units can easily be removed and replaced. At least one filter media replacement unit shall be provided.

#### **88.34 Ventilation**

Adequate facilities shall be provided for ventilation of the dewatering area in accordance with Paragraph 42.75. The exhaust air should be properly conditioned to avoid odor nuisance.

#### **88.35 Chemical Handling Enclosures**

Lime-mixing facilities should be completely enclosed to prevent the escape of lime dust. Chemical handling equipment should be automated to eliminate the manual lifting requirement. Refer to Section 57.

### **88.4 Drainage and Filtrate Disposal**

Drainage from sludge drying beds or filtrate from other dewatering units shall be returned to the wastewater treatment process at appropriate points and rates. (See also Paragraphs 56.7 and 84.64.)

### **88.5 Other Dewatering Facilities**

If it is proposed to dewater sludge by other methods, a detailed description of the process and design data shall accompany the plans. Refer to Paragraph 53.2 for any new process determinations.

## **89. SLUDGE STORAGE AND DISPOSAL**

### **89.1 Storage**

### **89.11 General**

Sludge storage facilities shall be provided at all mechanical treatment plants. Appropriate storage facilities may consist of any combination of drying beds, lagoons, separate tanks, additional volume in sludge stabilization units, pad areas or other means to store either liquid or dried sludge. Refer to Paragraphs 88.2 and 89.2 for drying bed and lagoon design criteria, respectively.

The design shall provide for odor control in sludge storage tanks and sludge lagoons including aeration, covering, or other appropriate means.

### **89.12 Volume**

Rational calculations justifying the number of days of storage to be provided shall be submitted and shall be based on the total sludge handling and disposal system. Refer to Paragraphs 84.7 and 85.8 for anaerobically and aerobically digested sludge production values. Sludge production values for other stabilization processes should be justified in the basis of design. If the land application method of sludge disposal is the only means of disposal utilized at a treatment plant, storage shall be provided based on considerations including at least the following items:

- a. Inclement weather effects on access to the application land;
- b. Temperatures including frozen ground and stored sludge cake conditions;
- c. Haul road restrictions including spring thawing conditions;
- d. Area seasonal rainfall patterns;
- e. Cropping practices on available land;
- f. Potential for increased sludge volumes from industrial sources during the design life of the plant;
- g. Available area for expanding sludge storage; and
- h. Appropriate pathogen reduction and vector attraction reduction requirements.

A minimum range of 120 to 180 days storage should be provided for the design life of the plant unless a different period is approved by the reviewing authority. Refer to Paragraph 89.33 for other sludge land application considerations.

## **89.2 Sludge Storage Lagoons**

### **89.21 General**

Sludge storage lagoons will be permitted only upon proof that the character of the digested sludge and the design mode of operation are such that offensive odors will not result. Where sludge lagoons are permitted, adequate provisions shall be made for other acceptable sludge handling methods in the event of upset or failure of the sludge digestion process.

### **89.22 Location**

Sludge lagoons shall be located as far as practicable from inhabited areas or areas

likely to be inhabited during the lifetime of the structures. Siting of sludge lagoons shall comply with the requirements of the reviewing authority.

### **89.23 Seal**

Adequate provisions shall be made to seal the sludge lagoon bottoms and embankments in accordance with the requirements of Paragraph 93.422 to prevent leaching into adjacent soils or ground water. The seal shall be protected to prevent damage from sludge removal activities. Groundwater monitoring may be required by the reviewing authority in accordance with Paragraph 93.55.

### **89.24 Access**

Provisions shall be made for pumping or heavy equipment access for sludge removal from the sludge lagoon on a routine basis.

### **89.25 Supernatant Disposal**

Lagoon supernatant shall be returned to the wastewater treatment process at appropriate points and rates. (See also Paragraphs 56.7 and 84.64.)

## **89.3 Disposal**

### **89.31 General**

Drainage facilities for sludge vehicle transfer stations shall be provided to allow any spillage or washdown material to be collected and returned to the wastewater treatment plant or sludge storage facility.

### **89.32 Sanitary Landfilling**

Sludge and sludge residues may be disposed of in approved sanitary landfills under the terms and conditions of the regulatory agency.

### **89.33 Land Application**

The reviewing authority should be contacted for specific design and approval requirements governing land application of municipal sludges. Additional operating criteria may be obtained from applicable federal regulations. Sludge may be utilized as a soil conditioner for agricultural, horticultural, or reclamation purposes. Important design considerations include but are not necessarily limited to: sludge stabilization process, appropriate pathogen and vector attraction reduction, sludge characteristics including the presence of inorganic and organic chemicals, application site characteristics (soils, groundwater elevations, setback distance requirements, etc.), local topography and hydrology, cropping practices, spreading and incorporation techniques, population density and odor control, local groundwater quality and usage.

Sludge mixing equipment or other provisions to assist in the monitoring of land applied sludge should be considered in the design of sludge handling and storage facilities.

Due to inclement weather and cropping practices, alternative sludge disposal options are recommended to ensure the sludge is properly managed.

Sludge should not be applied to land which is used for growing food crops to be

eaten raw, such as leafed vegetables and root crops.

#### **89.34 Sludge Lagoons for Disposal**

The utilization of lagoons for ultimate disposal of sludge is not recommended due to odor potential, area and volume required, and possible long term problems from groundwater contamination. The regulatory agency must be contacted for the acceptability of lagoons for final disposal.

#### **89.35 Other Disposal Methods**

If it is proposed to dispose of sludge by other methods, a detailed description of the technique and design data shall accompany the plans. Refer to Paragraph 53.2 for any new process determinations.

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## **CHAPTER 90 BIOLOGICAL TREATMENT**

### **91. TRICKLING FILTERS**

#### **91.1 General**

Trickling filters may be used for treatment of wastewater amenable to treatment by aerobic biological processes. Trickling filters shall be preceded by effective settling tanks equipped with scum and grease collecting devices, or other suitable pretreatment facilities.

Filters shall be designed to provide for reduction in carbonaceous and/or nitrogenous oxygen demand in accordance with water quality standards and objectives for the receiving waters as established by the appropriate reviewing authority, or to properly condition the wastewater for subsequent treatment processes. Multi-stage filters should be considered if needed to meet more stringent effluent standards.

#### **91.2 Hydraulics**

##### **91.21 Distribution**

###### **91.211 Uniformity**

The wastewater may be distributed over the filter by rotary distributors or other suitable devices which will ensure uniform distribution to the surface area. At design average flow, the deviation from a calculated uniformly distributed volume per square foot of the filter surface shall not exceed plus or minus 10 percent at any point. All hydraulic factors involving proper distribution of wastewater on the filters shall be carefully calculated. Such calculations shall be submitted to the appropriate reviewing authority.

For rotary distributors reverse reaction nozzles, hydraulic brakes or motor-driven distributor arms shall be provided to not exceed the maximum speed recommended by the distributor manufacturer and to attain the desired media flushing rate.

###### **91.212 Head Requirements**

For reaction type distributors, a minimum head of 24 inches (610 mm) between low water level in the siphon chamber and center of the arms is required. Similar allowance in design shall be provided for added pumping head requirements where pumping to the reaction type distributor is used.

###### **91.213 Clearance**

A minimum clearance of 12 inches (300 mm) between media and distribution arms shall be provided.

#### **91.22 Dosing**

Wastewater may be applied to the filters by siphons, pumps or by gravity discharge from preceding treatment units when suitable flow characteristics have been developed. Application of the wastewater shall be practically continuous.

The piping system shall be designed for recirculation.

### **91.23 Piping System**

The piping system, including dosing equipment and distributor, shall be designed to provide capacity for the design peak hourly flow, including recirculation required under Paragraph 91.55.

## **91.3 Media**

### **91.31 Quality**

The media may be crushed rock, slag, or manufactured material. The media shall be durable, resistant to spalling or flaking and relatively insoluble in wastewater. The top 18 inches (460 mm) shall have a loss by the 20-cycle, sodium sulfate soundness test of not more than 10 percent, as prescribed by ASCE Manual of Engineering Practice, Number 13. The balance is to pass a 10-cycle test using the same criteria. Slag media shall be free from iron or other leachable materials that will adversely affect the process or effluent quality. Manufactured media shall be resistant to ultraviolet degradation, disintegration, erosion, aging, all common acids and alkalies, organic compounds, and fungus and biological attack. Such media shall be structurally capable of supporting a person's weight or a suitable access walkway shall be provided to allow for distributor maintenance.

### **91.32 Depth**

Trickling filter media shall have a minimum depth of 6 feet (1.8 m) above the underdrains. Rock and/or slag filter media depths shall not exceed 10 feet (3 m) and manufactured filter media depths should not exceed the recommendations of the manufacturer. Forced ventilation should be considered in accordance with Paragraph 91.43.

### **91.33 Size, Grading, and Handling of Media**

#### **91.331 Rock, Slag, and Similar Media**

Rock, slag, and similar media shall not contain more than 5 percent by weight of pieces whose longest dimension is three times the least dimension. They shall be free from thin, elongated and flat pieces, dust, clay, sand or fine material and shall conform to the following size and grading when mechanically graded over a vibrating screen with square openings.

Passing 4½ inch (112 mm) screen - 100% by weight  
Retained on 3 inch (75 mm) screen - 95-100% by weight  
Passing 2 inch (50 mm) screen - 0-2% by weight  
Passing 1 inch (25 mm) screen - 0-1% by weight

#### **91.332 Manufactured Media**

Suitability will be evaluated on the basis of experience with installations handling similar wastes and loadings. To ensure sufficient void clearances, media with specific surface areas of no more than 30 square feet per cubic foot ( $100 \text{ m}^2/\text{m}^3$ ) are acceptable for filters employed for carbonaceous reduction, and 45 square feet per cubic foot ( $150 \text{ m}^2/\text{m}^3$ ) for second stage ammonia reduction.

### **91.333 Handling and Placing of Media**

Material delivered to the filter site shall be stored on wood-planked or other approved clean, hard-surfaced areas. All material shall be rehandled at the filter site and no material shall be dumped directly into the filter. Crushed rock, slag, and similar media shall be washed and rescreened or forked at the filter site to remove all fines. Such material shall be placed by hand to a depth of 12 inches (300 mm) above the tile underdrains. The remainder of the material may be placed by means of belt conveyors or equally effective methods approved by the engineer. All material shall be carefully placed so as not to damage the underdrains. Manufactured media shall be handled and placed as approved by the engineer. Trucks, tractors, and other heavy equipment shall not be driven over the filter during or after construction.

## **91.4 Underdrainage System**

### **91.41 Arrangement**

Underdrains with semicircular inverts or equivalent should be provided and the underdrainage system shall cover the entire floor of the filter. Inlet openings into the underdrains shall have an unsubmerged gross combined area equal to at least 15 percent of the surface area of the filter.

### **91.42 Hydraulic Capacity**

The underdrains shall have a minimum slope of 1 percent. Effluent channels shall be designed to produce a minimum velocity of 2 feet per second (0.6 m/s) at design average flow rates of application to the filter including recirculated flows. Refer to Paragraph 91.43.

### **91.43 Ventilation**

The underdrainage system, effluent channels, and effluent pipe shall be designed to permit free passage of air. The size of drains, channels, and pipe should be such that not more than 50 percent of their cross-sectional area will be submerged under the design peak instantaneous flow, including proposed or possible future recirculated flows.

Forced ventilation should be provided for covered trickling filters to ensure adequate oxygen for process requirements. Windows or simple louvered mechanisms so arranged to ensure air distribution throughout the enclosure shall be provided. The design of the ventilation facilities shall provide for operator control of air flow in accordance with outside seasonal temperature. Design computations showing the adequacy of air flow to satisfy process oxygen requirements shall be submitted.

### **91.44 Flushing**

Provision should be made for flushing the underdrains unless high rate recirculation is utilized. In small rock and slag filters, use of a peripheral head channel with vertical vents is acceptable for flushing purposes. Inspection facilities should be provided.

## **91.5 Special Features**

**91.51 Flooding**

Appropriate valves, sluice gates, or other structures shall be provided to enable flooding of filters comprised of rock or slag media for filter fly control.

**91.52 Freeboard**

A freeboard of 4 feet (1.2 m) or more should be provided for tall, manufactured filters to contain windblown spray. Provide at least 6 foot (1.8 m) headroom for maintenance of the distributor on covered filters.

**91.53 Maintenance**

All distribution devices, underdrains, channels, and pipes shall be installed so that they may be properly maintained, flushed or drained.

**91.54 Winter Protection**

Covers shall be provided to maintain operation and treatment efficiencies when climatic conditions are expected to result in problems due to cold temperatures.

**91.55 Recirculation**

The piping system shall be designed for recirculation as required to achieve the design efficiency. The recirculation rate shall be variable and subject to plant operator control at the range of 0.5:1 up to 4:1 (ratio of recirculation rate versus design average flow). A minimum of two recirculation pumps shall be provided.

**91.56 Recirculation Measurement**

Devices shall be provided to permit measurement of the recirculation rate. Elapsed time meters and pump head recording devices are acceptable for facilities treating less than 1 mgd (3785 m<sup>3</sup>/d). The design of the recirculation facilities shall provide for both continuity of service and the range of recirculation ratios. Reduced recirculation rates for periods of brief pump outages may be acceptable depending on water quality requirements.

**91.57 Ventilation Ports**

The underdrainage ventilation ports shall be designed to ensure that the interior flow will be retained inside the trickling filter.

**91.6 Rotary Distributor Seals**

Mercury seals shall not be permitted. Ease of seal replacement shall be considered in the design to ensure continuity of operation.

**91.7 Unit Sizing**

Required volumes of filter media shall be based upon pilot testing with the particular wastewater or any of the various empirical design equations that have been verified through actual full scale experience. Such calculations must be submitted if pilot testing is not utilized. Pilot testing is recommended to verify performance predictions based upon the various design equations, particularly when significant amounts of industrial wastes are present.

Trickling filter design shall consider peak organic load conditions including the oxygen demands due to recycle flows (i.e., heat treatment supernatant, vacuum filtrate, anaerobic digester supernatant, etc.) due to high concentrations of BOD<sub>5</sub> and TKN associated with such flows. The volume of media determined from either pilot plant studies or use of acceptable design equations shall be based upon the design maximum day BOD<sub>5</sub> organic loading rate rather than the design average BOD<sub>5</sub> rate. Refer to Paragraph 11.251.

## **92. ACTIVATED SLUDGE**

### **92.1 General**

#### **92.11 Applicability**

##### **92.111 Biodegradable Wastes**

The activated sludge process and its various modifications may be used where wastewater is amenable to biological treatment.

##### **92.112 Operational Requirement**

This process requires close attention and competent operating supervision, including routine laboratory control. These requirements shall be considered when proposing this type of treatment.

##### **92.113 Energy Requirements**

This process requires major energy usage to meet aeration demands. Energy costs and potential mandatory emergency public power reduction events in relation to critical water quality conditions must be carefully evaluated. Capability of energy usage phasedown while still maintaining process viability, both under normal and emergency energy availability conditions, must be included in the activated sludge design.

#### **92.12 Specific Process Selection**

The activated sludge process and its several modifications may be employed to accomplish varied degrees of removal of suspended solids and reduction of carbonaceous and/or nitrogenous oxygen demand. Choice of the process most applicable will be influenced by the degree and consistency of treatment required, type of waste to be treated, proposed plant size, anticipated degree of operation and maintenance, and operating and capital costs. All designs shall provide for flexibility in operation and should provide for operation in various modes, if feasible.

#### **92.13 Winter Protection**

In severe climates, protection against freezing shall be provided to ensure continuity of operation and performance. Insulation of the tanks by earthen banks should be considered.

### **92.2 Pretreatment**

Where primary settling tanks are not used, effective removal or exclusion of grit, debris, excessive oil or grease, and screening of solids shall be accomplished prior to the activated sludge process. Screening devices with clear openings of 1/4 inch (6 mm) or

less shall be provided.

Where primary settling is used, provision shall be made for discharging raw wastewater directly to the aeration tanks to facilitate plant start-up and operation during the initial stages of the plant's design life.

## 92.3 Aeration

### 92.31 Capacities and Permissible Loadings

The size of the aeration tank for any particular adaptation of the process shall be determined by full scale experience, pilot plant studies, or rational calculations based mainly on solids retention time, food to microorganism ratio and mixed liquor suspended solids levels. Other factors, such as size of treatment plant, diurnal load variations, and degree of treatment required, shall also be considered. In addition, temperature, alkalinity, pH, and reactor dissolved oxygen shall be considered when designing for nitrification.

Calculations should be submitted to justify the basis for design of aeration tank capacity. Calculations using values differing substantially from those in the accompanying table should reference actual operational plants. Mixed liquor suspended solids levels greater than 5000 mg/L may be allowed providing adequate data is submitted showing the aeration and clarification system capable of supporting such levels.

When process design calculations are not submitted, the aeration tank capacities and permissible loadings for the several adaptations of the processes shown in the following table shall be used. These values apply to plants receiving diurnal load ratios of design peak hourly BOD<sub>5</sub> to design average BOD<sub>5</sub> ranging from about 2:1 to 4:1. Thus, the utilization of flow equalization facilities to reduce the diurnal design peak hourly BOD<sub>5</sub> organic load may be considered by the appropriate reviewing authority as justification to approve organic loading rates that exceed those specified in the table.

PERMISSIBLE AERATION TANK CAPACITIES AND LOADINGS

Process	*Aeration Tank Organic Loading lb BOD <sub>5</sub> /d/1000 ft <sup>3</sup> [kg BOD <sub>5</sub> / (m <sup>3</sup> ·d)]**	F/M Ratio lb BOD <sub>5</sub> /d/lb MLVSS** [kg BOD <sub>5</sub> /(kg MLVSS·d)]	MLSS**** mg/L
Conventional Step Aeration Complete Mix	40 (0.64)	0.2-0.5	1000-3000
Contact Stabilization	50*** (0.80)	0.2-0.6	1000-3000
Extended Aeration Single Stage Nitrification	15 (0.24)	0.05-0.1	3000-5000

\* Volumetric loadings are based on the organic load influent to the aeration tank at plant design average BOD<sub>5</sub>.

\*\* Refer to 11.251(a) for definition of BOD.

\*\*\* Total aeration capacity, includes both contact and reaeration capacities. Normally the contact zone equals 30 to 35% of the total aeration capacity.

\*\*\*\* MLSS values are dependent upon the surface area provided for sedimentation and the rate of sludge return as well as the aeration process.

### **92.32 Arrangement of Aeration Tanks**

#### **a. Dimensions**

The dimensions of each independent mixed liquor aeration tank or return sludge reaeration tank shall be such as to maintain effective mixing and utilization of air. Ordinarily, liquid depths should not be less than 10 feet (3 m) or more than 30 feet (9 m) except in special design cases. An exception is that horizontally mixed aeration tanks shall have a depth of not less than 5.5 feet (1.7 m).

#### **b. Short-circuiting**

For very small tanks or tanks with special configuration, the shape of the tank, the location of the influent and sludge return, and the installation of aeration equipment should provide for positive control to prevent short-circuiting through the tank.

### **92.321 Number of Units**

Total aeration tank volume shall be divided among two or more units, capable of independent operation, when required by the appropriate reviewing authority to meet applicable effluent limitations and reliability guidelines.

### **92.322 Inlets and Outlets**

#### **a. Controls**

Inlets and outlets for each aeration tank unit shall be suitably equipped with valves, gates, stop plates, weirs, or other devices to permit controlling the flow to any unit and to maintain reasonably constant liquid level. The effluent weir for a horizontally mixed aeration tank system must be easily adjustable by mechanical means and shall be sized based on the design peak instantaneous flow plus the maximum return sludge flow. Refer to Paragraph 92.41. The hydraulic properties of the system shall permit the design peak instantaneous flow to be carried with any single aeration tank unit out of service.

#### **b. Conduits**

Channels and pipes carrying liquids with solids in suspension shall be designed to maintain self-cleansing velocities or shall be agitated to keep such solids in suspension at all rates of flow within the design limits. Adequate provisions should be made to drain segments of channels which are not being used due to alternate flow patterns.

### **92.323 Freeboard**

All aeration tanks should have a freeboard of not less than 18 inches

(460 mm). However, if a mechanical surface aerator is used, the freeboard should be not less than 3 feet (0.9 m) to protect against windblown spray freezing on walkways, etc.

## **92.33 Aeration Equipment**

### **92.331 General**

Oxygen requirements generally depend on maximum diurnal organic loading (design peak hourly BOD<sub>5</sub> as described in Paragraph 11.25), degree of treatment, and level of suspended solids concentration to be maintained in the aeration tank mixed liquor. Aeration equipment shall be capable of maintaining a minimum of 2.0 mg/L of dissolved oxygen in the mixed liquor at all times and provide thorough mixing of the mixed liquor. In the absence of experimentally determined values, the design oxygen requirements for all activated sludge processes shall be 1.1 lb O<sub>2</sub>/lb design peak hourly BOD<sub>5</sub> (1.1 kg O<sub>2</sub>/kg design peak hourly BOD<sub>5</sub>) applied to the aeration tanks, with the exception of the extended aeration process, for which the value shall be 1.5 to include endogenous respiration requirements.

Where nitrification is required or will occur, such as within the extended aeration process, the oxygen requirement for oxidizing ammonia must be added to the above requirement for carbonaceous BOD<sub>5</sub> removal and endogenous respiration requirements. The nitrogenous oxygen demand (NOD) shall be taken as 4.6 times the diurnal peak hourly TKN content of the influent. In addition, the oxygen demands due to recycle flows (i.e., heat treatment supernatant, vacuum filtrate, elutriates, etc.) must be considered due to the high concentrations of BOD<sub>5</sub> and TKN associated with such flows.

Careful consideration should be given to maximizing oxygen utilization per unit of power input. Unless flow equalization is provided, the aeration system should be designed to match the diurnal organic load variation while economizing on power input. Refer to Paragraph 92.31.

### **92.332 Diffused Air Systems**

The design of the diffused air system to provide the oxygen requirements shall be done by either of the two methods described below in (a) and (b), augmented as required by consideration of items (c) through (h):

- a. Having determined the oxygen requirements per Paragraph 92.331, air requirements for a diffused air system shall be determined by use of any of the well known equations incorporating such factors as:
  1. Tank depth;
  2. Alpha factor of waste;
  3. Beta factor of waste;
  4. Certified aeration device transfer efficiency;
  5. Minimum aeration tank dissolved oxygen concentration;
  6. Critical wastewater temperature; and
  7. Altitude of plant.

In the absence of experimentally determined alpha and beta factors, wastewater transfer efficiency shall be assumed to be not greater than 50 percent of clean water efficiency for plants treating primarily (90% or greater) domestic wastewater. Treatment plants where the waste contains higher percentages of industrial wastes shall use a correspondingly lower percentage of clean water efficiency and shall have calculations submitted to justify such a percentage. The design transfer efficiency should be included in the specifications.

- b. Normal air requirements for all activated sludge processes except extended aeration (assuming equipment capable of transmitting to the mixed liquor the amount of oxygen required in Paragraph 92.331) shall be considered to be 1500 cubic feet at standard conditions of pressure, temperature, and humidity per pound of BOD<sub>5</sub> tank loading (94 m<sup>3</sup>/kg BOD<sub>5</sub>). For the extended aeration process the value shall be 2050 cubic feet per pound of BOD<sub>5</sub> (128 m<sup>3</sup>/kg of BOD<sub>5</sub>).
- c. To the air requirements calculated above shall be added air required for channels, pumps, aerobic digesters, filtrate, and supernatant or other air-use demand.
- d. The specified capacity of blowers or air compressors, particularly centrifugal blowers, should take into account that the air intake temperature may reach 115°F (46 °C) or higher and the pressure may be less than normal. The specified capacity of the motor drive should also take into account that the intake air may be -20°F (-29 °C) or less and may require oversizing of the motor or a means of reducing the rate of air delivery to prevent overheating or damage to the motor.
- e. The blowers shall be provided in multiple units, so arranged and in such capacities as to meet the maximum air demand with the single largest unit out of service. The design shall also provide for varying the volume of air delivered in proportion to the load demand of the plant. Aeration equipment shall be easily adjustable in increments and shall maintain solids suspension within these limits.
- f. Diffuser systems shall be capable of providing for 200 percent of the designed average day oxygen demand. The air diffusion piping and diffuser system shall be capable of delivering normal air requirements with minimal friction losses.

Air piping systems should be designed such that total head loss from blower outlet (or silencer outlet where used) to the diffuser inlet does not exceed 0.5 psi (3.4 kPa) at average operating conditions.

The spacing of diffusers should be in accordance with the oxygen requirements through the length of the channel or tank, and should be designed to facilitate adjustment of their spacing without major revisions to air header piping.

All plants employing less than four independent aeration tanks

shall be designed to incorporate removable diffusers that can be serviced and/or replaced without dewatering the tank.

- g. Individual assembly units of diffusers shall be equipped with control valves, preferably with indicator markings, for throttling or for complete shutoff. Diffusers in any single assembly shall have substantially uniform pressure loss.
- h. Air filters shall be provided in numbers, arrangements, and capacities to furnish at all times an air supply sufficiently free from dust to prevent damage to blowers and clogging of the diffuser system used.

### **92.333 Mechanical Aeration Systems**

- a. Oxygen Transfer Performance

The mechanism and drive unit shall be designed for the expected conditions in the aeration tank in terms of the power performance. Certified testing shall be provided to verify mechanical aerator performance. Refer to applicable provisions of Paragraph 92.332. In the absence of specific design information, the oxygen requirements shall be calculated using a transfer rate not to exceed 2 pounds of oxygen per horsepower per hour [1.22 kg O<sub>2</sub>/(kW·h)] in clean water under standard test conditions. Design transfer efficiencies shall be included in the specifications.

- b. Design Requirements

The design requirements of a mechanical aeration system shall accomplish the following:

1. Maintain a minimum of 2.0 mg/L of dissolved oxygen in the mixed liquor at all times throughout the tank or basin;
2. Maintain all biological solids in suspension (for a horizontally mixed aeration tank system an average velocity of 1 foot per second (0.3 m/s) must be maintained);
3. Meet maximum oxygen demand and maintain process performance with the largest unit out of service;
4. Provide for varying the amount of oxygen transferred in proportion to the load demand on the plant; and
5. Provide that motors, gear housing, bearings, grease fittings, etc., be easily accessible and protected from inundation and spray as necessary for proper functioning of the unit.

- c. Winter Protection

Where extended cold weather conditions occur, the aerator mechanism and associated structure shall be protected from freezing due to splashing. Due to high heat loss, subsequent treatment units shall be protected from freezing.

## 92.4 Return Sludge Equipment

### 92.41 Return Sludge Rate

The minimum permissible return sludge rate of withdrawal from the final settling tank is a function of the concentration of suspended solids in the mixed liquor entering it, the sludge volume index of these solids, and the length of time these solids are retained in the settling tank. Since undue retention of solids in the final settling tanks may be deleterious to both the aeration and sedimentation phases of the activated sludge process, the rate of sludge return expressed as a percentage of the design average flow of wastewater should generally be variable between the limits set forth as follows:

Type of Process	% Design Average Flow	
	Minimum	Maximum
Conventional, Step Aeration or Complete Mix	15	100
Contact Stabilization	50	150
Single Stage Nitrification	50	150
Extended Aeration	50	150
Carbonaceous Stage of Separate Stage Nitrification	15	100
Nitrification Stage of Separate Stage Nitrification	50	200

The rate of sludge return shall be varied by means of variable speed motors, drives, or timers (small plants) to pump sludge at the above rates. All designs shall provide for flexibility in operation and should provide for operation in various process modes, if feasible.

### 92.42 Return Sludge Pumps

If motor drive return sludge pumps are used, the maximum return sludge capacity shall be obtained with the largest pump out of service. A positive head should be provided on pump suctions. Pumps should have at least 3 inch (80 mm) suction and discharge openings.

If air lifts are used for returning sludge from each settling tank hopper, no standby unit will be required provided the design of the air lifts facilitate their rapid and easy cleaning and provided other suitable standby measures are provided. Air lifts should be at least 3 inches (80 mm) in diameter.

### 92.43 Return Sludge Piping

Discharge piping should be at least 4 inches (100 mm) in diameter and should be

designed to maintain a velocity of not less than 2 feet per second (0.6 m/s) when return sludge facilities are operating at normal return sludge rates. Suitable devices for observing, sampling, and controlling return activated sludge flow from each settling tank hopper shall be provided, as outlined in Paragraph 73.24.

#### **92.44 Waste Sludge Facilities**

Waste sludge control facilities should have a capacity of at least 25 percent of the design average rate of wastewater flow and function satisfactorily at rates of 0.5 percent of design average wastewater flow or a minimum of 10 gallons per minute (0.6 L/s), whichever is larger. Means for observing, measuring, sampling, and controlling waste activated sludge flow shall be provided. Waste sludge may be discharged to the primary settling tank, sludge digestion tank, sludge thickening or dewatering processes, storage tank or any practical combination of these units.

#### **92.5 Measuring Devices**

Devices should be installed in all plants for indicating flow rates of raw wastewater or primary effluent, return sludge, and air to each tank unit. For plants designed for design average wastewater flows of 1 mgd (3785 m<sup>3</sup>/d) or more, these devices should totalize and record, as well as indicate flows. Where the design provides for all return sludge to be mixed with the raw wastewater (or primary effluent) at one location, then the mixed liquor flow rate to each aeration unit should be measured.

#### **92.6 Sequencing Batch Reactors**

The fill and draw mode of the activated sludge process commonly termed the Sequencing Batch Reactor may be approved at the discretion of the reviewing authority on a case by case basis under the provisions of Paragraph 53.2. The design must be based on experience at other facilities and shall meet the applicable requirements under Chapters 50, 70 and 90, except as modified in this Paragraph. Continuity and reliability of treatment equal to that of the continuous flow through modes of the activated sludge process shall be provided. Supplemental treatment units may be required to meet applicable effluent limitations and reliability guidelines. The reviewing authority should be contacted for design guidance and criteria where such systems are being considered. See also Section 65 where in-line flow equalization units are provided in addition to the decantable volume.

- a. Design F/M ratios in the range of 0.05 to 0.1 are permissible. The aeration tank volumetric loading should not exceed 15 lb BOD<sub>5</sub>/d/1000 ft<sup>3</sup> [0.24 kg BOD<sub>5</sub>/(m<sup>3</sup>·d)]. The reactor MLVSS and MLSS concentrations and aeration tank volumetric loading should be calculated at the low-water level.
- b. More than two tanks should be provided.
- c. The decantable volume and decanter capacity of the sequencing batch reactor system with the largest basin out of service should be sized to pass at least 75 percent of the design maximum day flow without changing cycle times. A decantable volume of at least 4 hours with the largest basin out of service based on 100 percent of the design maximum day flow is permissible.
- d. System reliability with any single aeration tank unit out of service and the instantaneous delivery of flow shall be evaluated in the design of decanter weirs and approach velocities. The treated effluent from each reactor should be free of scum

- and have a suspended solids concentration no greater than 30 mg/L at any time. See Paragraphs 53.413 and 72.43. Scum removal shall be provided. An adequate zone of separation between the sludge blanket and the decanter(s) shall be maintained throughout the decant phase.
- e. Decanters which draw the treated effluent from near the water surface throughout the decant phase are recommended.
  - f. Solids management to accommodate basin dewatering shall be considered.
  - g. The blowers shall be provided in multiple units, so arranged and in such capacities as to meet the maximum air demand in the oxic portions of the fill/react and react phases of the cycle with the single largest unit out of service. See Paragraph 92.332(e).
  - h. Mechanical mixing independent of aeration shall be provided for all systems where biological phosphorus removal or denitrification is required. The mixing equipment should be sized to thoroughly mix the entire basin from a settled condition within 5 minutes without aeration.
  - i. The design effluent quality performance requirements for the plant should be sufficiently stringent to ensure acceptable effluent quality from any reactor. Flow paced composite sampling equipment and continuous turbidity metering for separately monitoring the effluent quality from each basin may be required by the regulatory agency. All 24-hour effluent quality composite samples for compliance reporting or monitoring plant operations shall be flow-paced and include samples collected at the beginning and end of each decant phase. A programmable logic controller (PLC) shall be provided. Multiple PLCs should be provided as necessary to assure rapid process recovery or minimize the deterioration of effluent quality from the failure of a single controller. An uninterruptible power supply with electrical surge protection shall be provided for each PLC to retain program memory (i.e., process control program, last-known set points and measured process/equipment status, etc.) through a power loss. A hard-wired backup for manual override shall be provided in addition to automatic process control. Both automatic and manual controls shall allow independent operation of each tank. In addition, a fail-safe control shall be provided which cannot be adjusted by the operator allowing at least 20 minutes of settling between the react and decant phases.

## **93. WASTEWATER TREATMENT PONDS**

### **93.1 General**

This Section deals with generally used variations of treatment ponds capable of achieving secondary treatment including controlled-discharge pond systems, flow-through pond systems and aerated pond systems. Ponds utilized for equalization, percolation, evaporation, and sludge storage are not discussed in this Section.

### **93.2 Location**

#### **93.21 Surface Runoff**

Adequate provision must be made to divert stormwater runoff around the ponds and protect pond embankments from erosion.

**93.22 Ground Water Separation**

A minimum separation of 4 feet (1.2 m) between the bottom of the pond and the maximum ground water elevation should be maintained.

**93.23 Bedrock Separation**

A minimum separation of 10 feet (3.0 m) between the pond bottom and any bedrock formation is recommended.

**93.3 Basis of Design****93.31 Area and Loadings for Controlled-Discharge Facultative Treatment Pond Systems**

Pond design for design average BOD<sub>5</sub> loading may range from 15 to 35 pounds per acre per day [17 kg/(ha·d) to 40 kg/(ha·d)] at the mean operating depth in the primary cells and at least 180 days detention time between the 2 foot (0.6 m) and the maximum operating depth of the entire pond system. Refer to Paragraph 11.251. The detention time and organic loading rate shall depend on climatic conditions and effluent discharge limits.

**93.32 Area and Loadings for Flow-Through Facultative Treatment Ponds Systems**

Pond design for design average BOD<sub>5</sub> loading may vary from 15 to 35 pounds per acre per day [17 kg/(ha·d) to 40 kg/(ha·d)] for the primary pond(s). Refer to Paragraph 11.251. The major design considerations for BOD<sub>5</sub> loading must be directly related to the climatic conditions.

Design variables such as pond depth, multiple units, detention time, and additional treatment units must be considered with respect to applicable standards for BOD<sub>5</sub>, total suspended solids (TSS), fecal coliform, dissolved oxygen (DO) and pH.

A detention time of 90 to 120 days should be provided; however, this must be properly related to other design considerations. It should be noted that the major factor in the design is the duration of the cold weather period (water temperature less than 5°C).

**93.33 Aerated Treatment Pond Systems**

For the development of final design parameters, it is recommended that actual experimental data be developed; however, the aerated treatment pond system design for minimum detention time may be estimated using the following formula applied separately to each aerated cell:

$$t = E / 2.3k_1 \times (100 - E)$$

t = detention time, days

E = percent of BOD<sub>5</sub> to be removed in an aerated pond

k<sub>1</sub> = reaction coefficient, aerated lagoon, base 10. For normal domestic wastewater, the k<sub>1</sub> value may be assumed to be 0.12/day at 68°F (20 °C) and 0.06/day at 34°F (1 °C).

The reaction rate coefficient for domestic wastewater which includes some industrial wastes, other wastes, and partially treated wastewater must be determined experimentally for various conditions which might be encountered in the aerated ponds. Conversion of the reaction rate coefficient at other temperatures shall be made based on experimental data.

Raw wastewater strength should also consider the effect of any return sludge. Also, additional storage volume should be considered for sludge, and in northern climates, ice cover.

Oxygen requirements generally will depend on the design average BOD<sub>5</sub> loading, the degree of treatment, and the concentration of suspended solids to be maintained. Aeration equipment shall be capable of maintaining a minimum dissolved oxygen level of 2 mg/L in the ponds at all times. Suitable protection from weather shall be provided for electrical controls. Aerated cells shall be followed by a polishing cell with a volume of at least 0.3 of the total volume of the aerated cells.

See Paragraph 92.33 for details on aeration equipment.

### **93.34 Industrial Wastes**

Consideration shall be given to the type and effects of industrial wastes on the treatment process. In some cases it may be necessary to pretreat industrial or other discharges.

Industrial wastes shall not be discharged to ponds without assessment of the effects such substances may have upon the treatment process or discharge requirements in accordance with state and federal laws.

### **93.35 Number of Cells Required**

At a minimum, a wastewater treatment pond system should consist of three cells designed to facilitate both series and parallel operations. The maximum size of a pond cell should be 40 acres (16 ha). Two-cell systems may be utilized in very small installations.

All systems should be designed with piping flexibility to permit isolation of any cell without affecting the transfer and discharge capabilities of the total system. In addition, the ability to discharge the influent waste load to a minimum of two cells and/or all primary cells in the system should be provided.

#### **93.351 Controlled-Discharge Facultative Treatment Pond Systems**

For controlled-discharge systems the area specified as the primary ponds should be equally divided into two cells. The third or secondary cell volume should as a minimum, be equal to the volume of each of the primary cells.

In addition, design should permit for adequate elevation difference between primary and secondary ponds to permit gravity filling of the secondary from the primary. Where this is not feasible, pumping facilities shall be provided.

#### **93.352 Flow-Through Facultative Treatment Pond Systems**

At a minimum, primary cells shall provide adequate detention time to maximize BOD<sub>5</sub> removal. Secondary cells should then be provided for additional detention time with depths to 8 feet (2.4 m) to facilitate solids reduction. Design should also consider recirculation within the system.

### **93.353 Aerated Treatment Pond Systems**

A minimum of two aerated cells, plus a polishing cell is required. A tapered mode of aeration is recommended.

### **93.36 Pond Shape**

The shape of all cells should be such that there are no narrow or elongated portions. Round, square or rectangular ponds (length not exceeding three times the width) are considered most desirable. No islands, peninsulas or coves shall be permitted. Dikes should be rounded at corners to minimize accumulations of floating materials. Common-wall dike construction, wherever possible, is strongly encouraged.

## **93.4 Pond Construction Details**

### **93.41 Embankments and Dikes**

#### **93.411 Material**

Dikes shall be constructed of relatively impervious soil and compacted to at least 95 percent Standard Proctor Density to form a stable structure. Vegetation and other unsuitable materials shall be removed from the area where the embankment is to be placed.

#### **93.412 Top Width**

The minimum dike width shall be 8 feet (2.4 m) to permit access for maintenance vehicles.

#### **93.413 Maximum Slopes**

Inner and outer dike slopes shall not be steeper than 1 vertical to 3 horizontal (1:3).

#### **93.414 Minimum Slopes**

Inner slopes should not be flatter than 1 vertical to 4 horizontal (1:4). Flatter slopes can be specified for larger installations because of wave action but have the disadvantage of added shallow areas being conducive to emergent vegetation. Outer slopes shall be sufficient to prevent surface runoff from entering the ponds.

#### **93.415 Freeboard**

Minimum freeboard shall be 3 feet (0.9 m), except that for small systems 2 feet (0.6 m) may be acceptable.

#### **93.416 Design Depth**

The minimum operating depth should be sufficient to prevent growth of

aquatic plants and damage to the dikes, bottom, control structures, aeration equipment, and other appurtenances. In no case should pond depths be less than 2 feet (0.6 m).

a. **Controlled-Discharge and Flow-Through Facultative Treatment Pond Systems**

The maximum water depth shall be 6 feet (1.8 m) in primary cells. Greater depths in subsequent cells are permissible although supplemental aeration or mixing may be necessary.

b. **Aerated Treatment Pond Systems**

The design water depth should be 10 to 15 feet (3.0 m to 4.6 m). This depth limitation may be altered depending on the aeration equipment, waste strength, and climatic conditions.

### **93.417 Erosion Control**

A justification and detailed discussion of the method of erosion control which encompasses all relative factors such as pond location and size, seal material, topography, prevailing winds, cost breakdown, application procedures, etc., shall be provided.

a. **Seeding**

The dikes shall have a covered layer of at least 4 inches (100 mm), of fertile topsoil to promote establishment of an adequate vegetative cover wherever riprap is not utilized. Prior to prefilling (in accordance with Paragraph 93.424), adequate vegetation shall be established on dikes from the outside toe to 2 feet (0.6 m) above the pond bottom on the interior as measured on the slope. Perennial-type, low-growing, spreading grasses that minimize erosion and can be mowed are most satisfactory for seeding on dikes. In general, alfalfa and other long-rooted crops should not be used for seeding since the roots of this type are apt to impair the water-holding efficiency of the dikes.

b. **Additional Erosion Protection**

Riprap or some other acceptable method of erosion control is required as a minimum around all piping entrances and exits. For aerated cells the design should ensure erosion protection on the slopes and bottoms in the areas where turbulence will occur. Additional erosion control may also be necessary on the exterior dike slope to protect the embankment from erosion due to severe flooding of a watercourse.

c. **Alternate Erosion Protection.**

Alternate erosion control on the interior dikes slopes may be necessary for ponds which are subject to severe wave action. In these cases riprap, or an acceptable equal, shall be placed from at least 1 foot (0.3 m) above the high water mark to 2 feet (0.6 m) below the low water mark (measured on the vertical).

**93.42 Pond Bottom****93.421 Soil**

Soil used in constructing the pond bottom (not including the seal) and dike cores shall be relatively incompressible and tight and compacted at or up to 4 percent above the optimum water content to at least 95 percent Standard Proctor Density.

**93.422 Seal**

Ponds shall be sealed such that seepage loss through the seal is as low as practicably possible. Seals consisting of soils, bentonite, or synthetic liners may be considered provided the permeability, durability, and integrity of the proposed material can be satisfactorily demonstrated for anticipated conditions. Results of a testing program which substantiates the adequacy of the proposed seal must be incorporated into and/or accompany the engineering report. Standard ASTM procedures or acceptable similar methods shall be used for all tests.

To achieve an adequate seal in systems using soil, bentonite, or other seal materials, the hydraulic conductivity ( $k$ ) in centimeters per second specified for the seal shall not exceed the value derived from the following expression where  $L$  equals the thickness of the seal in centimeters.

$$k = 2.6 \times 10^{-9}L$$

The " $k$ " obtained by the above expression corresponds to a percolation rate of pond water of less than 500 gallons per day per acre [ $4.7 \text{ m}^3/(\text{ha}\cdot\text{d})$ ] at a water depth of 6 feet (1.8 m) and a liner thickness of 1 foot (0.3 m), using the Darcy's law equation.

For a seal consisting of a synthetic liner, seepage loss through the liner shall not exceed the quantity equivalent to seepage loss through an adequate soil seal.

**93.423 Uniformity**

The pond bottom shall be as level as possible at all points. Finished elevations shall not be more than 3 inches (75 mm) from the average elevation of the bottom.

**93.424 Prefilling**

Prefilling the pond should be considered in order to protect the liner, to prevent weed growth, to reduce odor, and to maintain moisture content of the seal. However, the dikes must be completely prepared as described in Paragraphs 93.417 (a) and (b) before the introduction of water.

**93.43 Influent Lines****93.431 Material**

Generally accepted material for underground sewer construction will be

given consideration for the influent line to the pond. Unlined corrugated metal pipe should be avoided, however, due to corrosion problems. In material selection, consideration must be given to the characteristics of the wastes, exceptionally heavy external loadings, abrasion, soft foundations, buoyancy and similar problems.

#### **93.432 Manhole**

A manhole or vented cleanout wye shall be installed prior to entrance of the influent line into the primary cell and shall be located as close to the dike as topography permits. Its invert shall be at least 6 inches (150 mm) above the maximum operating level of the pond and provide sufficient hydraulic head without surcharging the manhole.

#### **93.433 Flow Distribution**

Flow distribution structures shall be designed to effectively split hydraulic and organic loads equally to primary cells.

#### **93.434 Placement**

Influent lines may be located along the bottom of the pond with the top of the pipe just below the average upper elevation of the pond seal or liner. However, the full seal depth shall be maintained below the bottom of the pipe and throughout the transition area from the bottom of the pipe to the pond bottom.

In situations where pipes penetrate the lagoon seal, provisions to prevent seepage (such as anti-seep collars) shall be made.

#### **93.435 Point of Discharge**

All primary cells shall have individual influent lines which terminate approximately at the midpoint of the width and at approximately two-thirds the length away from the outlet structure so as to minimize short-circuiting.

All aerated cells shall have influent lines which distribute the load within the mixing zone of the aeration equipment.

#### **93.436 Influent Discharge Apron**

The influent line shall discharge horizontally into a shallow, saucer-shaped depression.

The end of the discharge line shall rest on a suitable concrete apron large enough to prevent the terminal influent velocity at the end of the apron from causing soil erosion. A minimum size apron of 2 feet (0.6 m) square shall be provided.

### **93.44 Control Structures and Interconnecting Piping**

#### **93.441 Structure**

Where possible, facilities design shall consider the use of multi-purpose control structures to facilitate normal operational functions such as

drawdown and flow distribution, flow and depth measurement, sampling, pumps for recirculation, chemical additions and mixing, and minimization of the number of construction sites within the dikes.

As a minimum, control structures shall be: (a) accessible for maintenance and adjustment of controls; (b) adequately ventilated for safety and to minimize corrosion; (c) locked to discourage vandalism; (d) contain controls to permit water level and flow rate control, and complete shutoff; (e) constructed of non-corrodible materials (metal-on-metal contact in controls should be of similar alloys to discourage electrochemical reactions); and (f) located to minimize short-circuiting within the cell and avoid freezing and ice damage.

Recommended devices to regulate water level are valves, slide tubes or dual slide gates. Stop logs are not to be used to regulate water levels. Regulators should be designed so that they can be preset to prevent the pond surface elevation from dropping below the desired operational level.

### **93.442 Piping**

All piping shall be of ductile iron or other acceptable material. Pipes should be anchored with adequate erosion control.

In situations where pipes penetrate the lagoon seal, provisions to prevent seepage (such as anti-seep collars) shall be made.

#### **a. Drawdown Structure Piping**

##### **1. Submerged Takeoffs**

For ponds designed for shallow or variable depth operations, submerged takeoffs are recommended. Intakes shall be located a minimum of 10 feet (3.0 m) from the toe of the dike and 2 feet (0.6 m) from the top of the seal, and shall employ vertical withdrawal.

##### **2. Multi-Level Takeoffs**

For ponds that are designed deep enough to permit stratification of pond content, multiple takeoffs are recommended. There shall be a minimum of 3 withdrawal pipes at different elevations. The bottom pipe shall conform to a submerged takeoff. The others should utilize horizontal entrance. Adequate structural support shall be provided.

##### **3. Surface Takeoffs**

For use under constant discharge conditions and/or relatively shallow ponds under warm weather conditions, surface overflow-type withdrawal is recommended. Design should evaluate floating weir box or slide tube entrance with baffles for scum control.

##### **4. Emergency Overflow**

To prevent overtopping of dikes, emergency overflow should be provided with capacity to carry the peak instantaneous flow expected.

b. Hydraulic Capacity

The hydraulic capacity for continuous discharge structures and piping shall allow for a minimum of 250 percent of the design maximum day flow of the system.

The hydraulic capacity for controlled-discharge systems shall permit transfer of water at a minimum rate of 6 inches (150 mm) of pond water depth per day at the available head.

## **93.5 Miscellaneous**

### **93.51 Fencing**

The pond area shall be enclosed with an adequate fence to prevent entering of livestock and discourage trespassing. Fencing should not obstruct maintenance vehicle traffic on top of the dikes. A vehicle access gate of sufficient width to accommodate mowing equipment shall be provided. All access gates shall be provided with locks.

### **93.52 Access**

An all-weather access road shall be provided to the pond site to allow year-round maintenance of the facility.

### **93.53 Warning Signs**

Appropriate permanent signs shall be provided along the fence around the pond to designate the nature of the facility and advise against trespassing. At least one sign shall be provided on each side of the site and one for every 500 feet (150 m) of its perimeter.

### **93.54 Flow Measurement**

Flow measurement requirements are presented in Paragraph 56.6. Effective weather protection shall be provided for the recording equipment.

### **93.55 Ground Water Monitoring**

An approved system of wells or lysimeters may be required around the perimeter of the pond site to facilitate ground water monitoring. The need for such monitoring will be determined on a case-by-case basis.

### **93.56 Pond Level Gauges**

Pond level gauges shall be provided.

### **93.57 Service Building**

A service building for laboratory and maintenance equipment shall be provided if required. Refer to Section 58.

## **94. OTHER BIOLOGICAL SYSTEMS**

### **94.1 General**

Biological treatment processes not included in these standards may be considered in accordance with Paragraph 53.2.

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## CHAPTER 100 DISINFECTION

### 101. GENERAL

Disinfection of the effluent shall be provided as necessary to meet applicable standards. The design shall consider meeting both the bacterial standards and the disinfectant residual limit in the effluent. The disinfection process should be selected after due consideration of waste characteristics, type of treatment process provided prior to disinfection, waste flow rates, pH of waste, disinfectant demand rates, current technology application, cost of equipment and chemicals, power cost, and maintenance requirements.

Chlorine is the most commonly used chemical for wastewater disinfection. The forms most often used are liquid chlorine and calcium or sodium hypochlorite. Other disinfectants, including chlorine dioxide, ozone, bromine, or ultraviolet disinfection, may be accepted by the reviewing authority in individual cases. If halogens are utilized, it may be necessary to dehalogenate if the residual level in the effluent exceeds effluent limitations or would impair the natural aquatic habitat of the receiving stream.

Where a disinfection process other than chlorine is proposed, supporting data from pilot plant installations or similar full scale installations may be required as a basis for the design of the system. Refer to Paragraph 53.2.

### 102. CHLORINE DISINFECTION

#### 102.1 Type

Chlorine is available for disinfection in gas, liquid (hypochlorite solution), and pellet (hypochlorite tablet) form. The type of chlorine should be carefully evaluated during the facility planning process. The use of chlorine gas or liquid will be most dependent on the size of the facility and the chlorine dose required. Large quantities of chlorine, such as are contained in ton cylinders and tank cars, can present a considerable hazard to plant personnel and to the surrounding area should such containers develop leaks. Both monetary cost and the potential public exposure to chlorine should be considered when making the final determination.

#### 102.2 Dosage

For disinfection, the capacity shall be adequate to produce an effluent that will meet the applicable bacterial limits specified by the regulatory agency for that installation. Required disinfection capacity will vary, depending on the uses and points of application of the disinfection chemical. The chlorination system shall be designed on a rational basis and calculations justifying the equipment sizing and number of units shall be submitted for the whole operating range of flow rates for the type of control to be used. System design considerations shall include the controlling wastewater flow meter (sensitivity and location), telemetering equipment and chlorination controls. For normal domestic wastewater, the following may be used as a guide in sizing chlorination facilities.

Type of Treatment	Dosage
Trickling filter plant effluent	10 mg/L
Activated sludge plant effluent	8 mg/L
Tertiary filtration effluent	6 mg/L
Nitrified effluent	6 mg/L

## **102.3 Containers**

### **102.31 Cylinders**

One hundred fifty pound (68 kg) cylinders are typically used where chlorine gas consumption is less than 150 pounds per day (68 kg/d). Cylinders should be stored in an upright position with adequate support brackets and chains at 2/3 of cylinder height for each cylinder.

### **102.32 Ton Containers**

The use of one-ton (907 kg) containers should be considered where the average daily chlorine consumption is over 150 pounds (68 kg).

### **102.33 Tank Cars**

At large installations, the use of tank cars, generally accompanied by evaporators, may be considered. Area wide public safety shall be evaluated. No interruption of chlorination shall be permitted during tank car switching.

The tank car being used for the chlorine supply shall be located on a dead end, level track that is a private siding. The tank car shall be protected from accidental bumping by other railway cars by a locked derail device or a closed locked switch or both. The area shall be clearly posted "DANGER-CHLORINE". The tank car shall be secured by adequate fencing with gates provided with locks for personnel and rail access.

The tank car site shall be provided with a suitable operating platform at the unloading point for easy access to the protective housing or the tank car for connection of flexible feedlines and valve operation. Adequate area lighting shall be provided for night time operation and maintenance.

### **102.34 Liquid Hypochlorite Solutions**

Storage containers for hypochlorite solutions shall be of sturdy, non-metallic lined construction and shall be provided with secure tank tops and pressure relief and overflow piping. Storage tanks should be either located or vented outside. Provision shall be made for adequate protection from light and extreme temperatures. Tanks shall be located where leakage will not cause corrosion or damage to other equipment. A means of secondary containment shall be provided to contain spills and facilitate cleanup. Due to deterioration of hypochlorite solutions over time, it is recommended that containers not be sized to hold more than one month's needs. At larger facilities and locations where delivery is not a problem, it may be desirable to limit on-site storage to one week. Refer to Section 57.

### **102.35 Dry Hypochlorite Compounds**

Dry hypochlorite compounds should be kept in tightly closed containers and stored in a cool, dry location. Some means of dust control should be considered, depending on the size of the facility and the quantity of compound used. Refer to Section 57.

## **102.4 Equipment**

**102.41 Scales**

Scales for weighing cylinders and containers shall be provided at all plants using chlorine gas. At large plants, scales of the indicating and recording type are recommended. At least a platform scale shall be provided. Scales shall be of corrosion-resistant material.

**102.42 Evaporators**

Where manifolding of several cylinders or ton containers will be required to evaporate sufficient chlorine, consideration should be given to the installation of evaporators to produce the quantity of gas required.

**102.43 Mixing**

The disinfectant shall be positively mixed as rapidly as possible, with a complete mix being effected in 3 seconds. This may be accomplished by either the use of turbulent flow regime or a mechanical flash mixer.

**102.44 Contact Period and Tank**

For a chlorination system, a minimum contact period of 15 minutes at design peak hourly flow or maximum rate of pumpage shall be provided after thorough mixing. For evaluation of existing chlorine contact tanks, field tracer studies should be done to assure adequate contact time.

The chlorine contact tank shall be constructed so as to reduce short-circuiting of flow to a practical minimum. Tanks not provided with continuous mixing shall be provided with "over-and-under" or "end-around" baffling to minimize short-circuiting.

The tank should be designed to facilitate maintenance and cleaning without reducing effectiveness of disinfection. Duplicate tanks, mechanical scrapers, or portable deck-level vacuum cleaning equipment shall be provided. Consideration should be given to providing skimming devices on all contact tanks. Covered tanks are discouraged.

**102.45 Piping and Connections**

Piping systems should be as simple as possible, specifically selected and manufactured to be suitable for chlorine service, with a minimum number of joints. Piping should be well supported and protected against temperature extremes.

Due to the corrosiveness of wet chlorine, all lines designated to handle dry chlorine shall be protected from the entrance of water or air containing water. Even minute traces of water added to chlorine results in a corrosive attack. Low pressure lines made of hard rubber, saran-lined, rubber-lined, polyethylene, polyvinylchloride (PVC), or other approved materials are satisfactory for wet chlorine or aqueous solutions of chlorine.

The chlorine system piping shall be color coded and labeled to distinguish it from other plant piping. Refer to Paragraph 54.5. Where sulfur dioxide is used, the piping and fittings for chlorine and sulfur dioxide systems shall be designed so that interconnection between the two systems cannot occur.

**102.46 Standby Equipment and Spare Parts**

Standby equipment of sufficient capacity should be available to replace the largest unit during shutdowns. Spare parts shall be available for all disinfection equipment to replace parts which are subject to wear and breakage.

**102.47 Chlorinator Water Supply**

An ample supply of water shall be available for operating the chlorinator. Where a booster pump is required, duplicate equipment should be provided, and, when necessary, standby power as well. Protection of a potable water supply shall conform to the requirements of Paragraph 56.2. Adequately filtered plant effluent should be considered for use in the chlorinator.

**102.48 Leak Detection and Controls**

A bottle of 56 percent ammonium hydroxide solution shall be available for detecting chlorine leaks. Where ton (907 kg) containers or tank cars are used, a leak repair kit approved by the Chlorine Institute shall be provided. Consideration should be given to the provision of caustic soda solution reaction tanks for absorbing the contents of leaking one-ton (907 kg) containers where such containers are in use. Consideration should be given to the installation of automatic gas detection and related alarm equipment.

**102.5 Housing****102.51 Feed and Storage Rooms**

If gas chlorination equipment or chlorine cylinders are to be in a building used for other purposes, a gas-tight room shall separate this equipment from any other portion of the building. Floor drains from the chlorine room should not be connected to floor drains from other rooms. Doors to this room shall open only to the outside of the building, and shall be equipped with panic hardware. Rooms shall be at ground level and should permit easy access to all equipment.

Storage areas for one-ton (907 kg) cylinders should be separated from the feed area. In addition, the storage area shall have designated areas for "full" and "empty" cylinders. Chlorination equipment should be situated as close to the application point as reasonably possible. For additional safety considerations, refer to Section 57.

**102.52 Inspection Window**

A clear glass, gas-tight, window shall be installed in an exterior door or interior wall of the chlorinator room to permit the units to be viewed without entering the room.

**102.53 Heat**

Rooms containing disinfection equipment shall be provided with a means of heating so that a temperature of at least 60°F (16 °C) can be maintained. The room should be protected from excess heat. Cylinders shall be kept at essentially room temperature. If liquid hypochlorite solution is used, the containers may be located in an unheated area.

### **102.54 Ventilation**

With chlorination systems, forced, mechanical ventilation shall be installed which will provide one complete fresh air change per minute when the room is occupied. The entrance to the air exhaust duct from the room shall be near the floor. The point of discharge shall be so located as not to contaminate the air inlet to any buildings or present a hazard at the access to the chlorinator room or other inhabited areas. Air inlets shall be so located as to provide cross ventilation with air and at such temperature that will not adversely affect the chlorination equipment. The outside air inlet shall be at least three feet above grade. The vent hose from the chlorinator shall discharge to the outside atmosphere above grade. Where public exposure may be extensive, scrubbers may be required on ventilation discharge.

### **102.55 Electrical Controls**

Switches for fans and lights shall be outside of the room at the entrance. A labeled signal light indicating fan operation should be provided at each entrance, if the fan can be controlled from more than one point.

### **102.56 Protective and Respiratory Gear**

Respiratory air-pac protection equipment, meeting the requirements of the National Institute for Occupational Safety and Health (NIOSH), shall be available where chlorine gas is handled, and shall be stored at a convenient location, but not inside any room where chlorine is used or stored. Instructions for using the equipment shall be posted. The units shall use compressed air, have at least 30-minute capacity and be compatible with the units used by the fire department responsible for the plant.

## **102.6 Sampling and Control**

### **102.61 Sampling**

Facilities shall be included for sampling disinfected effluent after the contact chamber as monitoring requirements warrant. In large installations, or where stream conditions warrant, provisions should be made for continuous monitoring of effluent chlorine residual.

### **102.62 Testing and Control**

Equipment shall be provided for measuring chlorine residual using accepted test procedures. The installation of demonstrated effective facilities for automatic chlorine residual analysis, recording, and proportioning systems should be considered at all large installations.

Equipment shall also be provided for measuring fecal coliform organisms using accepted test procedures as required by the regulatory agency.

## **103. DECHLORINATION**

### **103.1 Types**

Dechlorination of wastewater effluent may be necessary to reduce the toxicity due to chlorine residuals. The most common dechlorination chemicals are sulfur compounds, particularly sulfur dioxide gas or aqueous solutions of sulfite or bisulfite. Pellet

dechlorination systems are also available for small facilities.

The type of dechlorination system should be carefully selected considering criteria including the following: type of chemical storage required, amount of chemical needed, ease of operation, compatibility with existing equipment, and safety.

### 103.2 Dosage

The dosage of dechlorination chemical should depend on the residual chlorine in the effluent, the final residual chlorine limit, and the particular form of the dechlorinating chemical used. The most common dechlorinating agent is sulfite. The following forms of the compound are commonly used and yield sulfite ( $\text{SO}_2$ ) when dissolved in water.

Dechlorination Chemical	Theoretical mg/L Required to Neutralize 1 mg/L $\text{Cl}_2$
Sodium thiosulfate (solution)	0.56
Sodium sulfite (tablet)	1.78
Sulfur dioxide (gas)	0.9
Sodium meta bisulfite (solution)	1.34
Sodium bisulfite (solution)	1.46

Theoretical values may be used for initial approximations, to size feed equipment with the consideration that under good mixing conditions 10% excess dechlorinating chemical is required above theoretical values. Excess sulfur dioxide may consume oxygen at a maximum of 1.0 mg dissolved oxygen for every 4 mg  $\text{SO}_2$ .

The liquid solutions come in various strengths. These solutions may need to be further diluted to provide the proper dose of sulfite.

### 103.3 Containers

Depending on the chemical selected for dechlorination, the storage containers will vary from gas cylinders, liquid in 50 gallon (190 L) drums or dry compounds. Dilution tanks and mixing tanks will be necessary when using dry compounds and may be necessary when using liquid compounds to deliver the proper dosage. Solution containers should be covered to prevent evaporation and spills.

### 103.4 Feed Equipment, Mixing, and Contact Requirements

#### 103.41 Equipment

In general, the same type of feeding equipment used for chlorine gas may be used with minor modifications for sulfur dioxide gas. However, the manufacturer should be contacted for specific equipment recommendations. No equipment should be alternately used for the two gases. The common type of dechlorination feed equipment utilizing sulfur compounds include vacuum solution feed of sulfur dioxide gas and a positive displacement pump for aqueous solutions of sulfite or bisulfite.

The selection of the type of feed equipment utilizing sulfur compounds shall include consideration of the operator safety and overall public safety relative to the wastewater treatment plant's proximity to populated areas and the security of gas cylinder storage. The selection and design of sulfur dioxide feeding

equipment shall take into account that the gas reliquifies quite easily. Special precautions must be taken when using ton (907 kg) containers to prevent reliquefaction.

Where necessary to meet the operating ranges, multiple units shall be provided for adequate peak capacity and to provide a sufficiently low feed rate on turn down to avoid depletion of the dissolved oxygen concentrations in the receiving waters.

#### **103.42 Mixing Requirements**

The dechlorination reaction with free or combined chlorine will generally occur within 15 to 20 seconds. The dechlorination chemical should be introduced at a point in the process where the hydraulic turbulence is adequate to assure thorough and complete mixing. If no such point exists, mechanical mixing shall be provided. The high solubility of SO<sub>2</sub> prevents it from escaping during turbulence.

#### **103.43 Contact Time**

A minimum of 30 seconds for mixing and contact time shall be provided at the design peak hourly flow or maximum rate of pumpage. A suitable sampling point shall be provided downstream of the contact zone. Consideration shall be given to a means of reaeration to assure maintenance of an acceptable dissolved oxygen concentration in the stream following sulfonation.

#### **103.44 Standby Equipment and Spare Parts**

The same requirements apply as for chlorination systems. See Paragraph 102.46.

#### **103.45 Sulfonator Water Supply**

The same requirements apply as for chlorination systems. See Paragraph 102.47.

### **103.5 Housing Requirements**

#### **103.51 Feed and Storage Rooms**

The requirements for housing SO<sub>2</sub> gas equipment shall follow the same guidelines as used for chlorine gas. Refer to Paragraph 102.5 for specific details.

When using solutions of the dechlorinating compounds, the solutions may be stored in a room that meets the safety and handling requirements set forth in Section 57. The mixing, storage, and solution delivery areas must be designed to contain or route solution spillage or leakage away from traffic areas to an appropriate containment unit.

#### **103.52 Protective and Respiratory Gear**

The respiratory air-pac protection equipment is the same as for chlorine. See Paragraph 102.56. Leak repair kits of the type used for chlorine gas that are equipped with gasket material suitable for service with sulfur dioxide gas may be used. (Refer to The Compressed Gas Association Publication CGA G-3-

1995, "Sulfur Dioxide") For additional safety considerations, see Section 57.

### **103.6 Sampling and Control**

#### **103.61 Sampling**

Facilities shall be included for sampling the dechlorinated effluent for residual chlorine. Provisions shall be made to monitor for dissolved oxygen concentration after sulfonation when required by the regulatory agency.

#### **103.62 Testing and Control**

Provision shall be made for manual or automatic control of sulfonator feed rates based on chlorine residual measurement or flow.

## **104. ULTRAVIOLET RADIATION DISINFECTION**

Design standards, operating data, and experience for this process are not well established. Therefore, expected performance of the ultraviolet radiation disinfection (UVRD) units shall be based upon experience at similar full scale installations or thoroughly documented prototype testing with the particular wastewater. Critical parameters for UVRD units are dependent upon manufacturers' design, lamp selection, tube materials, ballasts, configuration, control systems, and associated appurtenances. Proposals on this disinfection process will be reviewed on a case-by-case basis at the discretion of the reviewing authority under the provisions of Paragraph 53.2.

Open channel designs with modular UVRD units that can be removed from the flow are required. At least two banks in series shall be provided in each channel for disinfection reliability and to ensure uninterrupted service during tube cleaning or other required maintenance. Operator safety (electrical hazards and UV radiation exposure) and tube cleaning frequency shall be considered. The hydraulic properties of the system shall be designed to simulate plug flow conditions under the full operating flow range. In addition, a positive means of water level control must be provided to achieve the necessary exposure time. Also refer to Paragraphs 54.2 and 54.3. Closed chamber units will be reviewed on a case by case basis in accordance with Paragraph 53.2.

This process should be limited to a high quality effluent having at least 65% ultraviolet radiation transmittance at 254 nanometers wave length, and BOD and suspended solids concentrations no greater than 30 mg/L at any time. The UV radiation dosage shall be based on the design peak hourly flow. As a general guide in system sizing for an activated sludge effluent with the preceding characteristics, a UV radiation dosage not less than  $30,000 \mu\text{W}\cdot\text{s}/\text{cm}^2$  may be used after adjustments for maximum tube fouling, lamp output reduction after 8760 hours of operation, and other energy absorption losses.

An alarm system shall be provided to separately indicate lamp failure and low UV intensity.

## **105. OZONE**

Ozone systems for disinfection should be evaluated on a case-by-case basis. Design standards, operating data, and experience for this process are not well established. Therefore, design of these systems should be based upon experience at similar full scale installations or thoroughly documented prototype testing with the particular wastewater.

## **CHAPTER 110 SUPPLEMENTAL TREATMENT PROCESSES**

### **111. PHOSPHORUS REMOVAL BY CHEMICAL TREATMENT**

#### **111.1 General**

##### **111.11 Method**

Addition of aluminum salts, iron salts, or lime may be used for the chemical removal of soluble phosphorus. The phosphorus reacts with the aluminum, iron, or calcium ions to form insoluble compounds. Those insoluble compounds may be flocculated with or without the addition of a coagulant aid such as a polyelectrolyte to facilitate separation by sedimentation, or sedimentation followed by filtration.

##### **111.12 Design Basis**

###### **111.121 Preliminary Testing**

Laboratory, pilot or full scale studies of various chemicals, feed points and treatment processes are recommended for existing plant facilities to determine the achievable performance level, cost-effective design criteria, and ranges of required chemical dosages.

The selection of a treatment process and chemical dosage for a new facility should be based on such factors as influent wastewater characteristics, the proposed chemical, effluent requirements, and anticipated treatment efficiency.

###### **111.122 System Flexibility**

Systems shall be designed with sufficient flexibility to allow for several operational adjustments in chemical feed location, chemical feed rates, and for feeding alternate chemical compounds.

#### **111.2 Process Requirements**

##### **111.21 Dosage**

The design chemical dosage shall include the amount needed to react with the phosphorus in the wastewater, the amount required to drive the chemical reaction to the desired state of completion, and the amount required due to inefficiencies in mixing or dispersion. Excessive chemical dosage should be avoided.

##### **111.22 Chemical Selection**

The choice of aluminum salts, iron salts, or lime should be based on the wastewater characteristics, chemical availability and handling, sludge processing and disposal methods, and the economics of the total system.

When lime is used, it may be necessary to neutralize the high pH prior to subsequent treatment in secondary biological systems or prior to discharge in those flow schemes where lime treatment is the final step in the treatment process. Problems associated with lime usage, handling, and sludge production

and dewatering shall be evaluated.

#### **111.23 Chemical Feed Points**

Selection of chemical feed points shall include consideration of the chemicals used in the process, necessary reaction times between chemical and polyelectrolyte additions, and the wastewater treatment processes and components utilized. Flexibility in feed locations shall be provided to optimize chemical usage and treatment efficiency.

#### **111.24 Flash Mixing**

Each chemical must be mixed rapidly and uniformly with the flow stream. Where separate mixing basins are provided, they should be equipped with mechanical mixing devices. The detention period should be at least 30 seconds.

#### **111.25 Flocculation**

The particle size of the precipitate formed by chemical treatment may be very small. Consideration should be given in the process design to the addition of synthetic polyelectrolytes to aid settling. The flocculation equipment should be adjustable in order to obtain optimum floc growth, control deposition of solids, and prevent floc destruction.

#### **111.26 Liquid - Solids Separation**

The velocity through pipes or conduits from flocculation basins to settling basins should not exceed 1.5 feet per second (0.5 m/s) in order to minimize floc destruction. Entrance works to settling basins should also be designed to minimize floc shear.

Settling basin design shall be in accordance with criteria outlined in Chapter 70. For design of the sludge handling system, special consideration should be given to the type and volume of sludge generated in the phosphorus removal process.

#### **111.27 Filtration**

Effluent filtration shall be considered where effluent phosphorus concentrations of less than 1 mg/L must be achieved.

### **111.3 Feed Systems**

#### **111.31 Location**

All liquid chemical mixing and feed installations should be installed on corrosion resistant pedestals and elevated above the highest liquid level anticipated during emergency conditions.

The chemical feed equipment shall be designed to meet the maximum dosage requirements for the design conditions.

Lime feed equipment should be located so as to minimize the length of slurry conduits. All slurry conduits shall be accessible for cleaning.

#### **111.32 Liquid Chemical Feed System**

Liquid chemical feed pumps should be of the positive displacement type with variable feed rate. Pumps shall be selected to feed the full range of chemical quantities required for the phosphorus mass loading conditions anticipated with the largest unit out of service. Consideration should be given to systems including pumps and piping that will feed either iron or aluminum compounds to provide flexibility. Refer to Paragraph 111.51.

Screens and valves shall be provided on the chemical feed pump suction lines.

An air break or anti-siphon device shall be provided where the chemical solution stream discharges to the transport water stream to prevent an induction effect resulting in overfeed.

Consideration shall be given to providing pacing equipment to optimize chemical feed rates.

### **111.33 Dry Chemical Feed System**

Each dry chemical feeder shall be equipped with a dissolver which is capable of providing a minimum 5-minute retention at the maximum feed rate.

Polyelectrolyte feed installations should be equipped with two solution vessels and transfer piping for solution make-up and daily operation.

Make-up tanks shall be provided with an eductor funnel or other appropriate arrangement for wetting the polymer during the preparation of the stock feed solution. Adequate mixing should be provided by a large-diameter low-speed mixer.

## **111.4 Storage Facilities**

### **111.41 Size**

Storage facilities shall be sufficient to ensure that an adequate supply of the chemical is available at all times. Exact size required will depend on size of shipment, length of delivery time, and process requirements. Storage for a minimum supply of 10 days should be provided.

### **111.42 Location and Containment**

The liquid chemical storage tank and tank fill connections shall be located within a containment structure having a capacity exceeding the total volume of all storage vessels. Valves on discharge lines shall be located adjacent to the storage tank and within the containment structure. Refer to Paragraph 57.2.

Auxiliary facilities, including pumps and controls, within the containment area shall be located above the highest anticipated liquid level. Containment areas shall be sloped to a sump area and shall not contain floor drains.

Bag storage should be located near the solution make-up point to avoid unnecessary transportation and housekeeping problems.

### **111.43 Accessories**

Platforms, stairs, and railings shall be provided as necessary, to afford

convenient and safe access to all filling connections, storage tank entries, and measuring devices.

Storage tanks shall have reasonable access provided to facilitate cleaning.

## **111.5 Other Requirements**

### **111.51 Materials**

All chemical feed equipment and storage facilities shall be constructed of materials resistant to chemical attack by all chemicals normally used for phosphorus removal. Refer to Section 57.

### **111.52 Temperature, Humidity, and Dust Control**

Precautions shall be taken to prevent chemical storage tanks and feed lines from reaching temperatures likely to result in freezing or chemical crystallization at the concentrations employed. A heated enclosure or insulation may be required. Consideration shall be given to temperature, humidity, and dust control in all chemical feed room areas.

### **111.53 Cleaning**

Consideration shall be given to the accessibility of piping. Piping should be installed with plugging wyes, tees or crosses with removable plugs at changes in direction to facilitate cleaning.

### **111.54 Filling Drains and Draw-Off**

Above-bottom drawoff from chemical storage or feed tanks shall be provided to avoid withdrawal of settled solids into the feed system. A bottom drain shall also be installed for periodic removal of accumulated settled solids. Provisions shall be made in the fill lines to prevent back siphonage of chemical tank contents.

## **111.6 Safety and Hazardous Chemical Handling**

The chemical handling facilities shall meet the appropriate safety and hazardous chemical handling facilities requirements of Section 57.

## **111.7 Sludge Handling**

Consideration shall be given to the type and additional capacity of the sludge handling facilities needed when chemicals are added. Refer to Chapter 80.

## **112. HIGH RATE EFFLUENT FILTRATION**

### **112.1 General**

#### **112.11 Applicability**

Granular media filters may be used as an advanced treatment device for the removal of residual suspended solids from secondary effluents. Filters may be necessary where effluent concentrations of less than 20 mg/L of suspended solids and/or 1.0 mg/L of phosphorus must be achieved or to obtain adequate turbidity reduction for urban water reuse. A pre-treatment process such as

chemical coagulation and sedimentation or other acceptable process should precede the filter units where effluent suspended solids requirements are less than 10 mg/L.

### **112.12 Design Considerations**

Care should be given in designing pipes or conduits ahead of filter units, if applicable, to minimize shearing of floc particles. Consideration should be given in the plant design to provide flow-equalization facilities to moderate filter influent quality and quantity.

## **112.2 Filter Types**

Filters may be of the gravity type or pressure type. Pressure filters shall be provided with ready and convenient access to the media for inspection or cleaning. Where abnormal quantities of greases or similar solids which result in filter plugging are expected, filters should be of the gravity type.

## **112.3 Filtration Rates**

### **112.31 Allowable Rates**

Filtration rates shall not exceed 5 gpm/sq ft [3.40 L/(m<sup>2</sup>·s)] based on the design peak hourly flow rate applied to the filter units. The expected design maximum suspended solids loading to the filter should also be considered in determining the necessary filter area.

### **112.32 Number of Units**

Total filter area shall be provided in two or more units, and the filtration rate shall be calculated on the total available filter area with one unit out of service.

## **112.4 Backwash**

### **112.41 Backwash Rate**

The backwash rate shall be adequate to fluidize and expand each media layer a minimum of 20 percent based on the media selected. The backwash system shall be capable of providing variable backwash rates. Minimum and maximum backwash rates shall be based on demonstrated satisfactory field experience under similar conditions. The design shall provide for a minimum backwash period of 10 minutes.

### **112.42 Backwash Pumps**

Pumps for backwashing filter units shall be sized and interconnected to provide the required backwash rate to any filter with the largest pump out of service. Filtered water from the clear well or chlorine tank shall be used as the source of backwash water. Waste filter backwash shall be adequately treated.

### **112.43 Backwash Surge Control**

The rate of return of waste filter backwash water to treatment units shall be controlled so that the rate does not exceed 15 percent of the design average daily flow rate to the treatment unit. The hydraulic and organic load from waste backwash water shall be considered in the overall design of the treatment plant.

Surge tanks shall have a minimum capacity of two backwash volumes, although additional capacity should be considered to allow for operational flexibility. Where waste backwash water is returned for treatment by pumping, adequate pumping capacity shall be provided with the largest unit out of service.

#### **112.44 Backwash Water Storage**

Total backwash water storage capacity provided in an effluent clearwell or other unit shall equal or exceed the volume required for two complete backwash cycles.

#### **112.5 Filter Media Selection**

Selection of proper media type and size will depend on required effluent quality, the type of treatment provided prior to filtration, the filtration rate selected, and filter configuration. In dual or multi-media filters, media size selection must consider compatibility among media. Media shall be selected and provided to meet specific conditions and requirements relative to the project under consideration. The selection and sizing of the media shall be based on demonstrated satisfactory field experience under similar conditions. All media shall have a uniformity coefficient of 1.7 or less. The uniformity coefficient, effective size, depth, and type of media shall be set forth in the specifications.

#### **112.6 Filter Appurtenances**

The filters shall be equipped with washwater troughs, surface wash or air scouring equipment, means of measurement and positive control of the backwash rate, equipment for measuring filter head loss, positive means of shutting off flow to a filter being backwashed, and filter influent and effluent sampling points. If automatic controls are provided, there shall be a manual override for operating equipment, including each individual valve essential to the filter operation. The underdrain system shall be designed for uniform distribution of backwash water (and air, if provided) without danger of clogging from solids in the backwash water. If air is to be used for filter backwash, separate backwash blower(s) shall be provided. Provision shall be made to allow periodic chlorination of the filter influent or backwash water to control slime growths. When chemical disinfection is not provided at the plant, manual dosage of chlorine compounds is acceptable.

#### **112.7 Access and Housing**

Each filter unit shall be designed and installed so that there is ready and convenient access to all components and the media surface for inspection and maintenance without taking other units out of service. Housing for filter units shall be provided. The housing shall be constructed of suitable corrosion-resistant materials. All controls shall be enclosed and the structure housing filter, controls and equipment shall be provided with adequate heat and ventilation equipment to minimize problems with excess humidity.

#### **112.8 Proprietary Equipment**

Where proprietary filtration equipment not conforming to the preceding requirements is proposed, data which supports the capability of the equipment to meet effluent requirements under design conditions shall be provided. Such equipment will be reviewed on a case-by-case basis at the discretion of the regulatory agency. Refer to Paragraph 53.2.

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## **APPENDIX HANDLING AND TREATMENT OF SEPTAGE AT A WASTEWATER TREATMENT PLANT**

### **General**

One method of septage disposal is the discharge to a municipal wastewater treatment plant. All plants require special design considerations prior to the acceptance of septage.

### **Definition**

Septage is a general term for the contents removed from septic tanks, portable vault toilets, privy vaults, holding tanks, very small wastewater treatment plants, or semi-public facilities (i.e., schools, motels, mobile home parks, campgrounds, small commercial endeavors) receiving wastewater from domestic sources.

Non domestic (industrial) wastes are not included in the definition and are not covered by this appendix.

Contents from grease traps should not be hauled to most municipal wastewater treatment plants for disposal.

### **Characteristics**

Compared to raw domestic wastewater from a conventional municipal sewer collection system, septage usually is quite high in organics, grease, hair, stringy material, scum, grit, solids, and other extraneous debris. Substantial quantities of phosphorus, ammonia nitrogen, bacterial growth inhibitors, and cleaning materials may be present in septage depending on the source. Tables No. 1 and No. 2 (Tables 3-4 and 3-8 from the U.S. EPA Handbook entitled "Septage Treatment and Disposal" 1984, EPA-625/6-84-009 reprinted herein) give a comparison of some of the common parameters for septage and municipal wastewater.

Data for local septage to be received should be collected for design of septage receiving and treatment systems. The characteristics of septage should be expected to vary widely from load to load depending on the source.

### **Treatment**

Septage is normally considered treatable at a plant. However, unless proper engineering planning and design is provided, septage may represent a shock loading or have other adverse impacts on plant processes and effluent quality which will be influenced by many factors including the following:

- a. Capacity (mgd) ( $m^3/d$ ) of the plant relative to the amount and rate of septage directed to the plant;
- b. Unused plant capacity available (above current sewer collection system loadings) to treat septage loadings;
- c. Sensitivity of the treatment plant process to daily fluctuations in loadings brought about by the addition of septage;
- d. Slug septage loadings of BOD, ammonia nitrogen, or phosphorus which may cause process upset, odor nuisance, aeration tank/aerated digester foaming, or pass through to the effluent;

- e. The point of introduction of the septage into the plant process. Feasible alternative points of feed to the treatment units shall be evaluated including feed to the sludge processing units provided the unit function will not be adversely affected;
- f. The ability to control feed rates of septage to the plant for off peak loading periods; and,
- g. The volume and concentrations of bacterial growth inhibitors in septage from some portable vault toilets and recreational dump station holding tanks.

The permitted plant effluent regulatory limits on each of the controlled parameters must be considered when evaluating these factors.

### **Considerations**

It is essential that an adequate engineering evaluation be made of the existing plant and the anticipated septage loading prior to receiving septage at the plant. The regulatory agency shall be contacted to obtain the appropriate approvals prior to the acceptance of septage. For proposed plant expansion and upgrading, the engineering report or facility plan (refer to Chapter 10) shall include anticipated septage loading in addressing treatment plant sizing and process selection. The following items should be included as appropriate in the engineering evaluation and facility planning:

- a. The uninterrupted and satisfactory treatment (within the plant regulatory limits) of wasteloads from the sewer system must not be adversely affected by the addition of septage to the plant;
- b. In general, the smaller the plant design capacity relative to the septage loading, the more subject the plant will be to upset and potential violation of permitted discharge effluent limits;
- c. Allocation of organic plant capacity originally planned for future growth;
- d. For plants to be expanded and upgraded, the engineering evaluation and facility planning should jointly consider the sensitivity of the treatment process to receiving septage and the impact on discharge parameter limits;
- e. An evaluation of available plant operator staff and the staffing requirements necessary when septage is to be received. Plant staff should be present when septage is received and unloaded. Added laboratory work associated with receiving septage for treatment should be included in the staffing and laboratory facilities evaluation;
- f. The space for constructing septage receiving facilities that are to be off-line from the raw wastewater incoming from the sewer system. The location of the septage receiving facility and the septage hauler unloading area should consider other plant activity and traffic flow; and,
- g. The impact of the septage handling and treatment on the plant sludge handling and processing units and ultimate sludge disposal procedures.

### **Receiving Facility**

The design of the septage receiving station at the plant should provide for the following elements:

- a. A hard surface haul truck unloading ramp sloped to a drain to allow ready cleaning of any spillage and washing of the haul tank, connector hoses, and fittings. The ramp drainage

must be tributary to treatment facilities and shall exclude excessive stormwater;

- b. A flexible hose fitted with easy connect coupling to provide for direct connection from the haul truck outlet to minimize spillage and help control odors;
- c. Washdown water with ample pressure, hose, and spray nozzle for convenient cleaning of the septage receiving station and haul trucks. The use of chlorinated effluent may be considered for this purpose. If a potable water source is used, it must be protected in accordance with Section 56 of these Recommended Standards;
- d. An adequate off-line septage receiving tank should be provided. Capability to collect a representative sample of any truck load of waste accepted for discharge at the plant shall be provided. The receiving tank should be designed to provide complete draining and cleaning by means of a sloped bottom equipped with a drain sump. The design should give consideration to adequate mixing, for testing, uniformity of septage strength, and chemical addition, if necessary, for treatability and odor control. The operator shall have authority to prevent and/or stop any disposal that is likely to cause a discharge violation;
- e. Screening, grit, and grease removal of the septage as appropriate to protect the treatment units;
- f. Pumps provided for handling the septage should be of the nonclogging design and capable of passing 3-inch (75 mm) diameter solids;
- g. Valving and piping for operational flexibility to allow the control of the flow rate and point of septage discharge to the plant;
- h. Safety features to protect the operational personnel. Refer to Section 57; and
- i. Laboratory and staffing capability to determine the septage strength and/or toxicity to the treatment processes. Provision for operation reports to include the plant load attributed to septage.

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